

TWO-PHASE FLOW AND MULTIPHYSICS SIMULATIONS IN COMSOL

***By
Dr. K. K. Singh***

***CHEMICAL ENGINEERING DIVISION
BHABHA ATOMIC RESEARCH CENTRE
TROMBAY, MUMBAI - 400085***



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Objective and Outline of the Presentation

Objective

- *Share some of the research works carried out at Chemical Engineering Division, BARC using COMSOL Multiphysics*
- *Highlight the capability of COMSOL Multiphysics to simulate problems involving two-phase flow and multiple physics*

Part-1: Two-phase Flow Simulations

- *Drop formation at a single hole in a sieve plate*
- *Air pulsed liquid columns*
- *Liquid-liquid two-phase flow at microfluidic junctions*

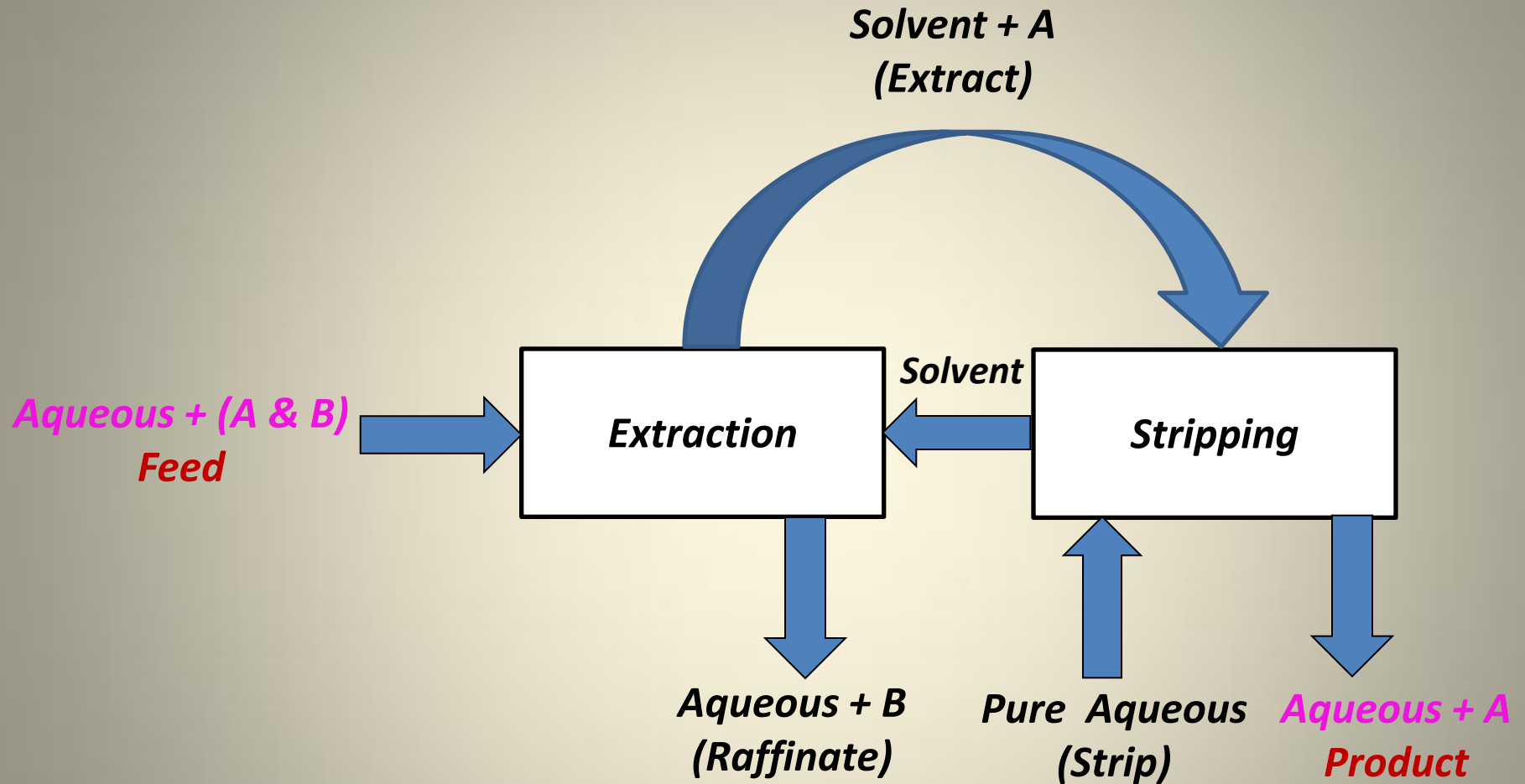
Part-2: Multiphysics Simulations

- *Flow electrolysers*
- *Pore of a supported liquid membrane*
- *Mass transfer for a single droplet*

Part-1

Two-phase Flow Simulations

Drop Formation at a Single Hole



A typical solvent extraction flow sheet

Drop Formation at a Single Hole

$$m = K_L a \tau \Delta C$$

$$a = \frac{6\phi}{d_{32}}$$

$m \Rightarrow$ amount of mass transferred (mol)

$a \Rightarrow$ interfacial area (m^2)

$\tau \Rightarrow$ contact time (sec)

$\Delta C \Rightarrow$ average concentration difference (mol/m^3)

$K_L \Rightarrow$ mass transfer coefficient (m/s)

$\phi \Rightarrow$ volume fraction of dispersed phase (-)

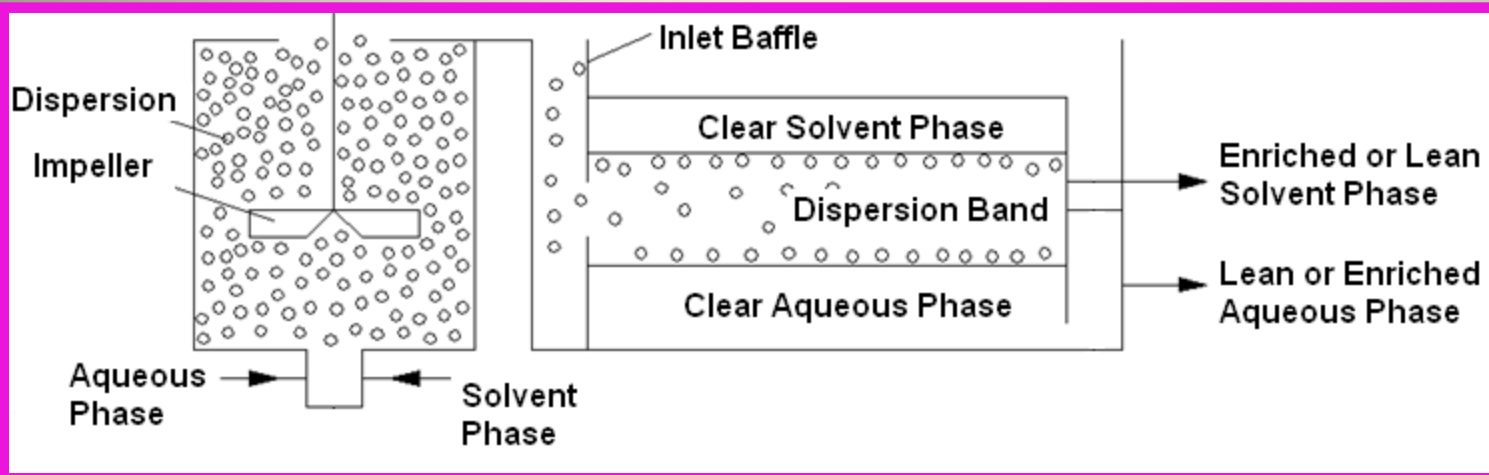
$d_{32} \Rightarrow$ Sauter mean diameter (m)

Conventional Contactors

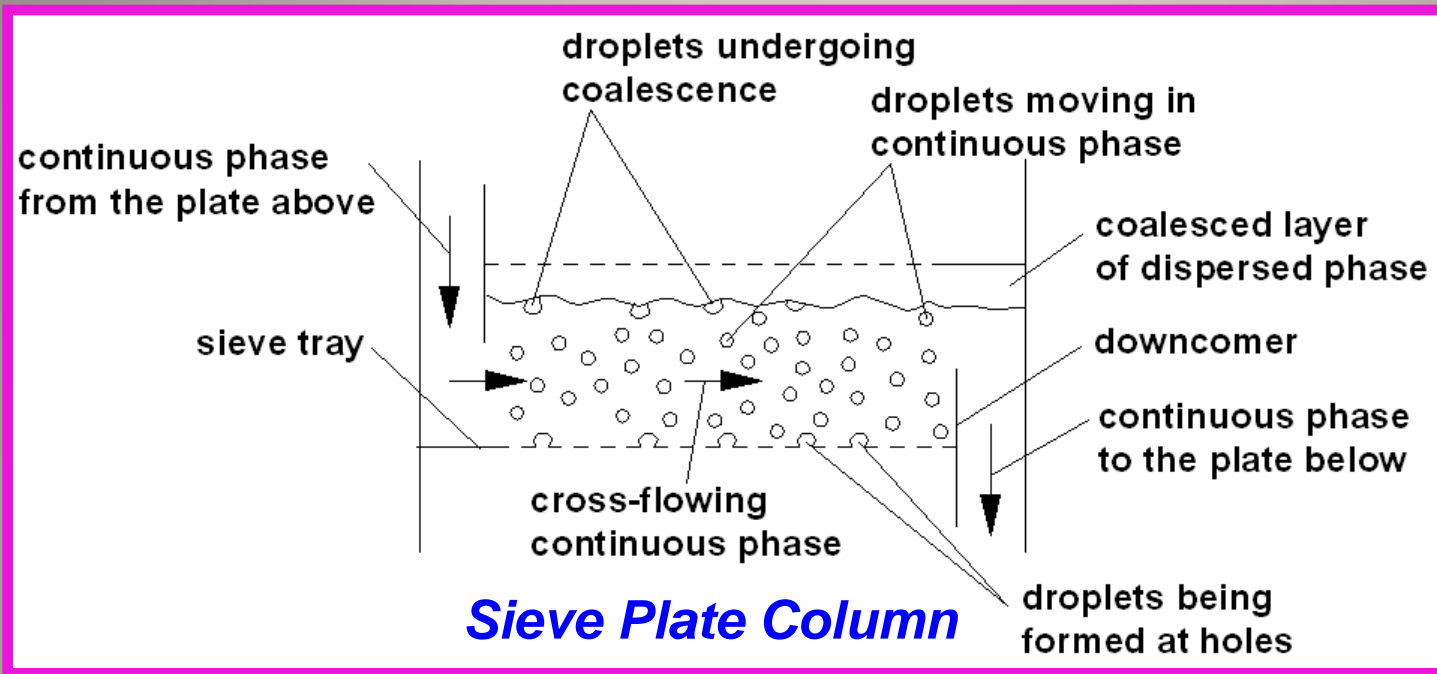
- Mixer settlers
- Pulsed columns
- Rotating disk contactors
- Centrifugal extractor

Novel Contactors

- Microfluidic devices
- Hollow fibre modules



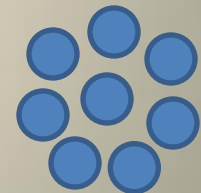
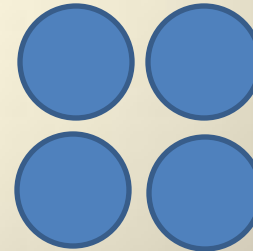
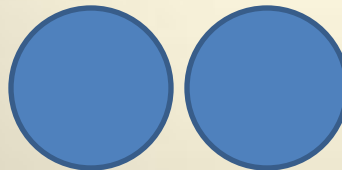
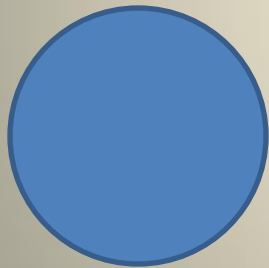
Drop Formation at a Single Hole



$$m = K_L a \tau \Delta C$$

$$a = \frac{6\phi}{d_{32}}$$

Drops of an optimum size are required

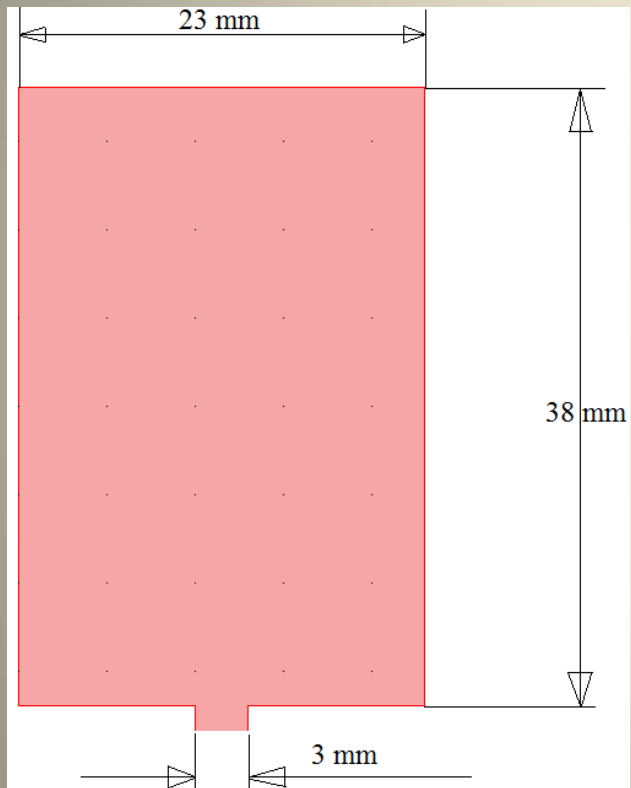


Drop size and hence specific interfacial area will depend on

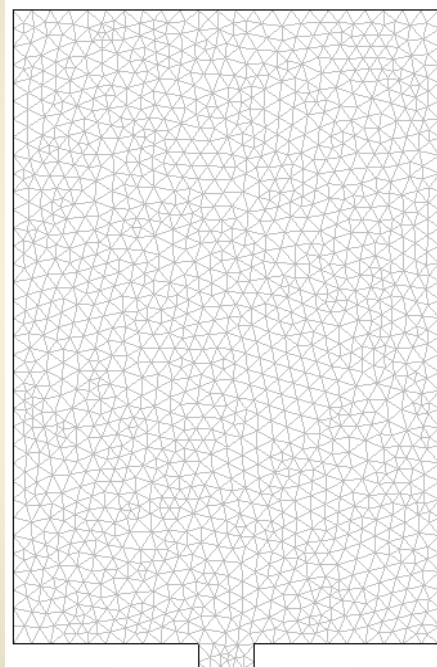
- **Flow rates**
- **Physical properties of the continuous and the dispersed phases**
- **Plate geometry (hole size, type of hole, open area)**

Drop Formation at a Single Hole

- Objective was to understand the process of drop formation
- Only one hole was considered
- Continuous phase was considered quiescent



Computational domain



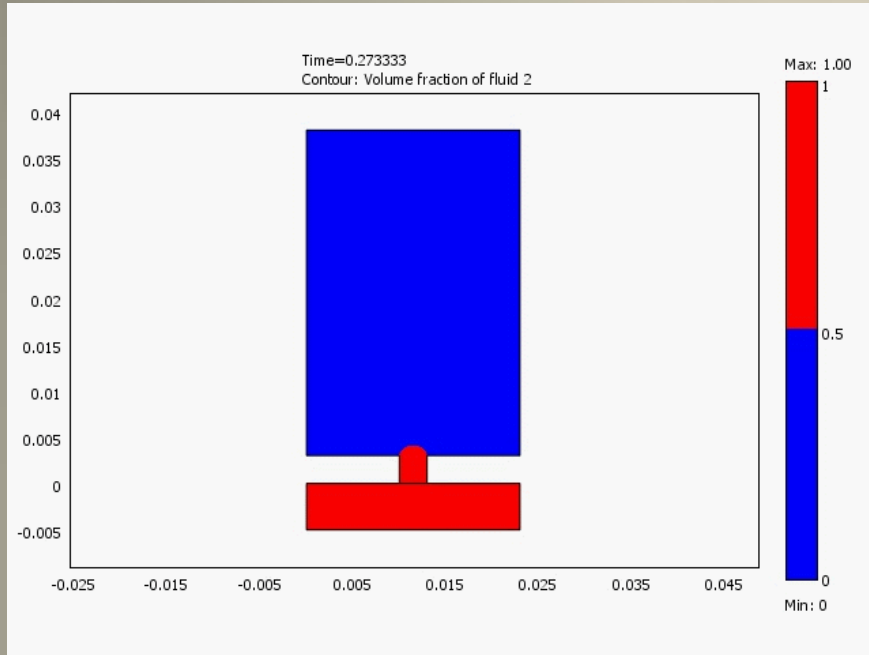
*Meshed
computational Domain*

*Phase field method for
interface tracking*

Continuous phase: Water

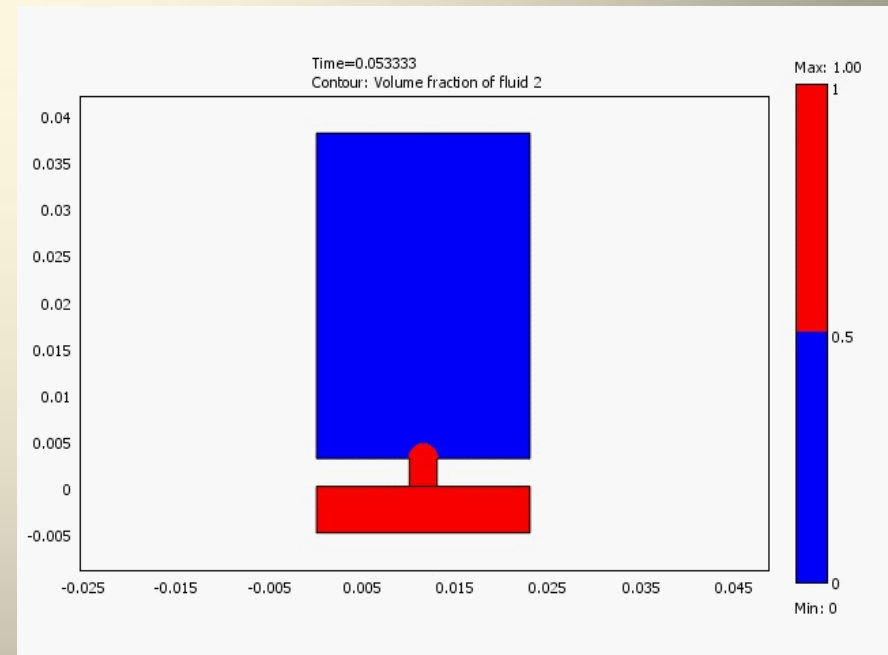
Dispersed phase: Exxol D80

Drop Formation at a Single Hole

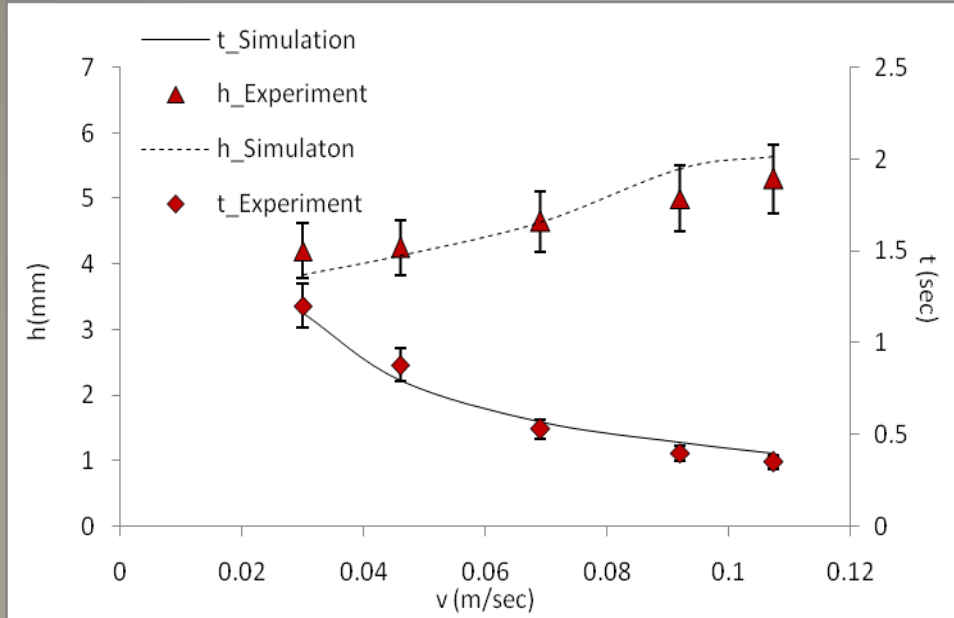


$V = 0.03 \text{ m/s}$

$V = 0.11 \text{ m/s}$



Drop Formation at a Single Hole

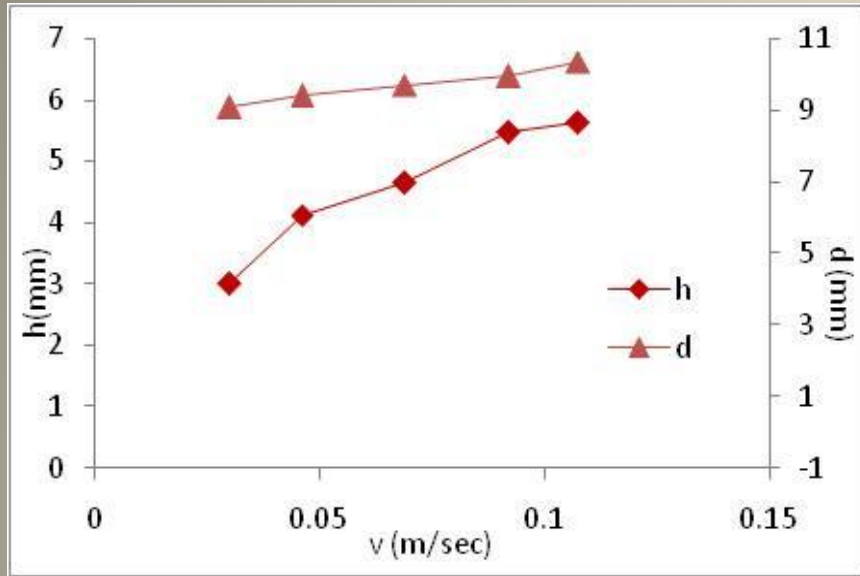


Validation was done using the data reported in literature

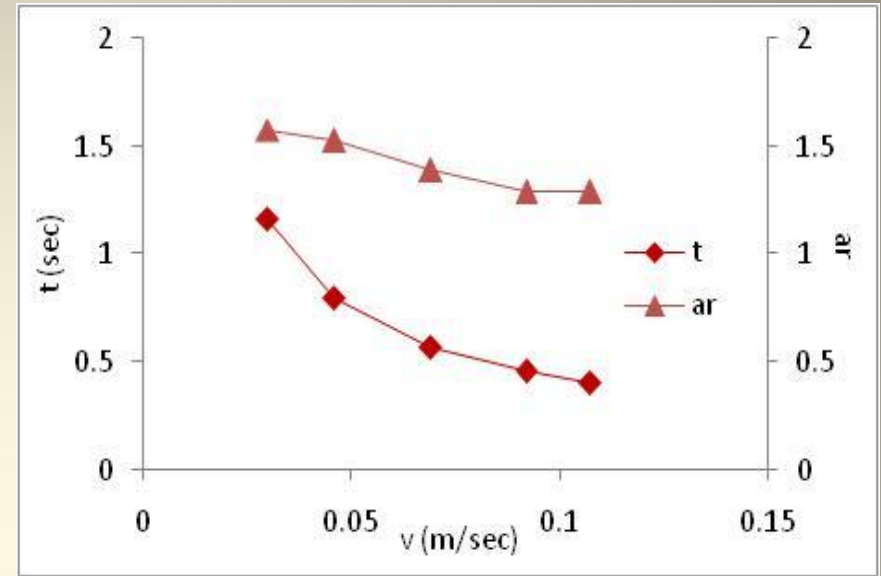
Parametric studies were done to understand the effects of following variables on drop formation process

- *Flow rate***
- *Physical properties (density, viscosity, interfacial tension, contact angle)***
- *Geometry (hole diameter, type of hole)***

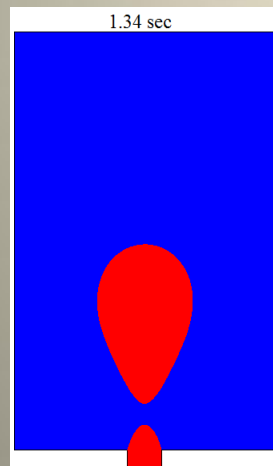
Drop Formation at a Single Hole



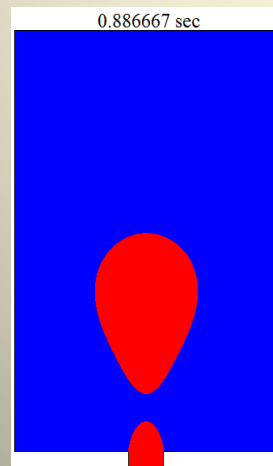
Effect of velocity on height of drop detachment and drop diameter



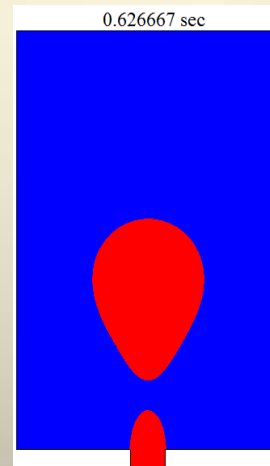
Effect of velocity on time of drop detachment and aspect ratio



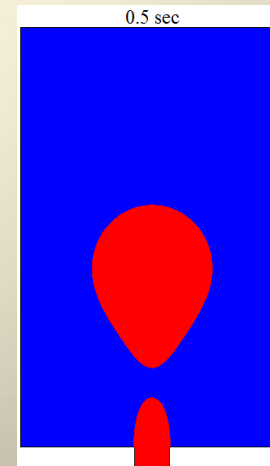
0.03 m/sec



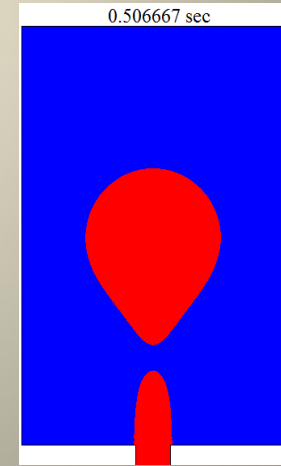
0.046 m/sec



0.069 m/sec



0.092 m/sec



0.107 m/sec

Drop Formation at a Single Hole

$$\frac{dEo^{0.42}}{d_h} = 1.962 - \frac{0.0087487}{Fr} + \frac{0.81402}{\theta^2}$$

$$Eo = \frac{(\rho_C - \rho_D)gd_h^2}{\sigma}$$

$$Fr = \frac{v^2}{gd_h}$$

Results from parametric studies were used to obtain a correlation for equivalent drop diameter

$d \Rightarrow$ Equivalent drop diameter (m)

$d_h \Rightarrow$ Hole diameter (m)

$\theta \Rightarrow$ Contact angle (radian)

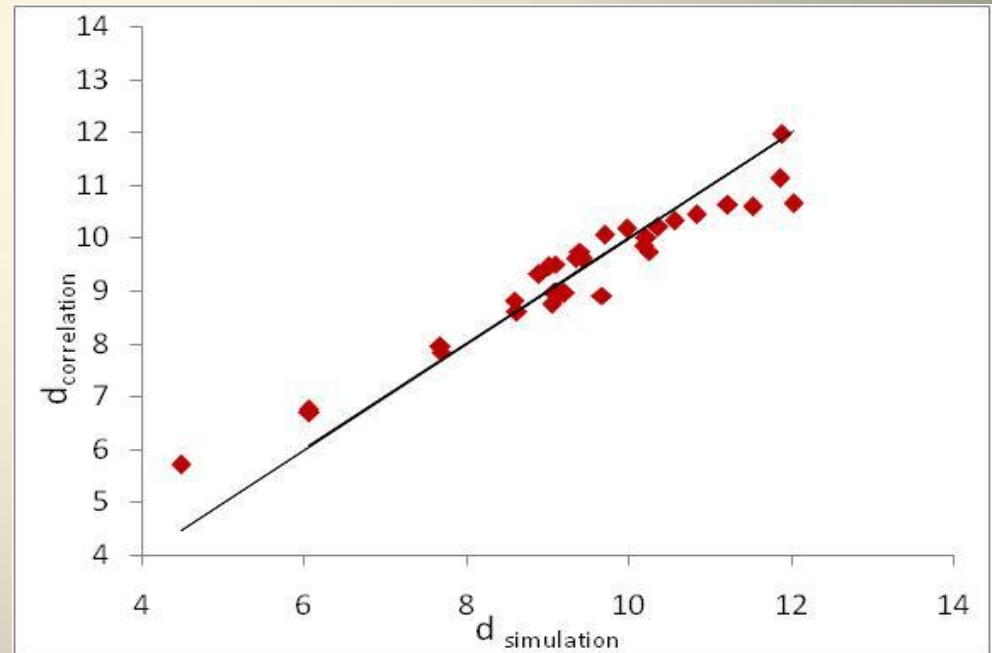
$Eo \Rightarrow$ Eotvos number

$Fr \Rightarrow$ Froude number

$\rho_C \Rightarrow$ Density of the continuous phase

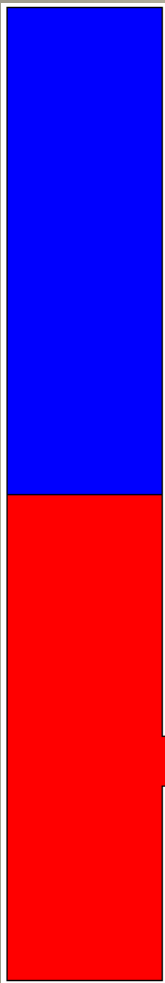
$\rho_D \Rightarrow$ Density of the dispersed phase

$\sigma \Rightarrow$ Interfacial tension

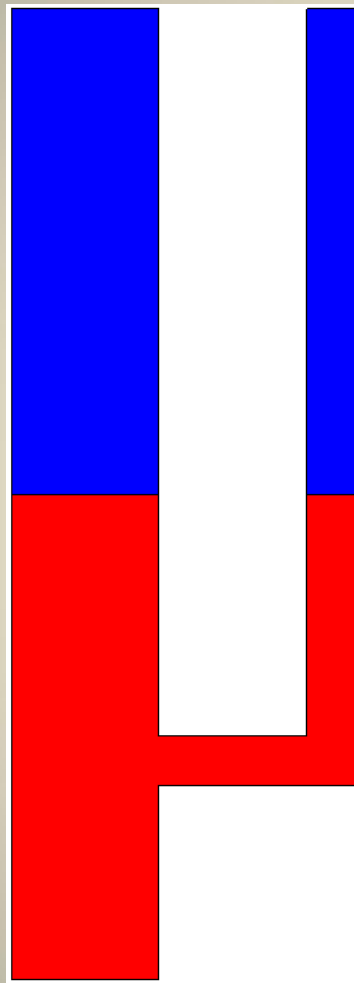


The study helps us understand the process of drop formation at a single hole

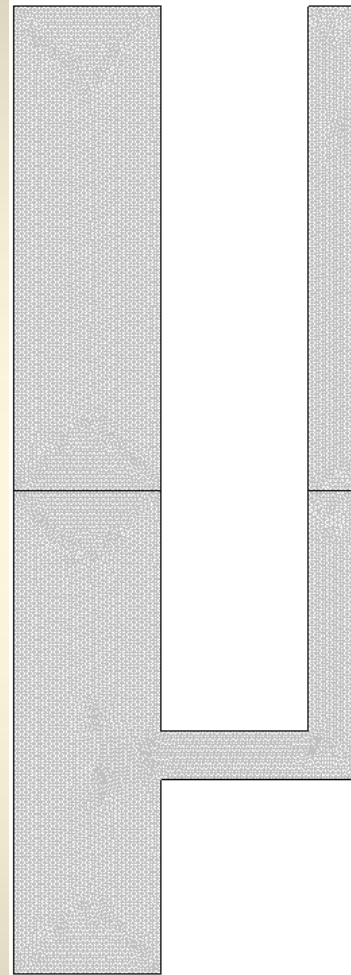
Air Pulsed Liquid Column



Liquid column



Liquid column with pulse leg



Meshed computational domain

Column height 1 m
Column diameter 6 inch
Pulse leg size 2 inch

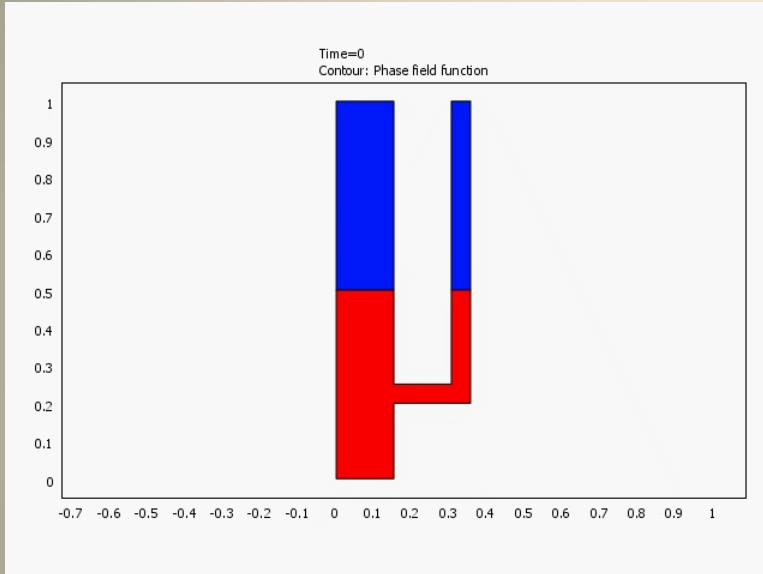
Phase field method was used for interface tracking

Laminar flow of water and air

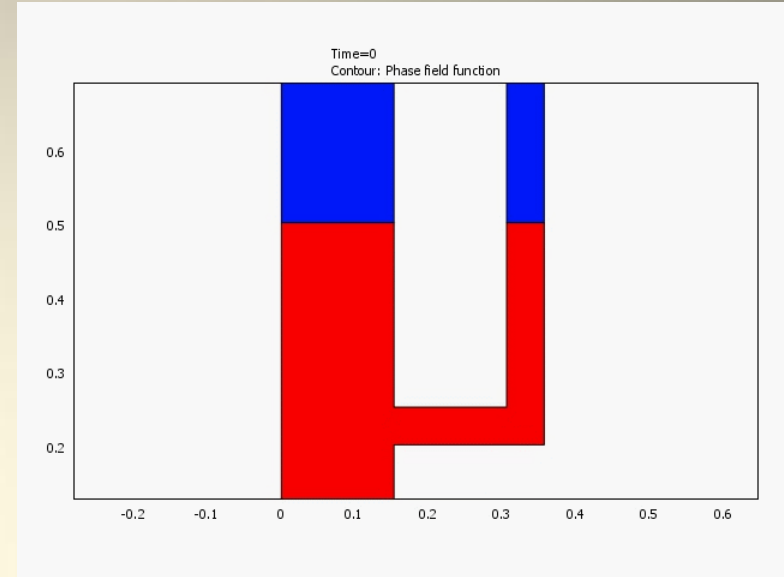
Cyclic air pressure applied at pulse leg

2D simulations

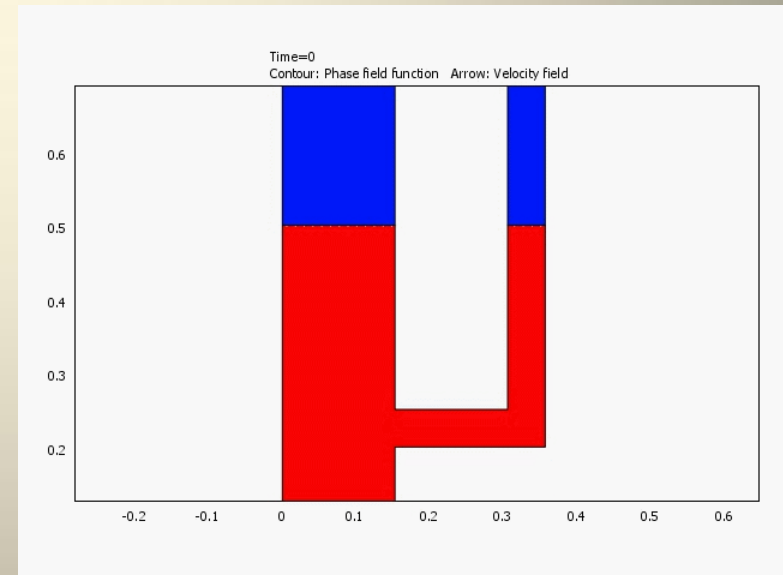
Air Pulsed Liquid Column



Animation showing movement of liquid level in the column and pulse leg

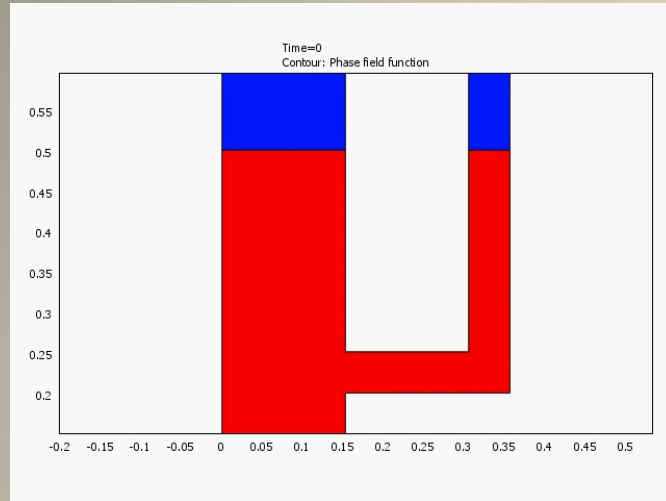


Closer look at the interfaces

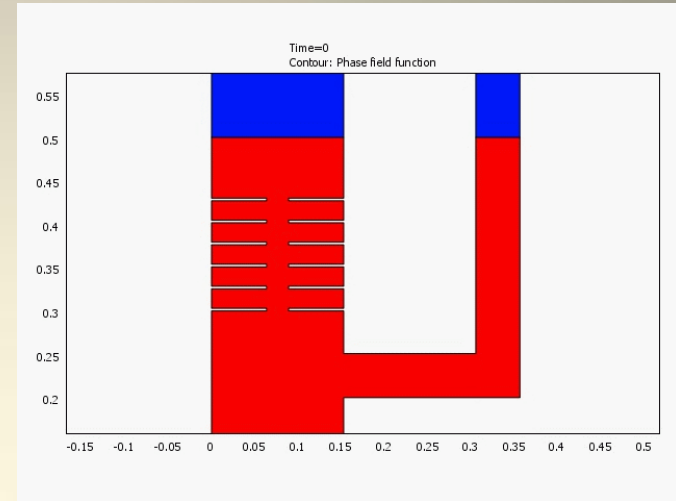


Velocity Vectors

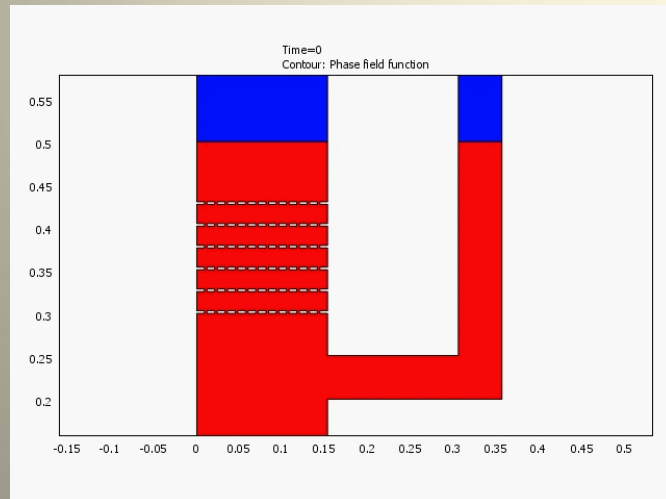
Air Pulsed Liquid Column



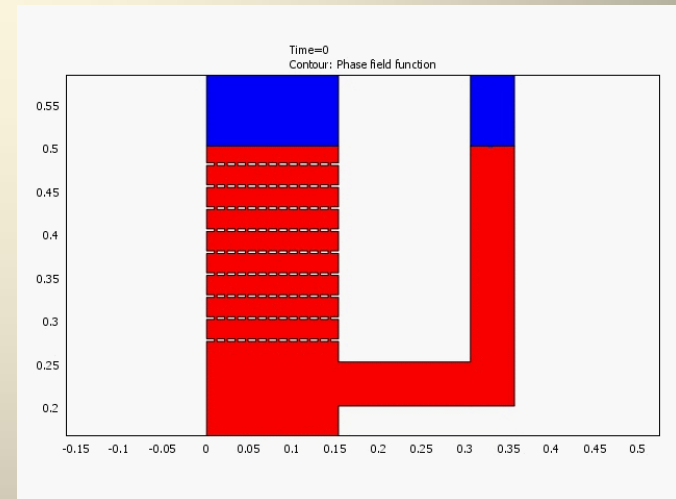
Column without internals



Column with orifice plates

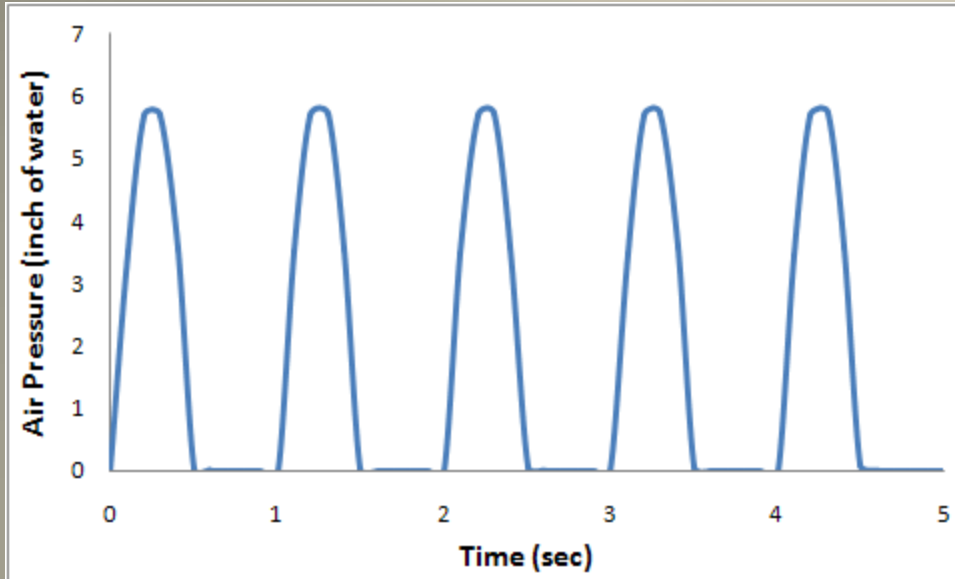


Column with 6 sieve plates



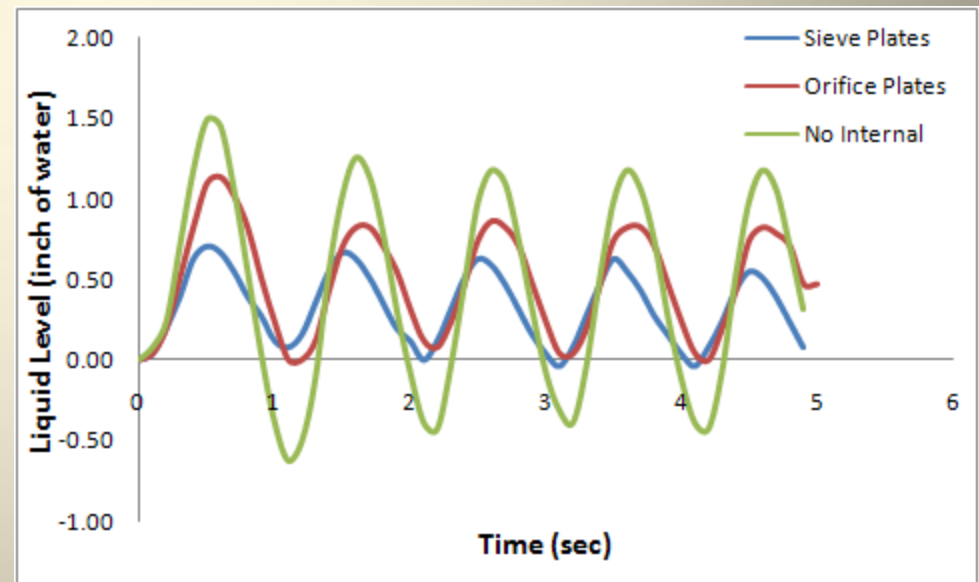
Column with 9 sieve plates

Air Pulsed Liquid Column



Simulation results are as expected i.e. amplitude of liquid level fluctuation for a given air pressure cycle reduces as the pressure drop attributable to the internals in the column increases

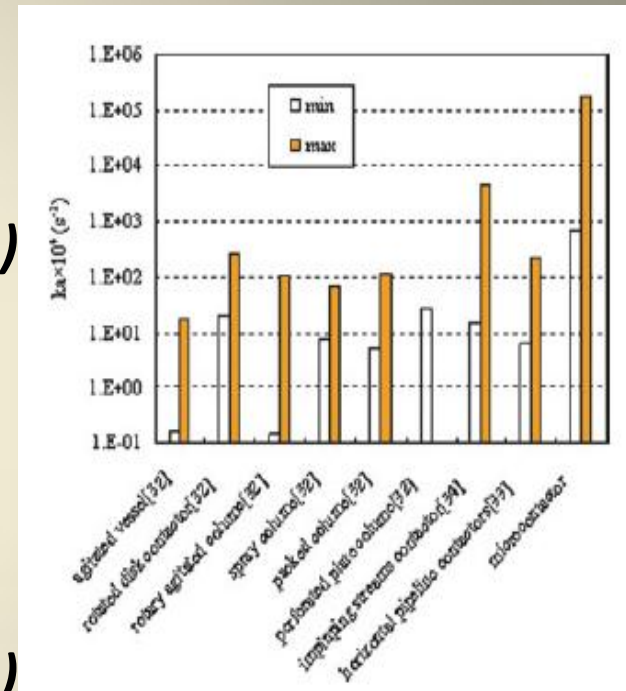
The simulations can be used to fix the air pressure cycle for a desired amplitude of liquid level fluctuation in the column.



L-L Two-phase Flow at Microfluidic Junctions

Advantages of Microfluidic Devices

- High specific interfacial area for heat transfer and multiphase applications
- Less uncertainty in scale up
- Low inventory (better for hazardous chemicals)
- Uninterrupted production
- In situ production / distributed production

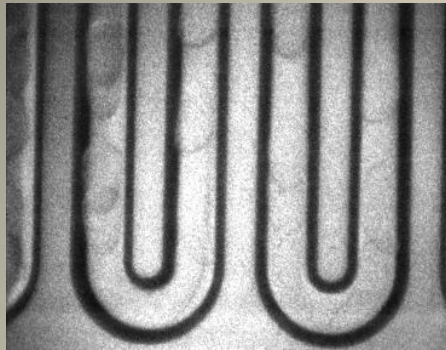


Comparison of overall mass transfer coefficients in different SX equipment

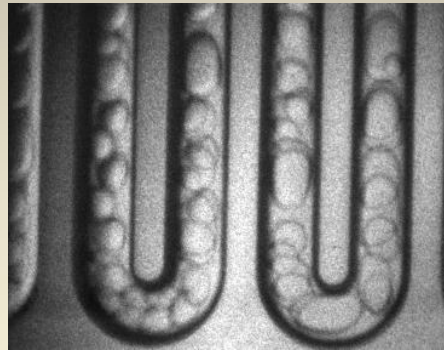
Advantages of SX in Microchannels

- High specific interfacial area (low contact time)
- Ordered and controllable flow patterns
- Monodispersed droplets (ease in phase separation)

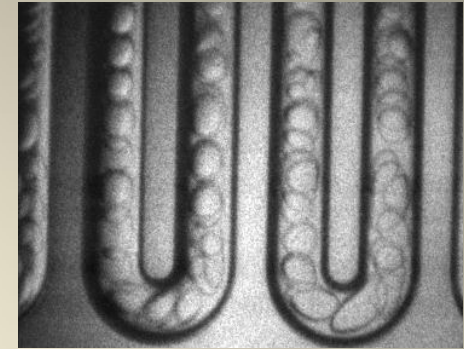
L-L Two-phase Flow at Microfluidic Junctions



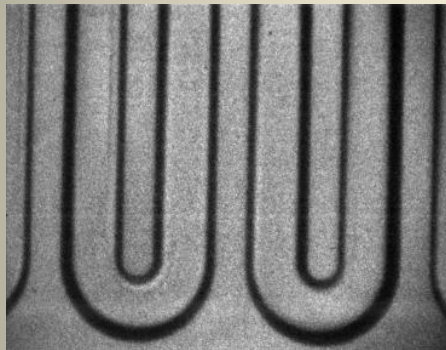
Slug Flow



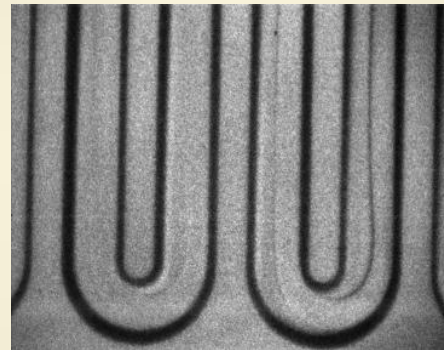
Slug and Droplet Flow



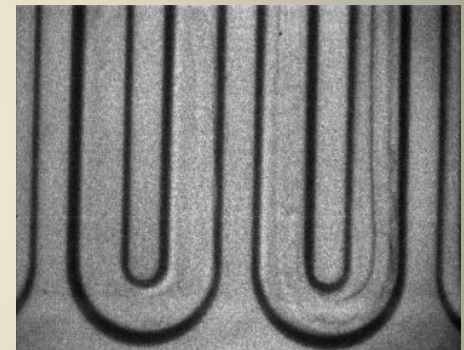
Droplet Flow



Unstable Annular Flow

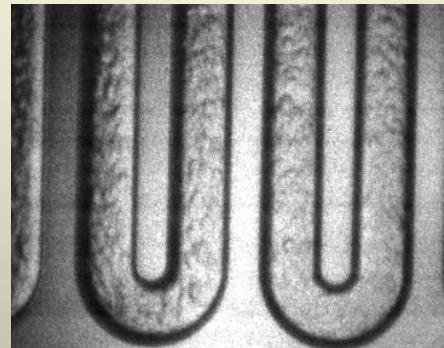


Annular Flow



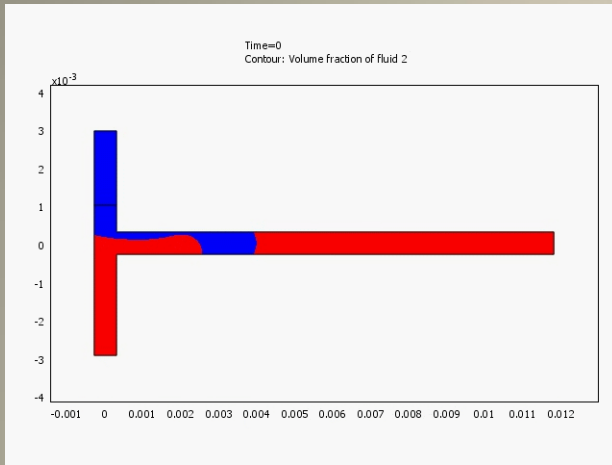
Annular Dispersed Flow

Different types of L-L flow patterns observed in a serpentine microchannel for water butanol system

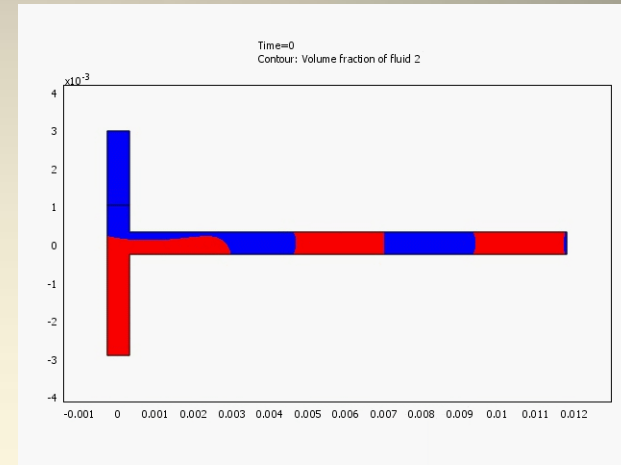


Fully Dispersed Flow

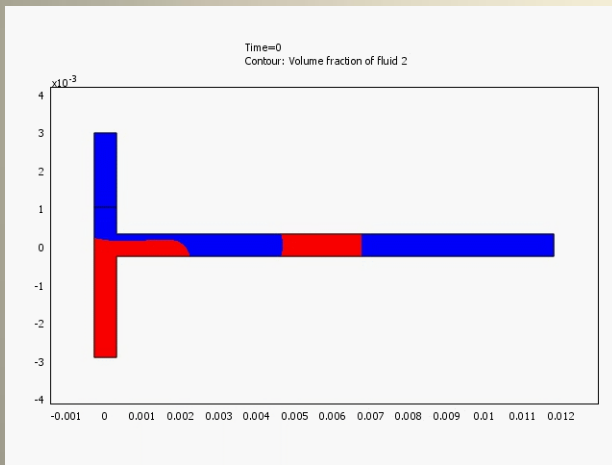
L-L Two-phase Flow at Microfluidic Junctions



$V_d = 0.942 \text{ cm/s}$
 $V_c = 0.471 \text{ cm/s}$



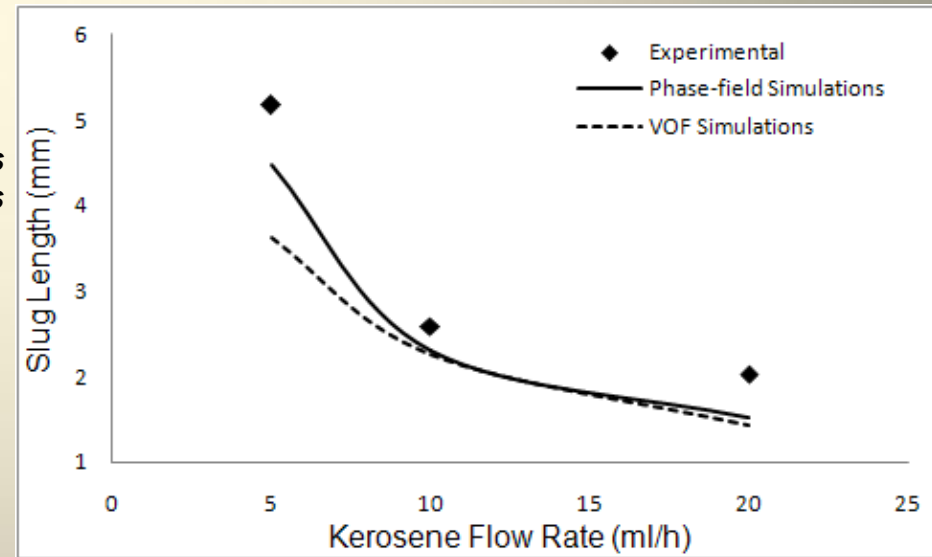
$V_d = 0.942 \text{ cm/s}$
 $V_c = 0.942 \text{ cm/s}$



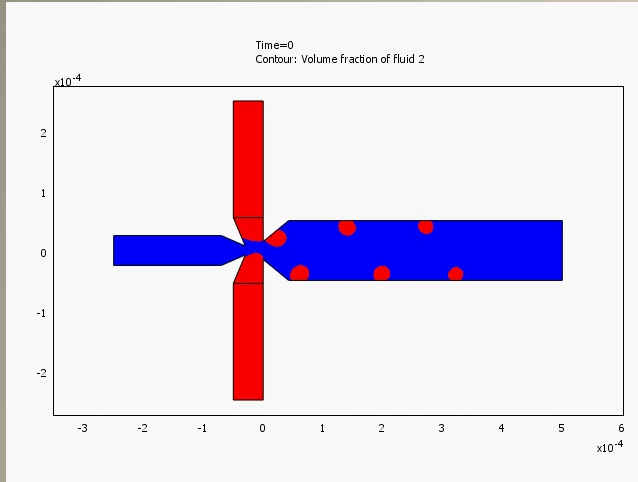
$V_d = 0.942 \text{ cm/s}$
 $V_c = 1.883 \text{ cm/s}$

Red Color
Kerosene

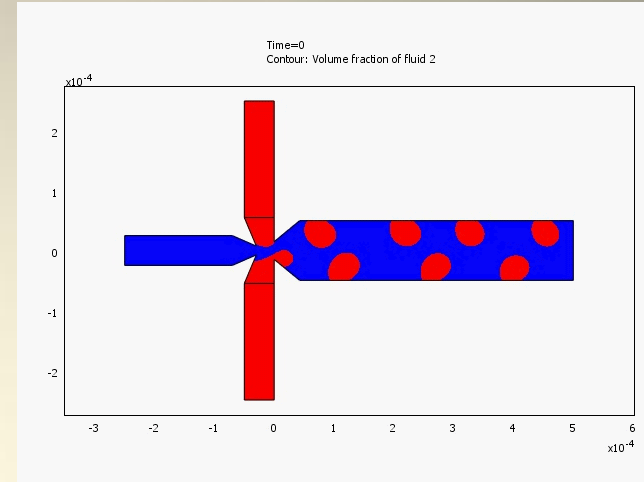
Blue Color
Water



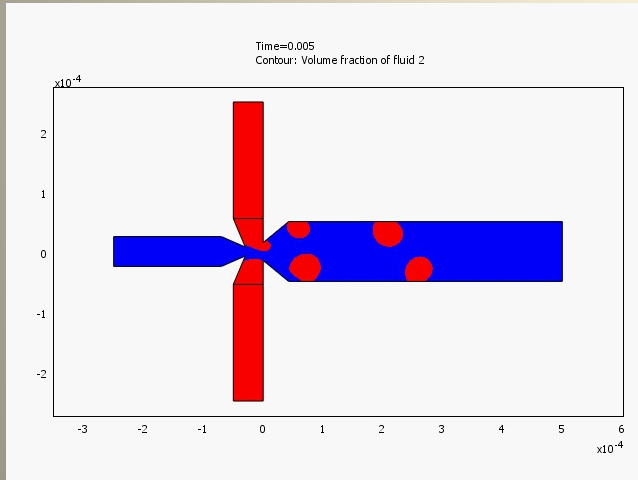
L-L Two-phase Flow at Microfluidic Junctions



$V_d = 0.067 \text{ cm/s}$
 $V_c = 1.53 \text{ cm/s}$



$V_d = 0.167 \text{ cm/s}$
 $V_c = 1.33 \text{ cm/s}$



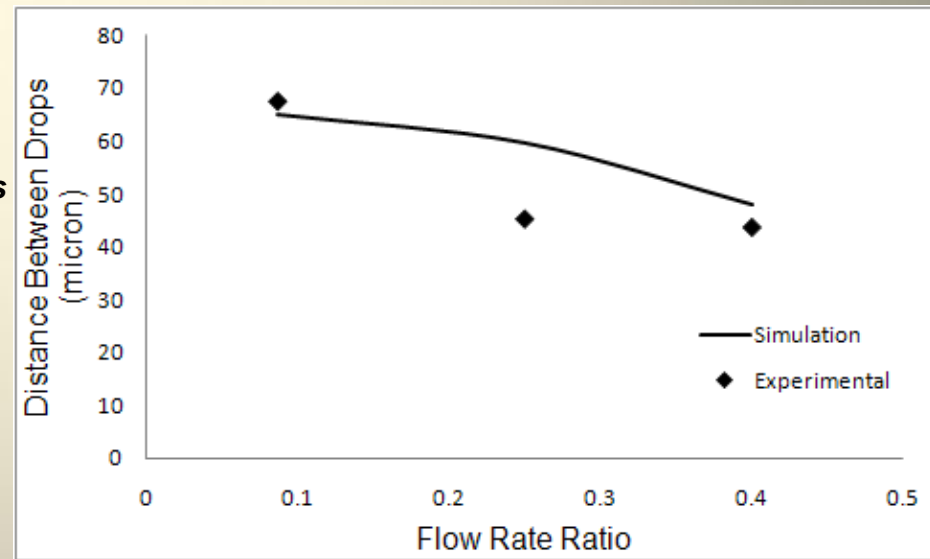
$V_d = 0.267 \text{ cm/s}$
 $V_c = 1.33 \text{ cm/s}$

Red Color

Blue Color

Water

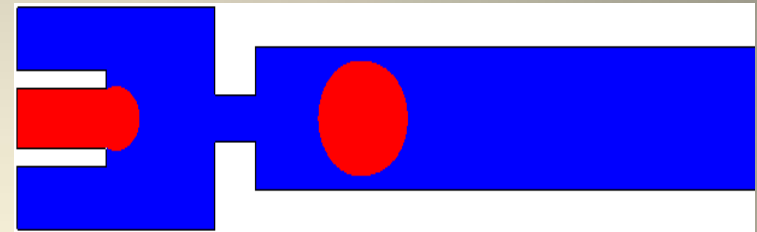
Olive Oil



L-L Two-phase Flow at Microfluidic Junctions



Cross-flow T-junction



Flow Focusing Junction

- ***Numerical simulations can be used to predict liquid-liquid two-phase flow patterns at microfluidic junctions if geometry, flow conditions and physical properties are known***
- ***Numerical simulations can serve as a screening tool to zero in on a geometry that will give the desired flow pattern***

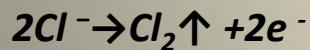
Part-2

Multiphysics Simulations

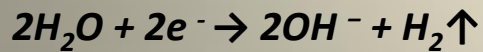
Numerical Simulation of Flow Electrolysers

- **To study the effect of flow field on the performance of electro-neutral bulk of a flow electrolyzer having stationary cathode**
- **Simulation of flow electrolyser having streaming mercury cathode**
- **Coupled solution of Navier-Stokes and Nernst-Planck equations**
- **Validation of the computational approach was done using the data reported in literature**

Reactions:

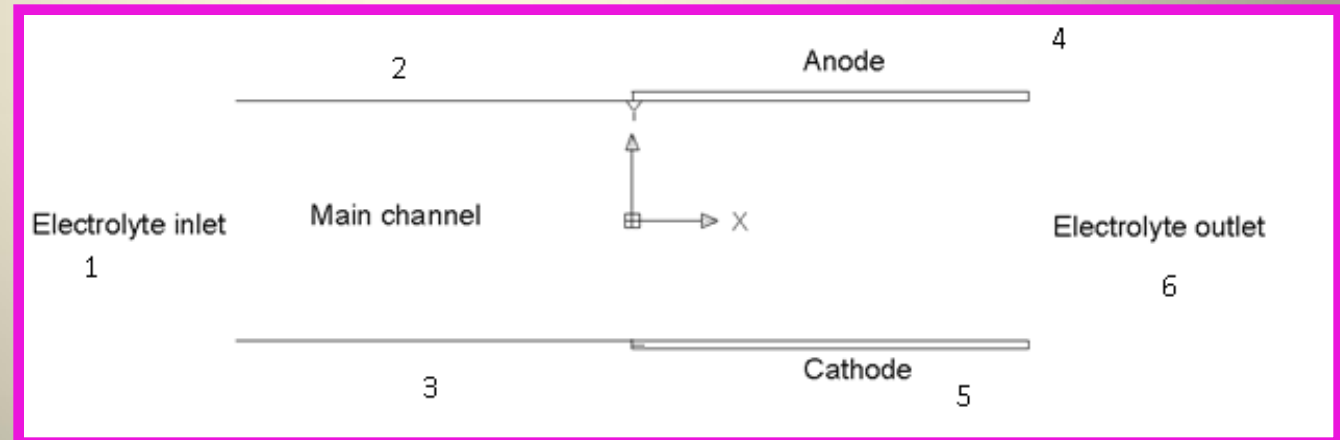


(at the anode)



(at the cathode)

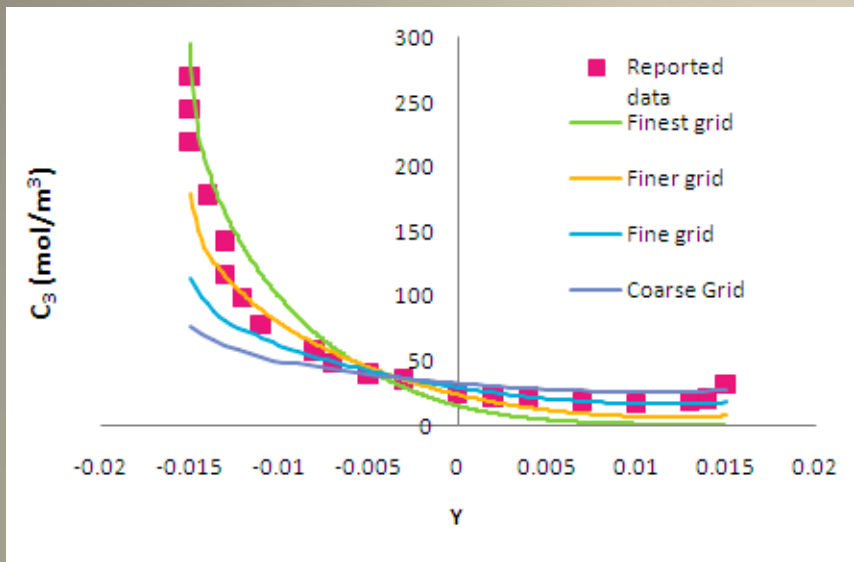
Na^+ , Cl^- , OH^- are the ions.



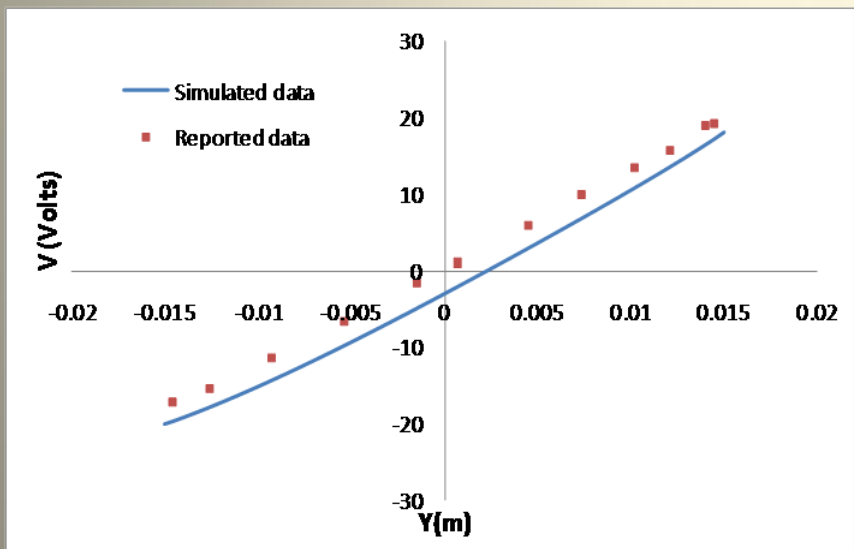
Domain used for validating the computational approach

Lu et al., Numerical simulation of salt water electrolysis in parallel plate electrode channel under forced convection. *Electrochimica Acta*, 53 (2007), 768-776.

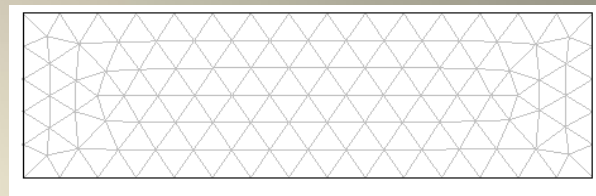
Numerical Simulation of Flow Electrolysers



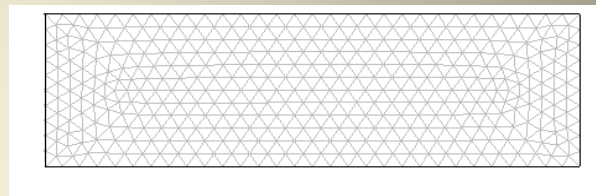
Concentration profile at the outlet



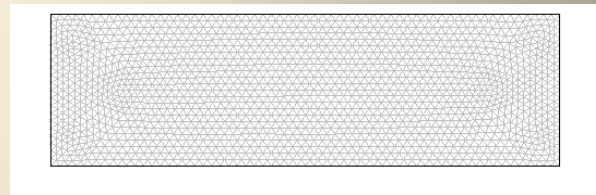
Potential profile at the outlet



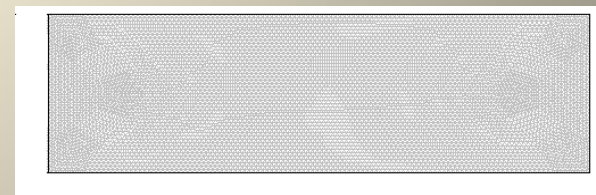
6 elements/cm²



26 elements/cm²

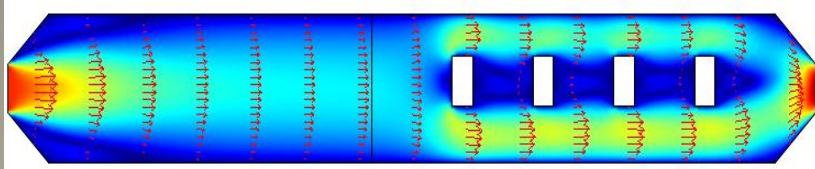


103 elements/cm²

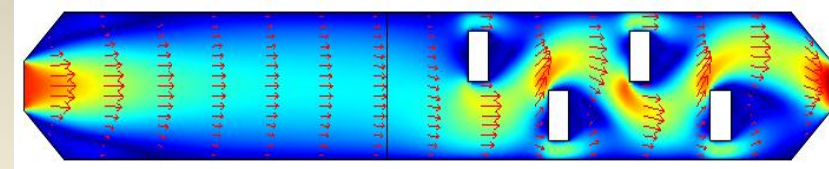


211 elements/cm²

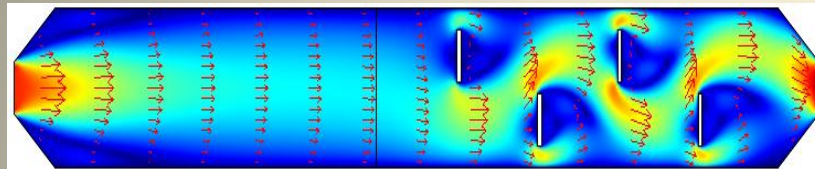
Numerical Simulation of Flow Electrolysers



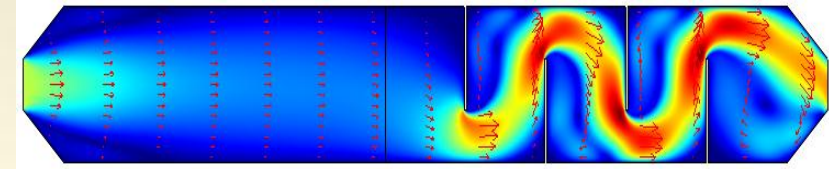
Thick rectangular obstacles



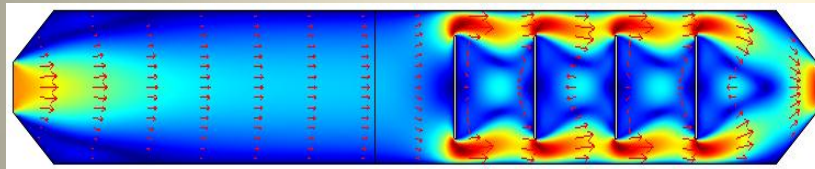
Thick rectangular obstacles



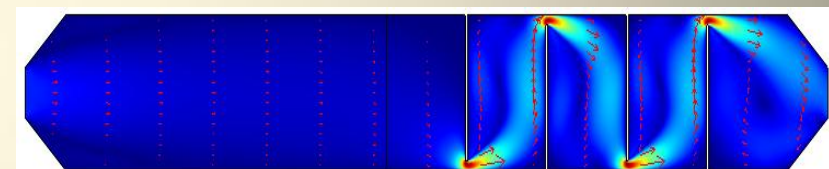
Thin rectangular obstacles



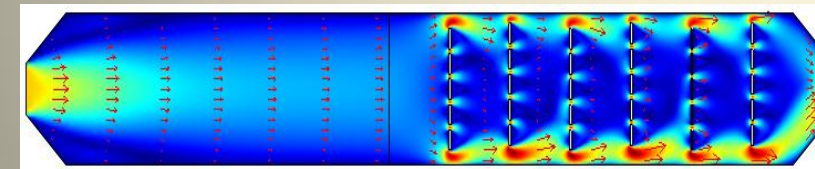
Baffles in flow path



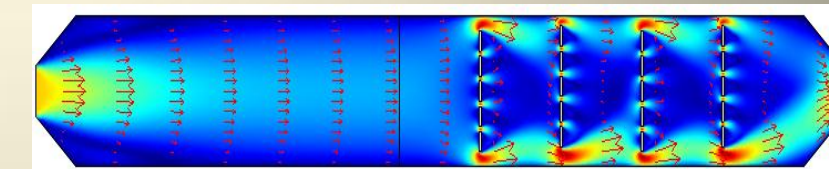
Baffles in flow path



Baffles in flow path



Mesh in flow path



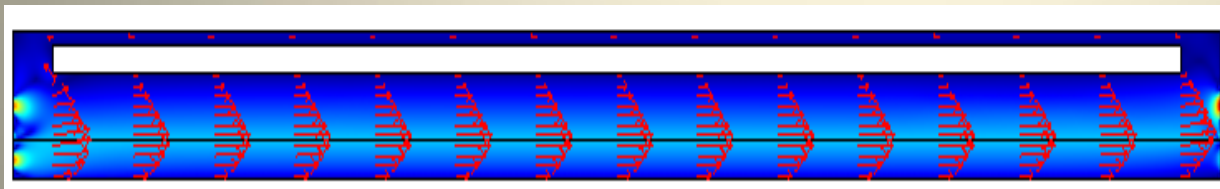
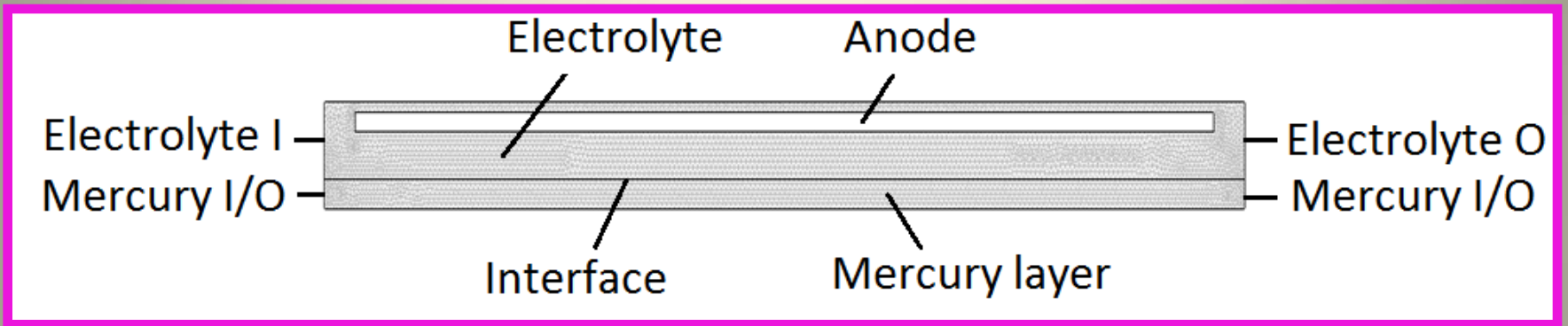
Mesh in flow path

Obstacles ensuring higher velocities close to anode and cathode (mesh type obstacles and baffles in the centre) may lead to better performance of electro-neutral bulk.

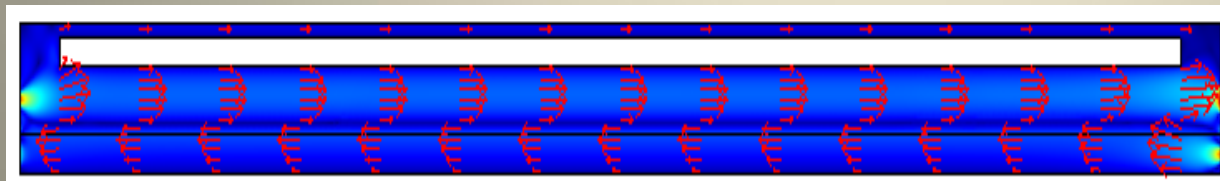
Numerical Simulation of Flow Electrolysers

Numerical Simulation of flow electrolyser with streaming mercury cathode

- *Comparison of co-current and counter-current configurations*
- *Effect of mercury flow rate*



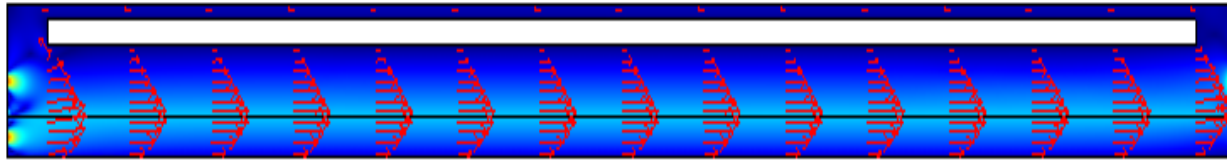
Current density 62691 (A/m²)



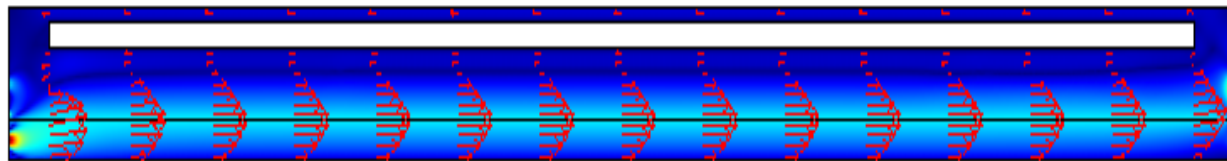
Current density 58785 (A/m²)

Numerical Simulation of Flow Electrolysers

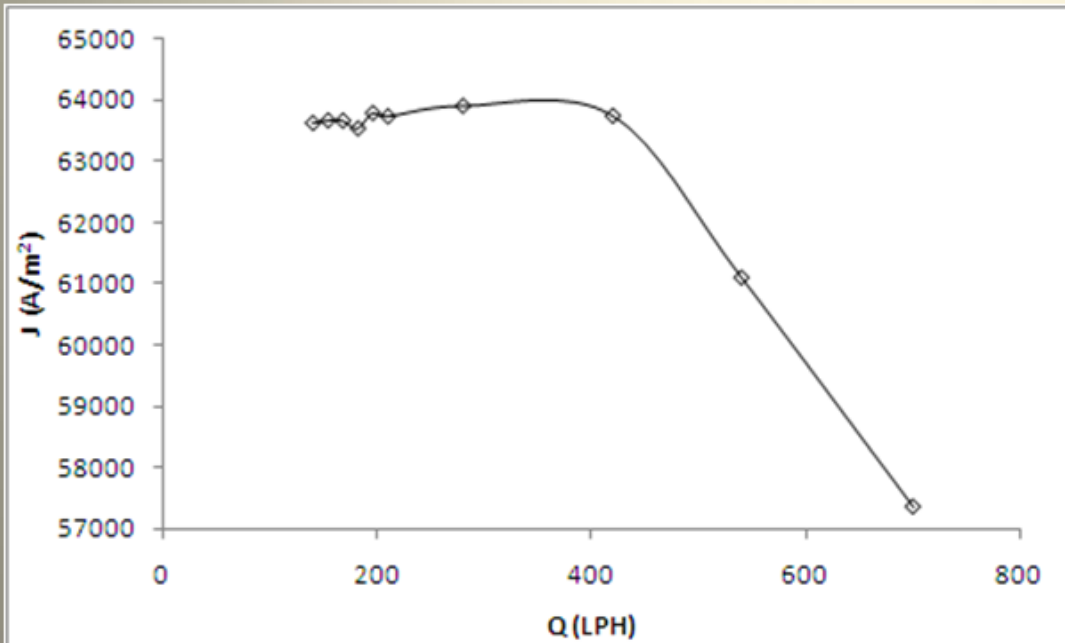
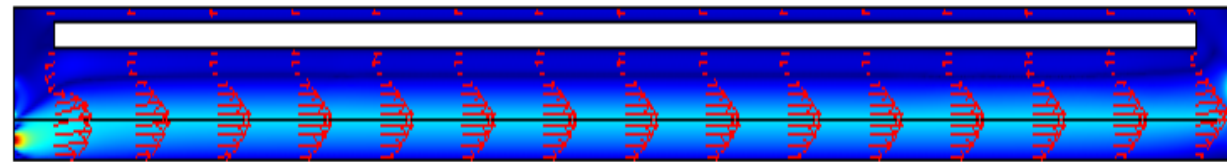
140 LPH



420 LPH



700 LPH



Current density reduces with continued increase in mercury flow rate

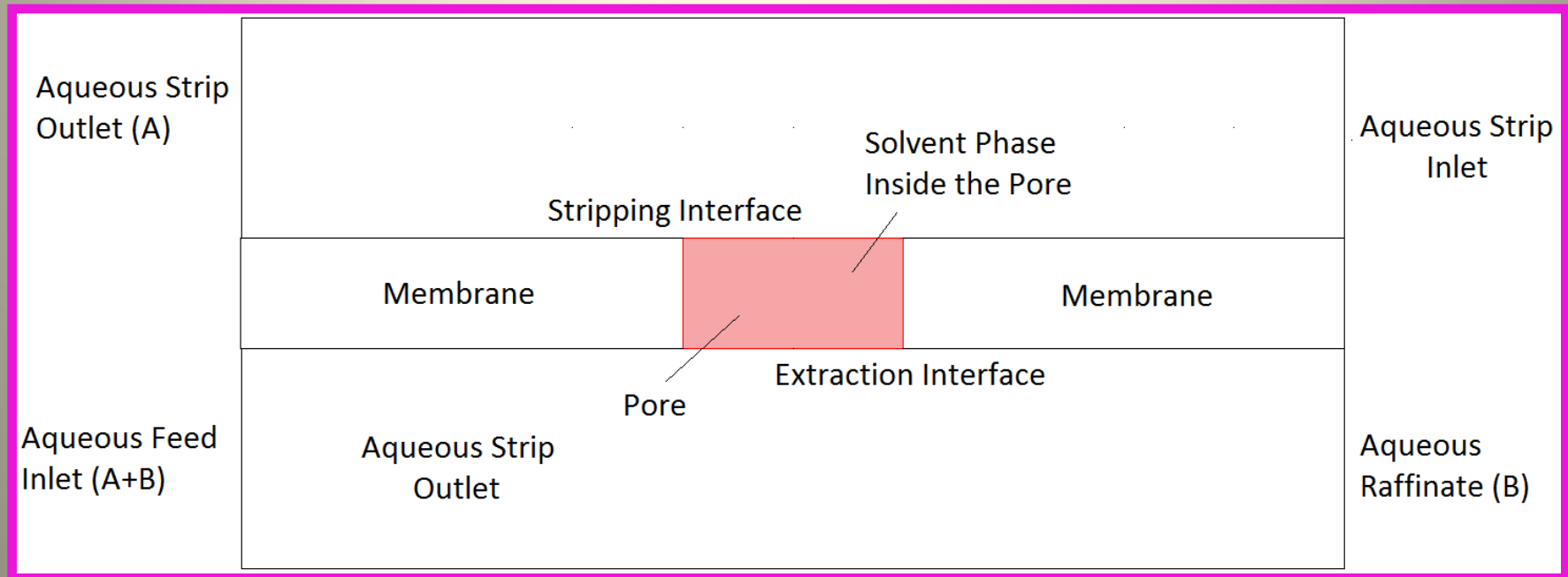
The study provided useful insights into the working of flow electrolysers having streaming mercury cathode

Mass Transfer In a Single Pore of SLM

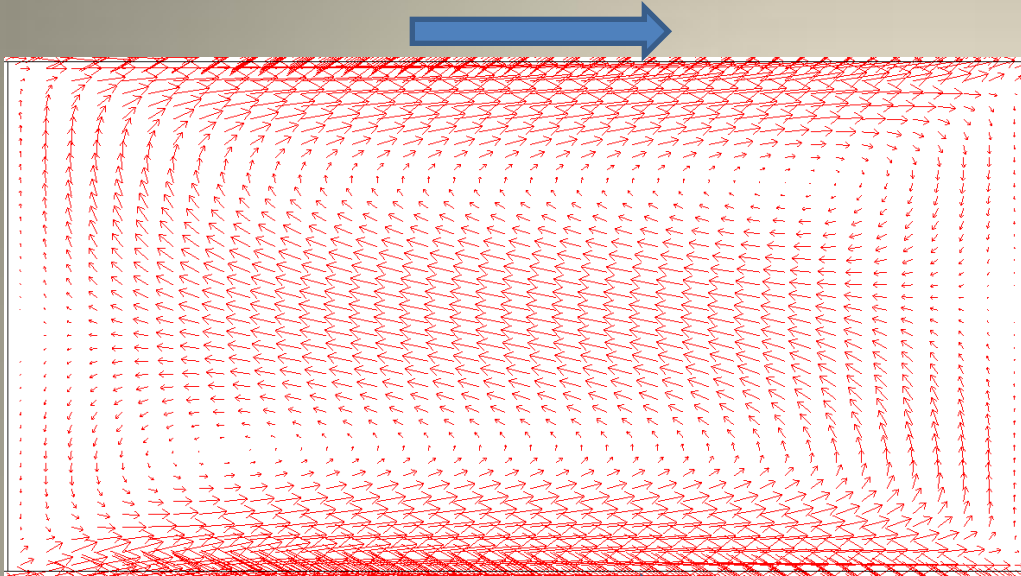
To develop understanding of mass transfer at pore level using numerical simulations and to understand the effects of

- **Flow direction**
- **Physical properties**
- **Pore size**

Coupled solution of Navier-Stokes and Convection-Diffusion equations

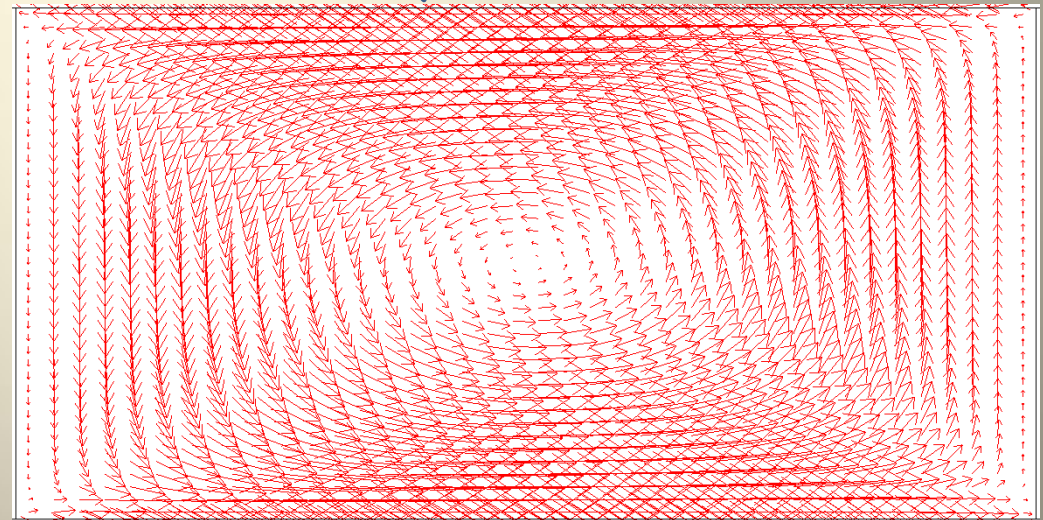
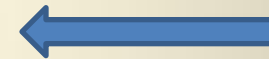
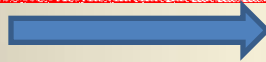


Mass Transfer In a Single Pore of SLM



Two circulation loops

Velocity vectors in the pore for co-current flow

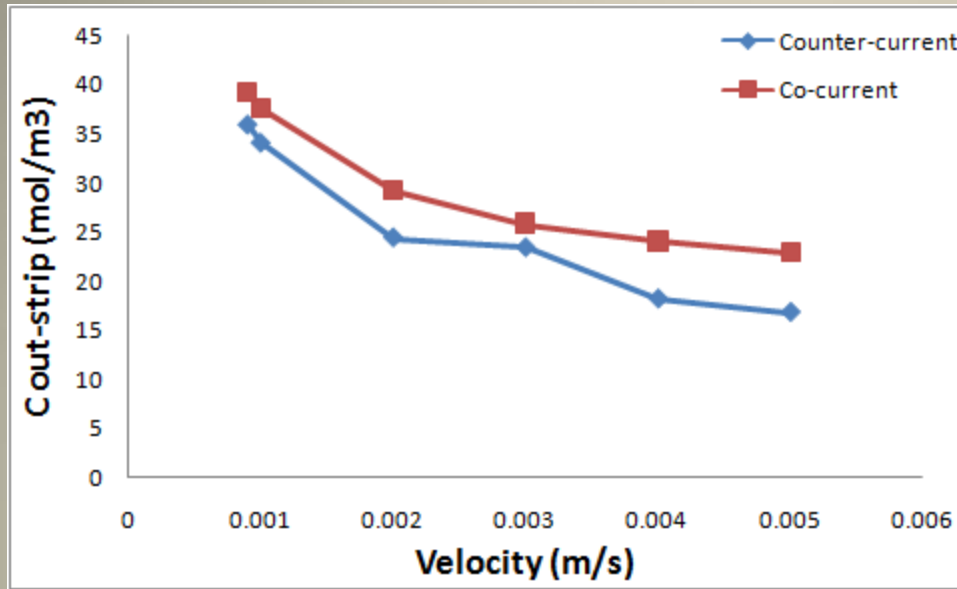


Single circulation loop

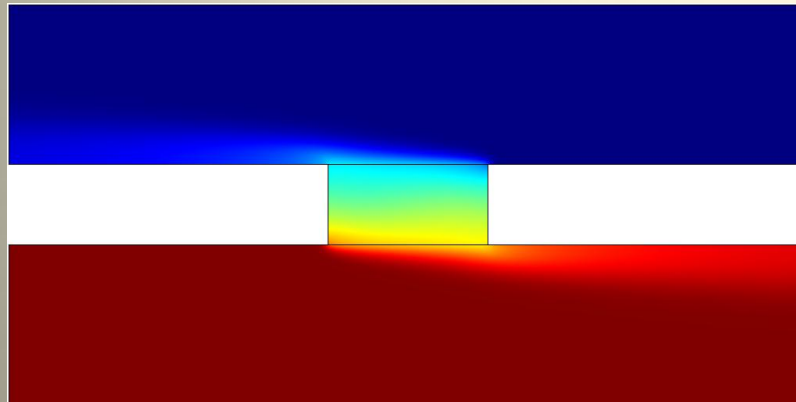
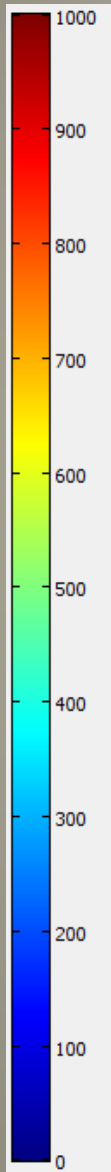
Velocity vectors in the pore for counter-current flow



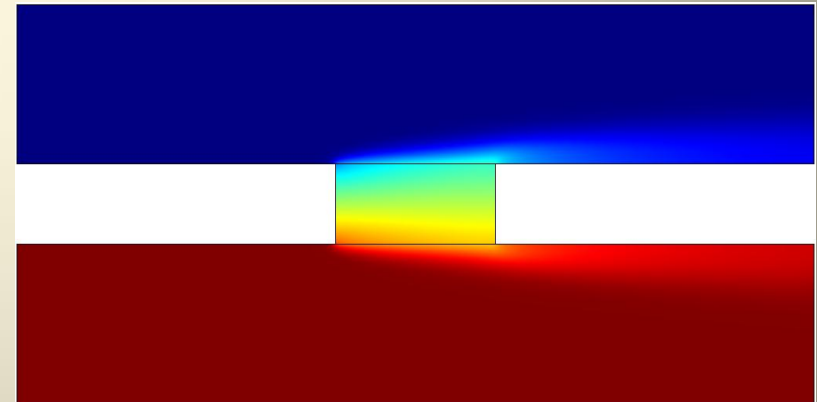
Mass Transfer In a Single Pore of SLM



The study led to an understanding of what happens at pore level in a supported liquid membrane



Counter-current flow



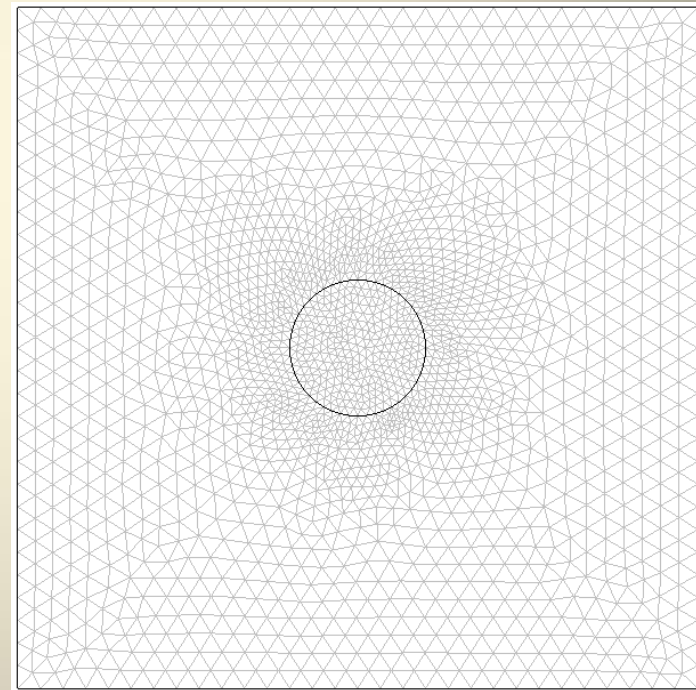
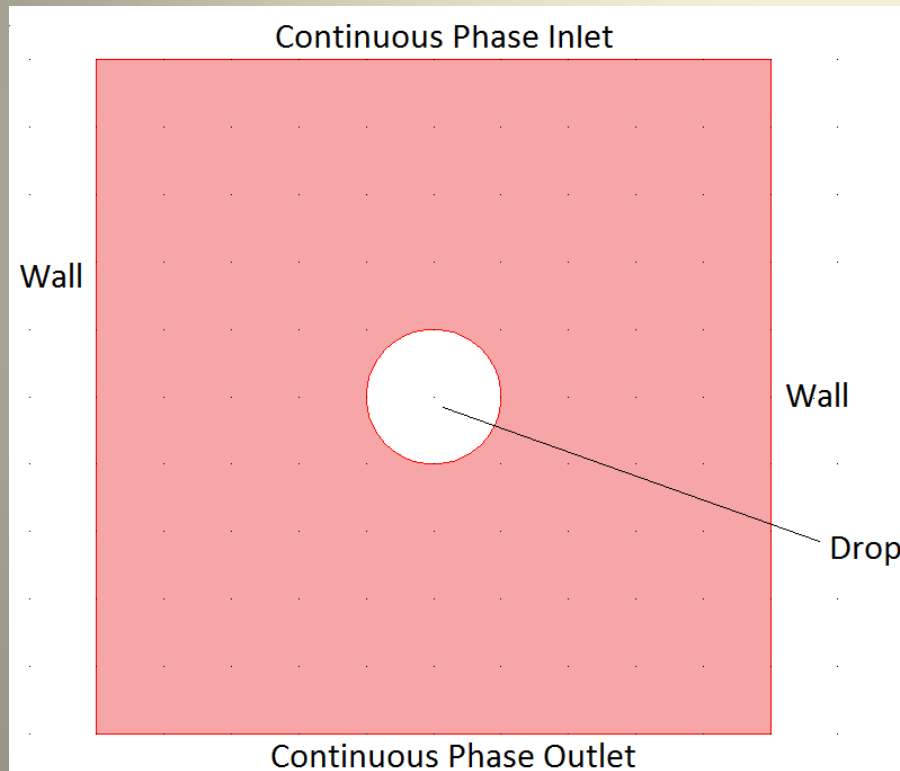
Co-current flow

Concentration contours

Mass Transfer For a Single Droplet

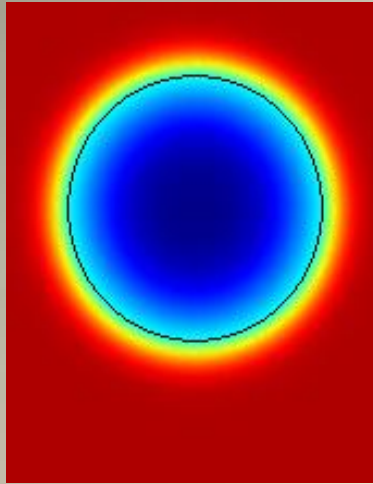
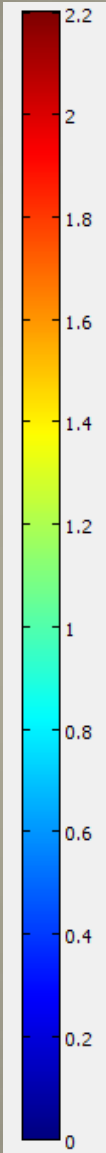
- **Effect of external flow field on internal recirculation inside a drop**
- **Effect internal recirculation on mass transfer rates**

Coupled solution of Navier-Stokes and Convection-Diffusion equations

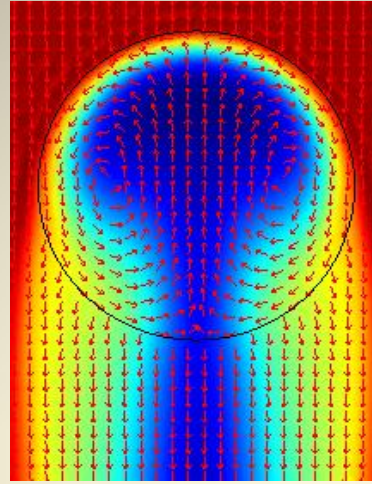


Features like identity boundary conditions etc. were used to implement appropriate boundary conditions at the interface.

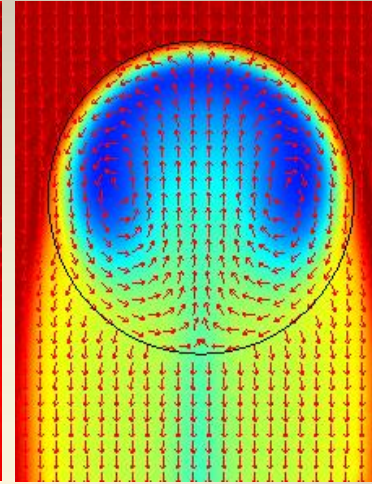
Mass Transfer for a Single Droplet



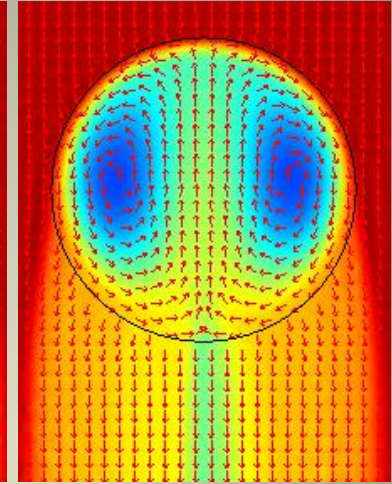
$V = 0.0$ m/s



$V = 0.0005$ m/s

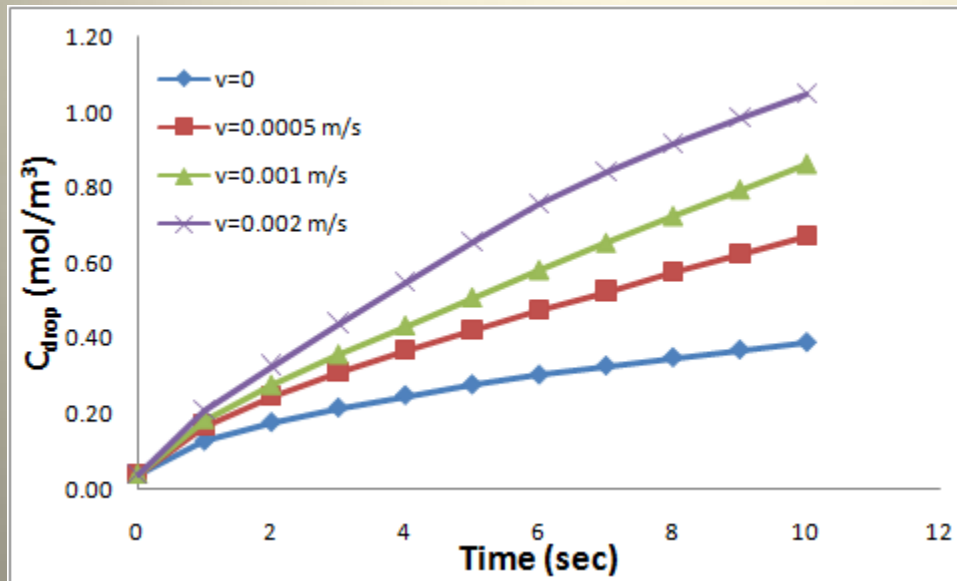


$V = 0.001$ m/s



$V = 0.002$ m/s

Contours of concentration inside the droplet for different velocities of the external phase



The study shows that internal circulation within a drop and its effect on mass transfer can be captured using simulations carried out in COMSOL multiphysics.

Conclusions

- ***Several interesting application of COMSOL Multiphysics to simulate two-phase flow and multiphysics problems have been presented.***
- ***In some cases results obtained from COMSOL have been quantitatively validated using the experimental data.***
- ***In other cases the results have been qualitatively validated.***
- ***COMSOL Multiphysics is found to be a very useful tool to gain insights into working of process equipment and phenomena involving two-phase flow and multiple physics.***

Acknowledgement

Mr. Nirvik Sen, Scientific Officer, Chemical Engineering Division, BARC

Drop formation at a single hole in a sieve plate

Ms. Pragati Shukla, Scientific Officer, Alkali Metal Section, BARC

Numerical simulation of flow electrolysers

THANKS