

# Numerical and Experimental Investigation of Natural Convection Flow of CO<sub>2</sub> in Aqueous

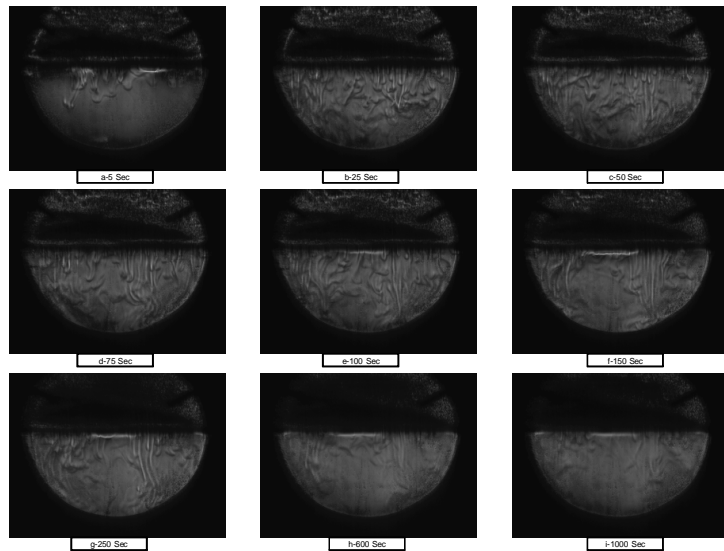
R. Khosrokhavar<sup>1</sup>, G. Elsinga<sup>1</sup>, R. Farajzadeh<sup>2</sup>, and J. Bruining<sup>1</sup>

<sup>1</sup>Delft University of Technology, The Netherlands, <sup>2</sup>Shell International Global Solutions B.Vb., The Netherlands

**Introduction:** Optimal storage of carbon dioxide (CO<sub>2</sub>) in aquifers requires dissolution in the aqueous phase.

## Experimental Results:

A set of experiments has been done to visualize  $(\partial_y c)$  the induced convection currents when carbon dioxide is brought above a layer of liquid water, (p=64 bar, T=313 K).



**Results:** The numerical result is shown in Fig. 1 (22286 elements) and Fig.2 (11566 elements).

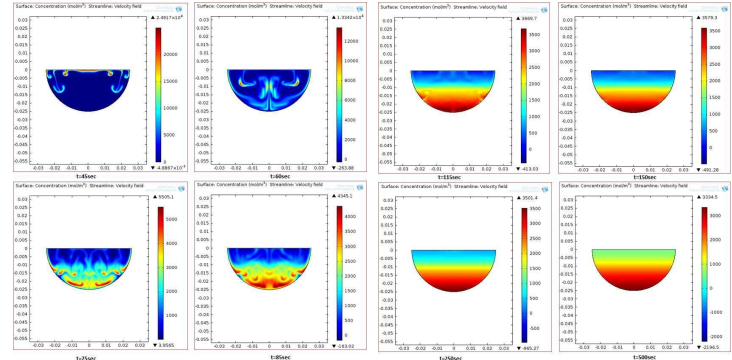


Figure 1 shows a numerical simulation for experimental conditions in the conventional formulation.

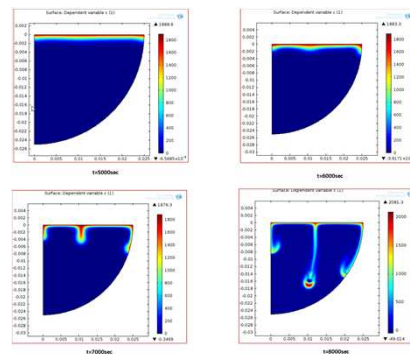


Figure 2 shows a numerical simulation for the experimental conditions in the stream function formulation.

## Computational Methods:

### a) Conventional Formulation:

we consider a 2D cross-section of a cylindrical cell. For the liquid phase, we apply the creeping flow equation and the transport of diluted species in term of pressure, velocity and concentration. At the interface a domain probe and distributed ODE are implemented.

### b) Streamline Formulation:

Equivalently We define the stream function and the vorticity as follows :

$$v = \frac{\partial \psi}{\partial y}, \quad u = -\frac{\partial \psi}{\partial x} \quad (1) \quad \omega = \frac{\partial u}{\partial x} - \frac{\partial v}{\partial y} \quad (2)$$

### Governing Equations:

$$\nabla^2 \psi = -\omega \quad (3) \quad \nabla^2 \omega = -Gr \frac{\partial c}{\partial x} \quad (4)$$

$$\frac{\partial c}{\partial t} + \mathbf{v} \cdot \mathbf{grad} c = D \Delta c \quad (5)$$

where  $\psi$  is stream function and  $\omega$  is vorticity.  $u$  and  $v$  are velocities in  $x$  &  $y$  directions.

## Conclusions:

In principle it is possible to simulate natural convection both with the conventional and the stream function formulation. Both the simulations and the experiment show the existence of a region of high concentration gradient near the gas-liquid interface. However, in the simulation the onset of instabilities occurs later in the experiments.

Denser grid simulations are required for more meaningful comparisons.

## References:

1. Khosrokhavar, R; Elsinga, G ; Mojaddam, A ; Farajzadeh, R.; Bruining, J. Visualization of Natural Convection Flow of (Sub-) and (Super-) Critical CO<sub>2</sub> in Aqueous and Oleic Systems by Applying Schlieren Method, SPE 143264, EUROPEC Vienna, Austria (2011).
2. Farajzadeh, R.; Zitha P.L.J. and Bruining, J. Enhanced mass transfer of CO<sub>2</sub> into water: experiment and modeling. Ind. Eng. Chem. Res., 48 (9), pp. 4542-4552. A.A. (2009)