

Fluid-Thermal Analysis of an Air-Cooled Inverter with Laminar Flow

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The Problem

To design alternate configurations for a 55 kW inverter heat sink with laminar flow, utilizing the module designed for a cylindrical inverter with turbulent flow by Tawfik [5,6].

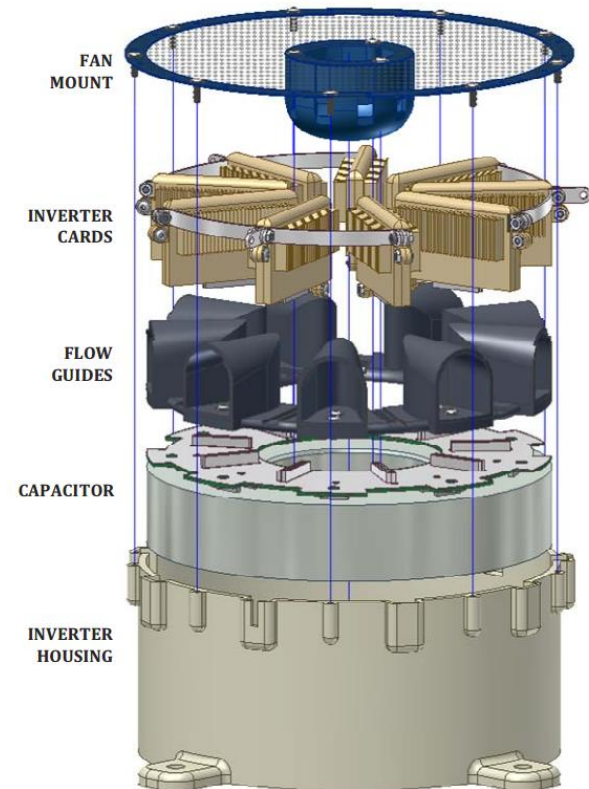
The alternate configurations should satisfy the same maximum temperature limit of 200 °C.

Differences:

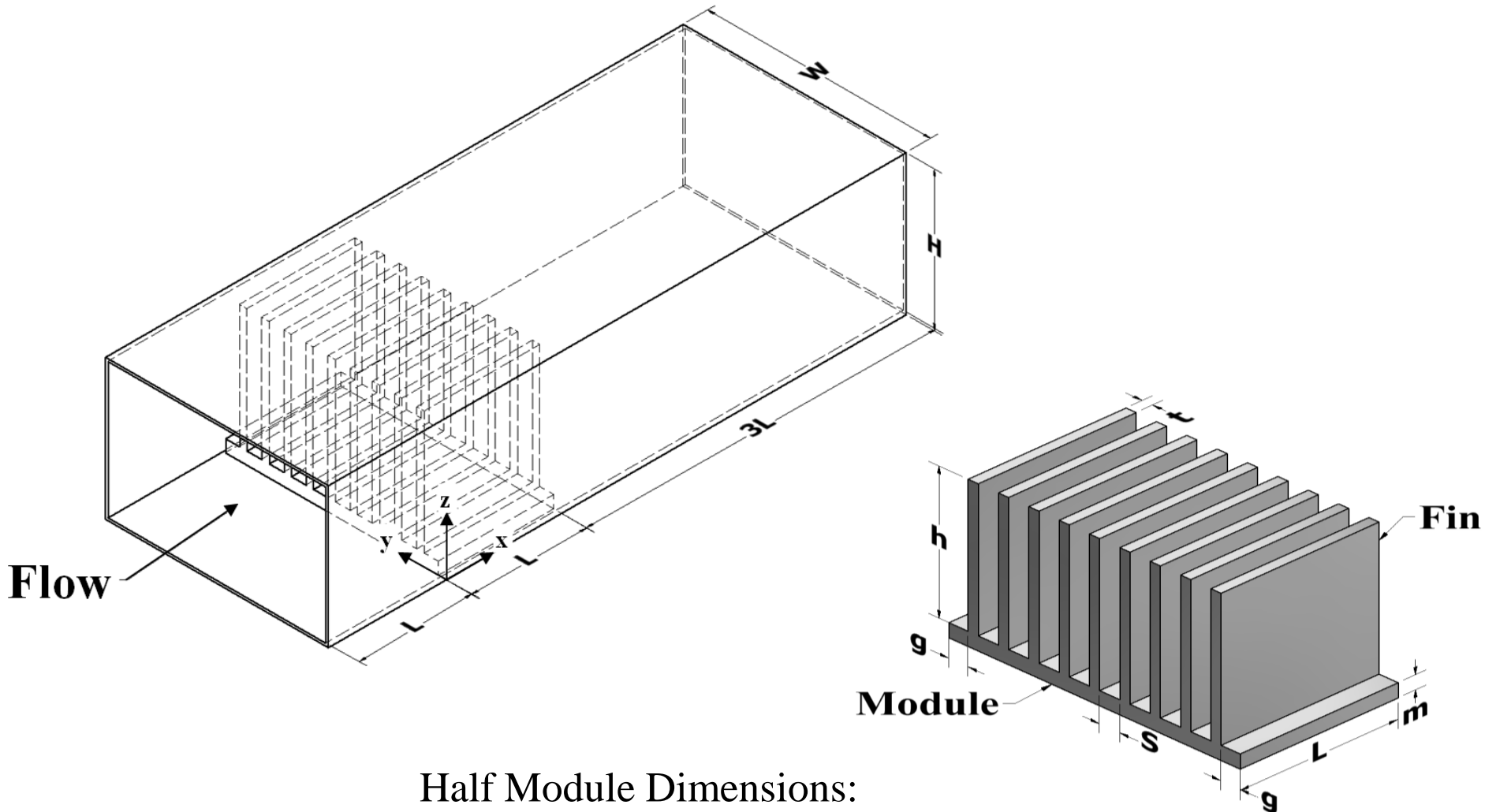
- Modules are in linear Configuration
- Laminar Flow

Similarities:

- Same Module size
- Same Generation Rate of 170 W



The Configuration



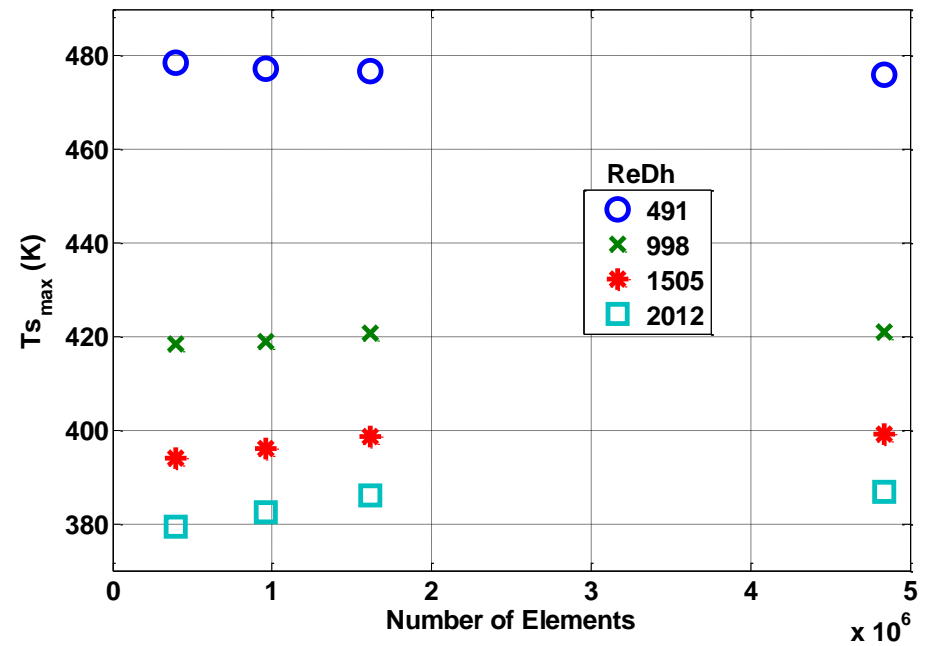
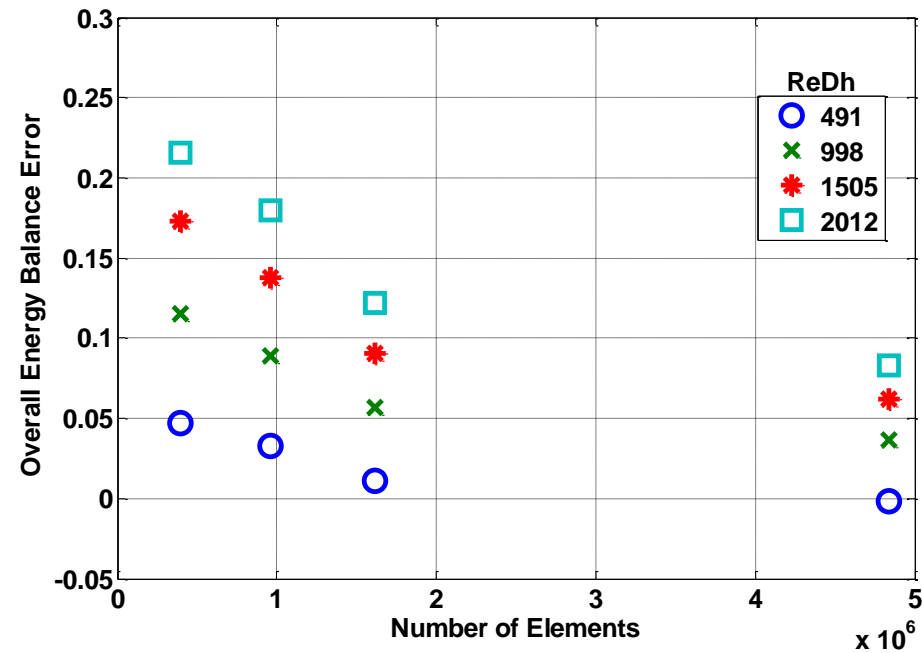
Half Module Dimensions:
 $W = 86.36 \text{ mm}$; $L = 46.84 \text{ mm}$; $m = 5 \text{ mm}$

Model Assumptions

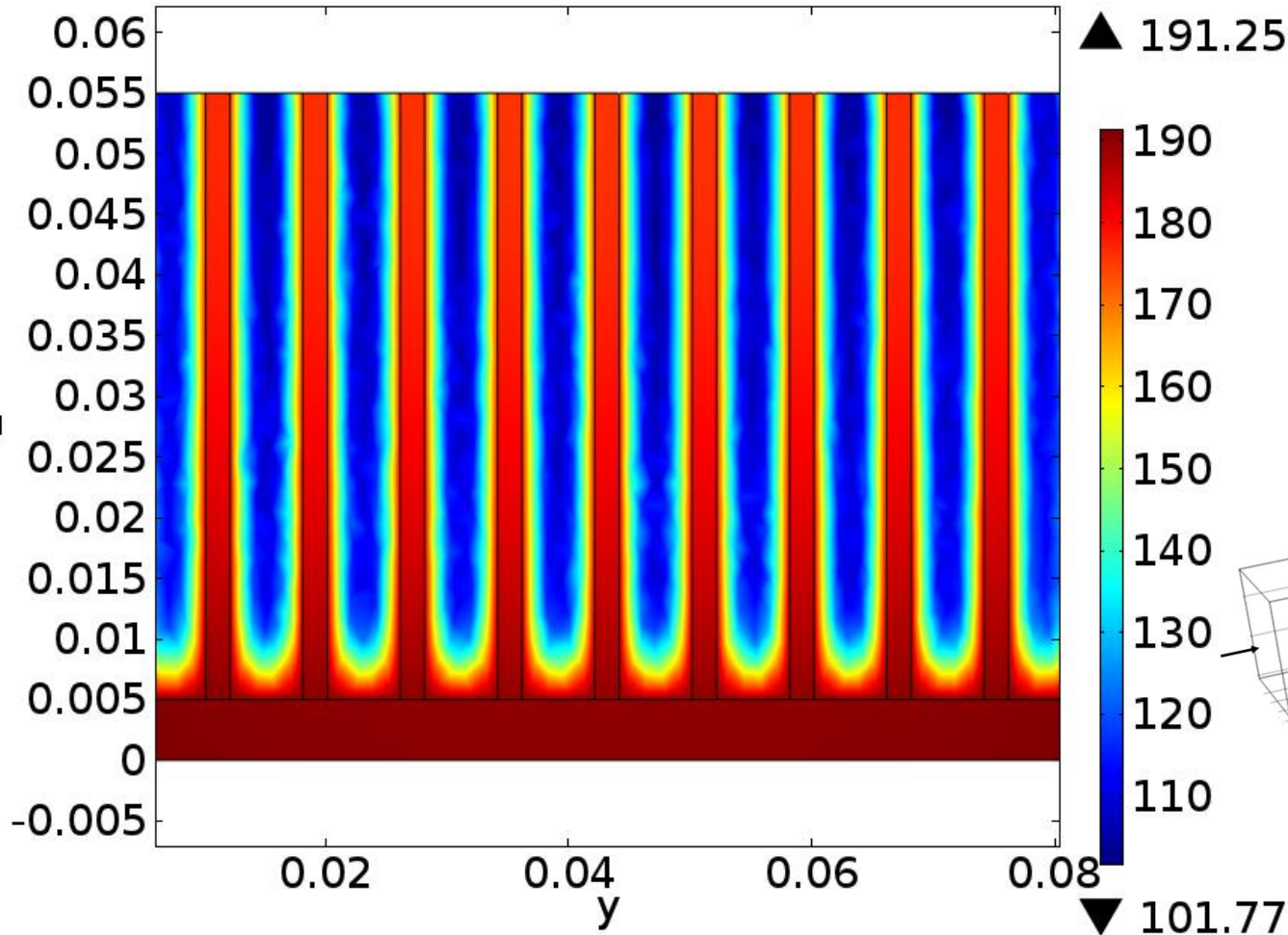
- Variable fluid properties for air from COMSOL material data base
- Constant aluminum properties from COMSOL material data base
- Half module internal generation rate 85.5 W
- Fin and module material: aluminum
- Inlet velocity calculated from specified inlet $ReDh$

Influence of Mesh Refinement on OEBE and $T_{s_{\max}}$

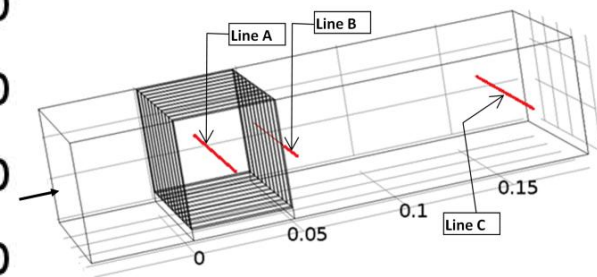
$t = 3 \text{ mm}$, $h = 50 \text{ mm}$, $s = 6 \text{ mm}$, $N_{\text{fins}} = 9$
Area (exposed to air) = $47,636 \text{ mm}^2$



Temperature Distribution in Y-Z Plane Through Line A (in °C)

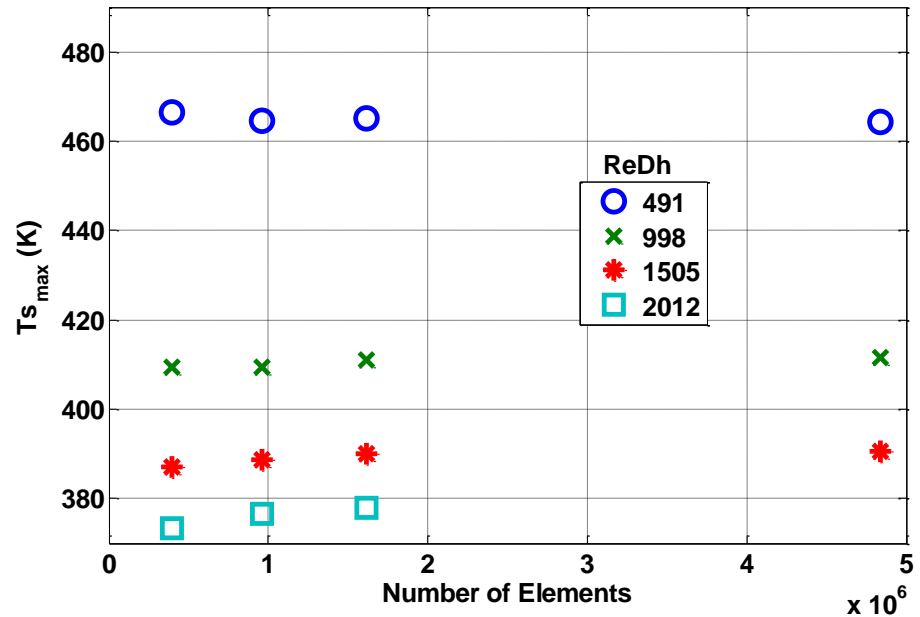
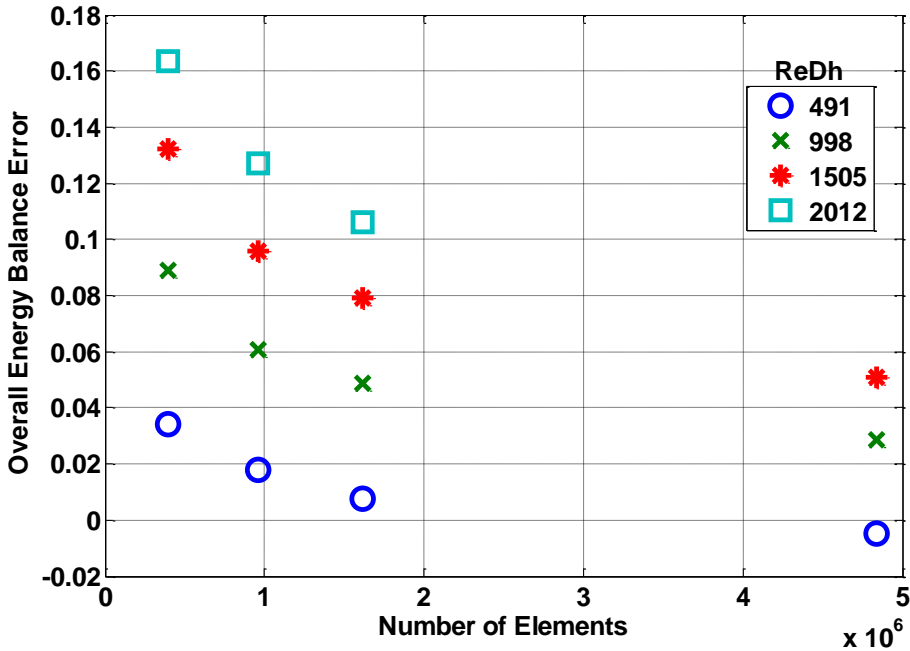


Module, Fins and Air Temperatures

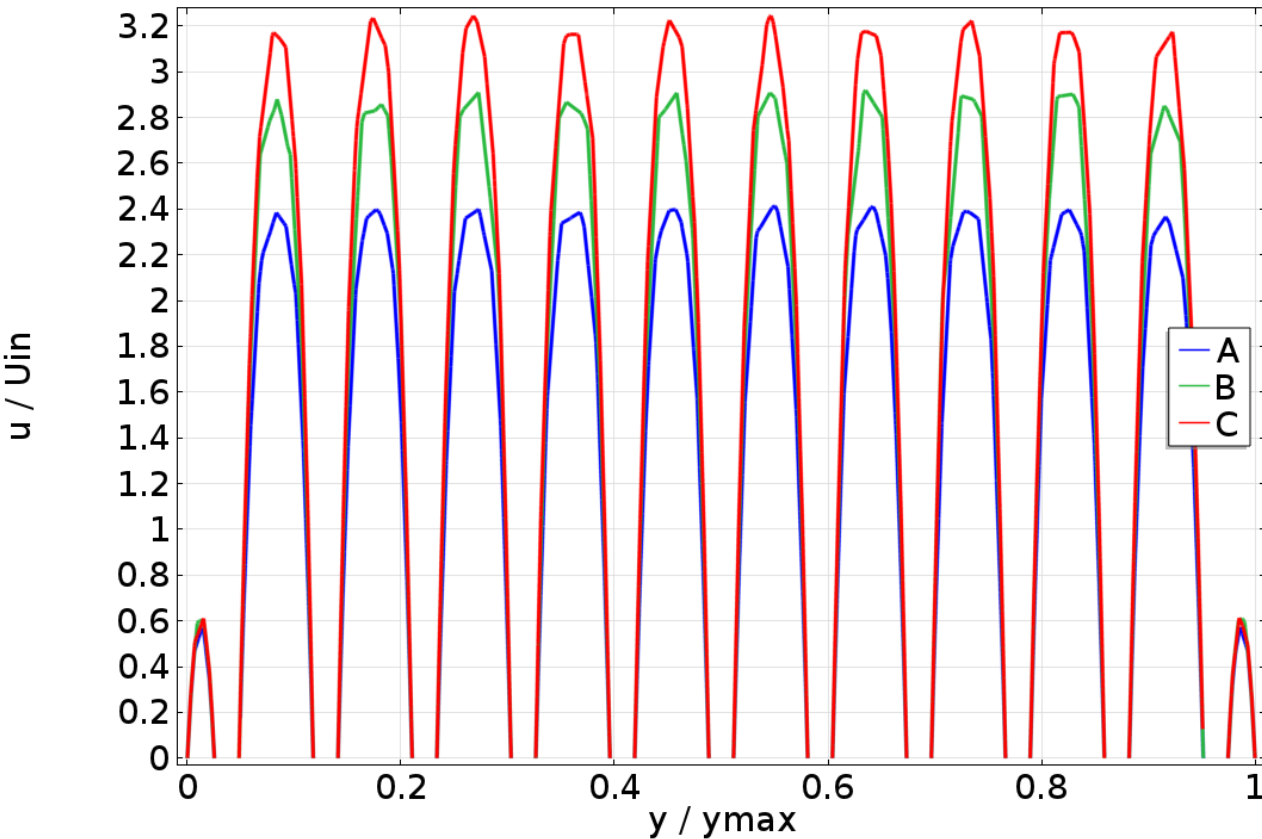


Influence of Mesh Refinement on OEBE and $T_{s_{\max}}$

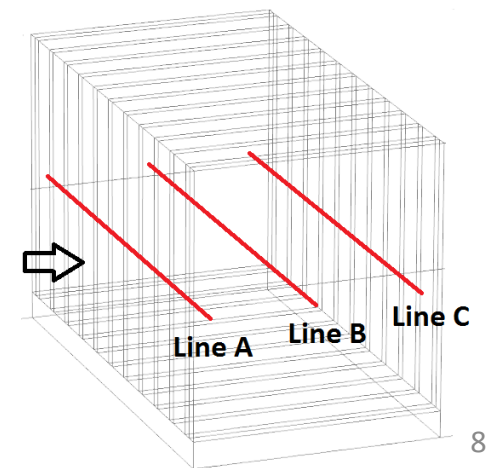
$t = 2 \text{ mm}$, $h = 50 \text{ mm}$, $s = 6 \text{ mm}$, $N_{\text{fins}} = 11$
Area = 56,738 mm²



Developing Flow in Channels



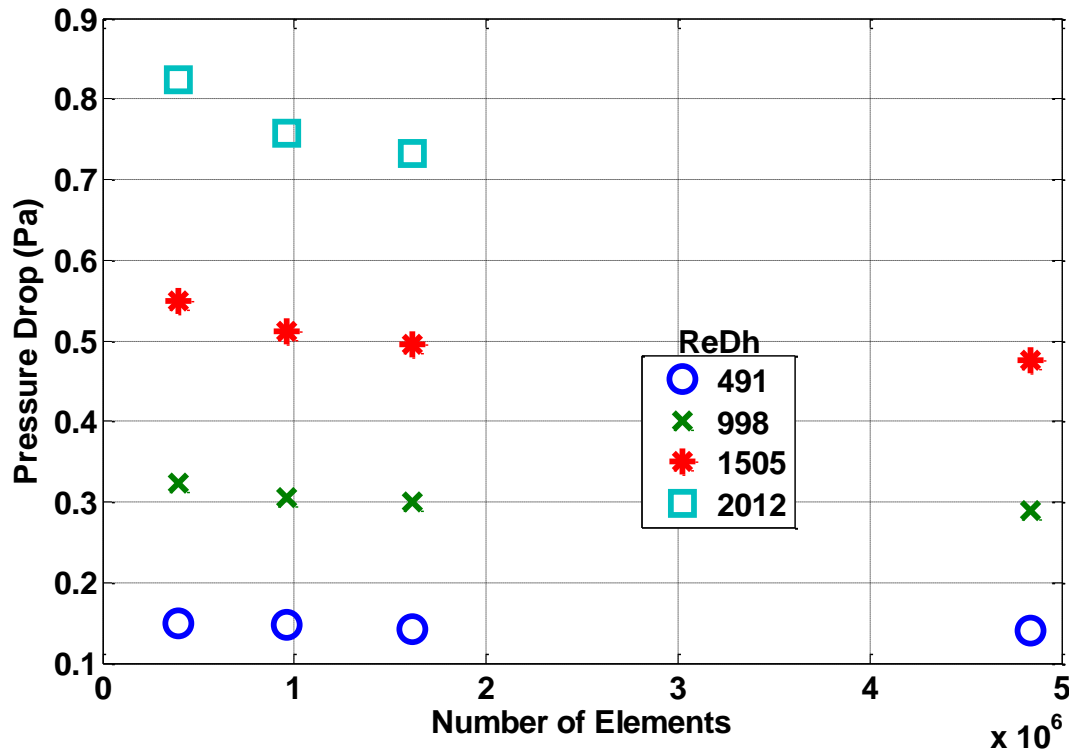
Re = 491
Fine mesh
h = 50 mm
s = 6 mm
t = 2 mm



Developing flows have higher heat transfer coefficients relative to fully developed flow.

Influence of Mesh Refinement on Pressure Drop

$t = 2 \text{ mm}$, $h = 50 \text{ mm}$, $s = 6 \text{ mm}$, $N_{\text{fins}} = 11$
Area = 56,738 mm²



Unlike $T_{s_{\text{max}}}$, the pressure drop is more sensitive to mesh refinement at higher $ReDh$.

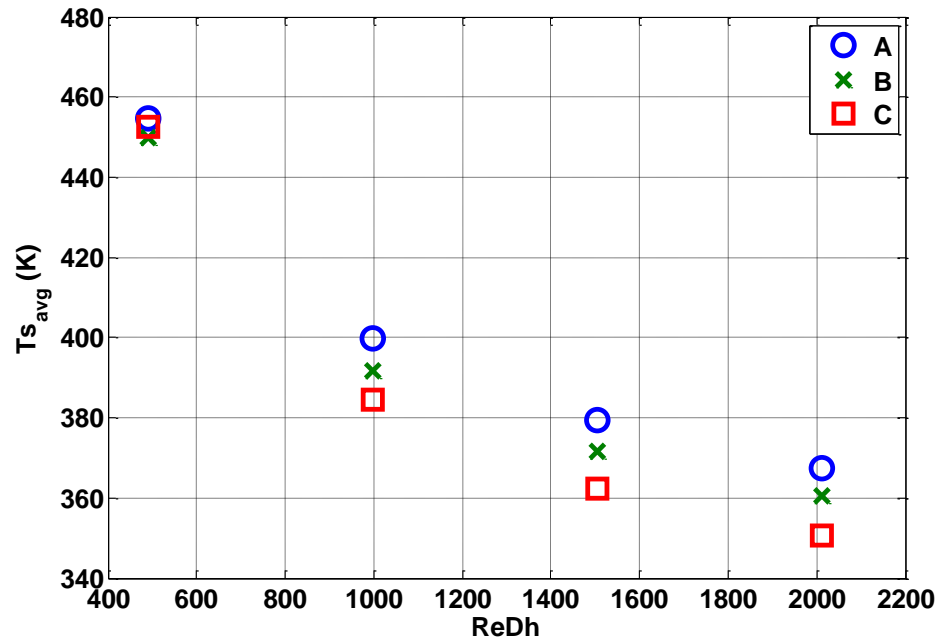
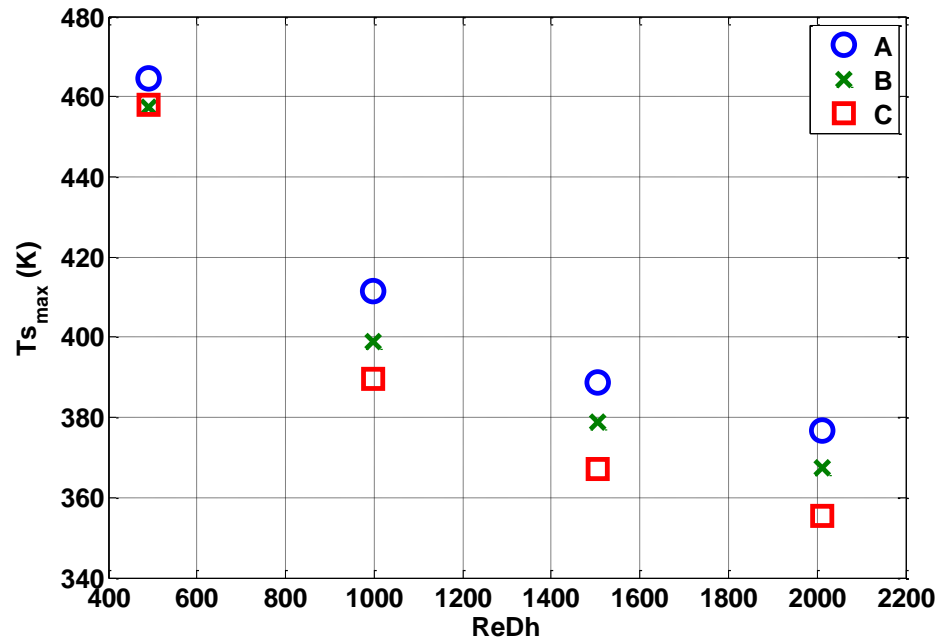
Selected Configurations for Further Study

To reduce overall volume, the fin height needs to be reduced while keeping the exposed area for heat transfer and $T_{s_{\max}}$ relatively unchanged.

This can be achieved by increasing the number of fins and reducing the spacing between them.

Case	t (mm)	h (mm)	s (mm)	N_{fins}	Area Exposed to Air (mm ²)
A	2	50	6	11	56,738
B	2	42	4.5	13	56,160
C	2	33	3	17	57,251

$T_{s_{max}}$ and $T_{s_{avg}}$ for Configurations A, B and C

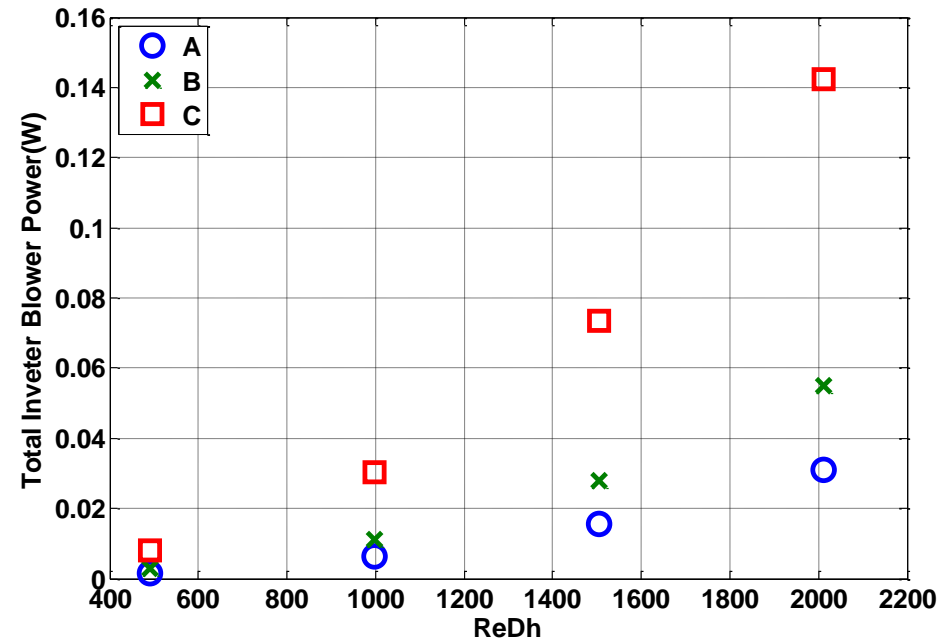
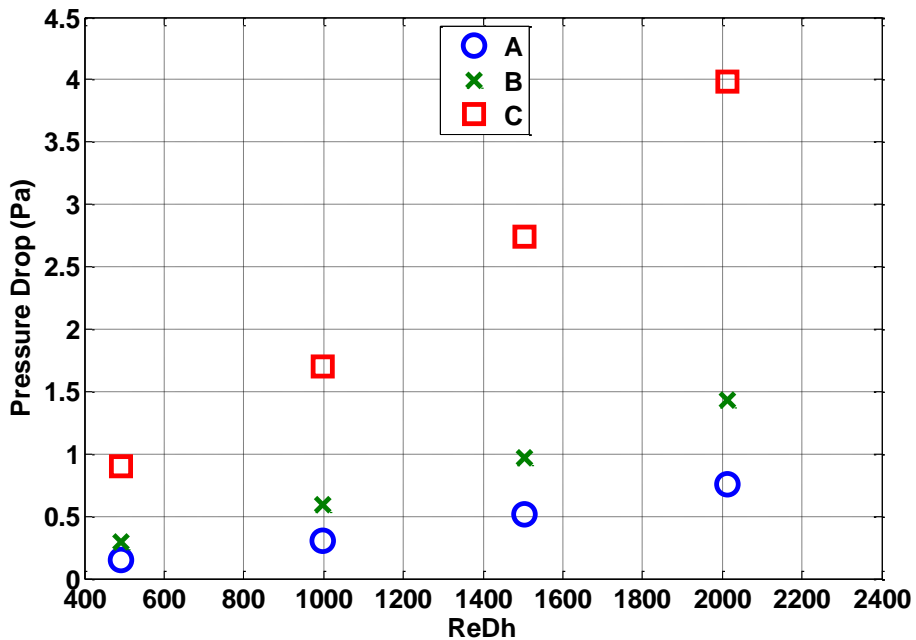


At any given $ReDh$, inlet velocity is increasing from A to C because of a decrease in hydraulic diameter.

Pressure Drop and Blower Power for Configurations A, B and C

Pressure Drop

Blower Power



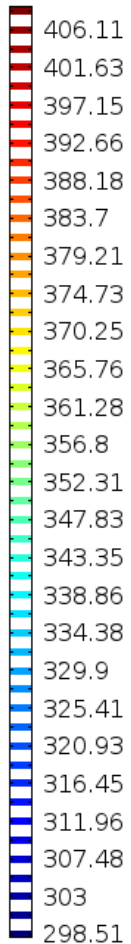
Conclusions

With laminar flow conditions it is shown that acceptable $T_{s_{\max}}$ values are achievable.

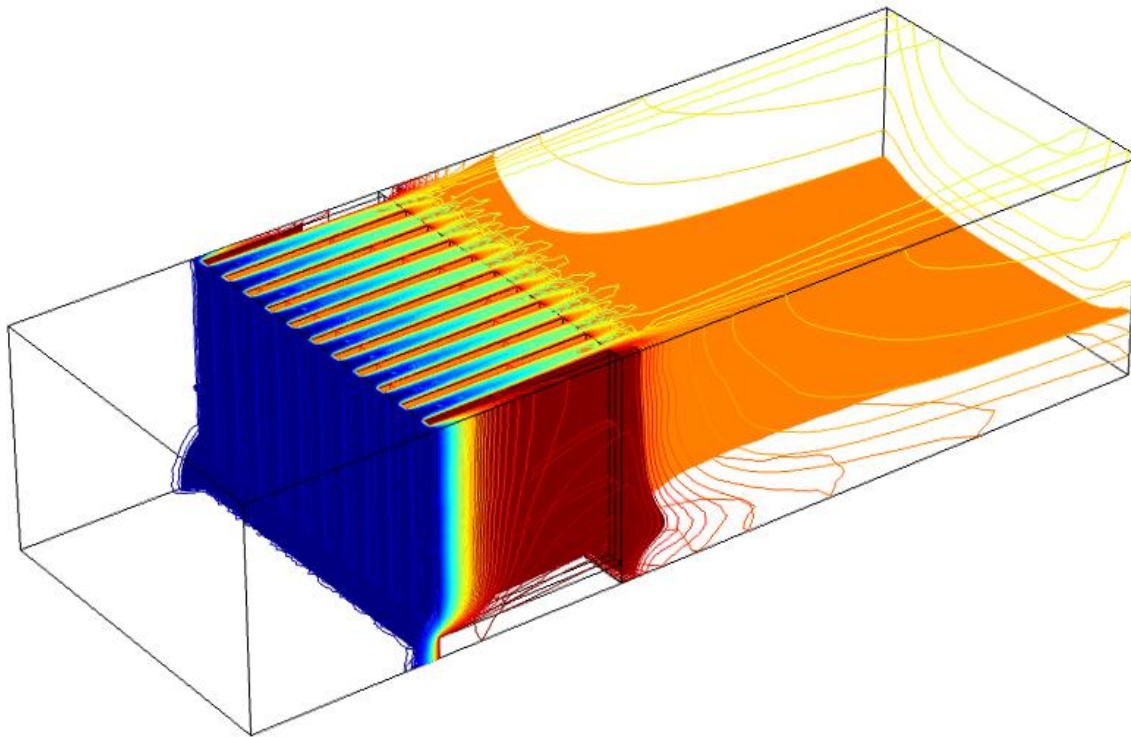
- $T_{s_{\max}}$ is less sensitive to mesh refinement.
- OEBE and pressure drop are much more sensitive to mesh refinement.
- Flow in the channels between fins is in the developing state for all Re_{Dh} considered.
- The overall volume was successfully reduced, while keeping the exposed area for heat transfer and $T_{s_{\max}}$ relatively unchanged.

Temperature Contours and Isosurfaces

▲ 408.35



▼ 298.51



$Re = 998$

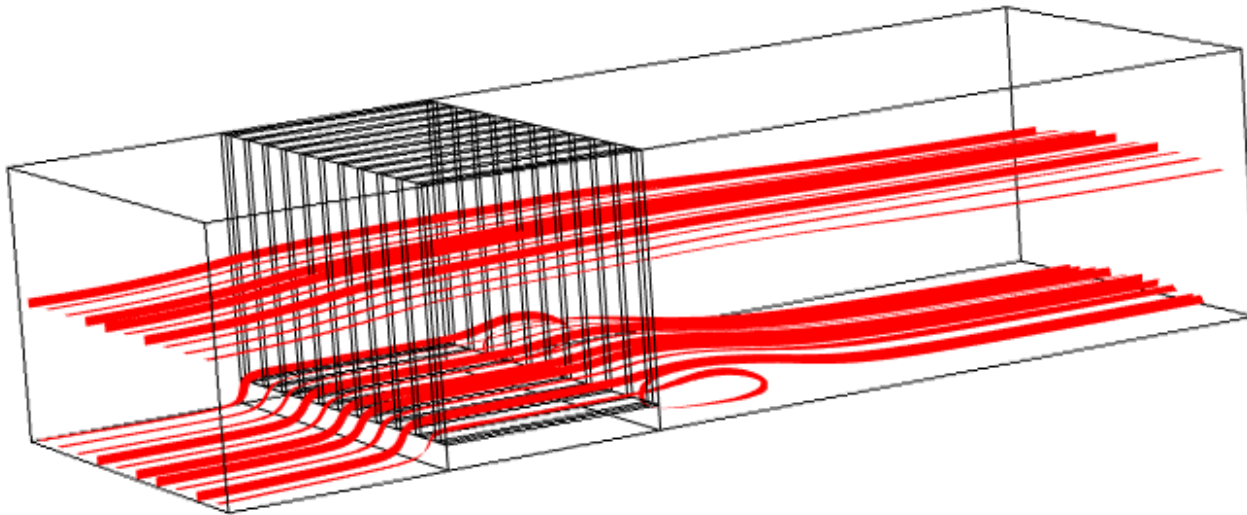
Normal mesh

$h = 50 \text{ mm}$

$s = 6 \text{ mm}$

$t = 2 \text{ mm}$

Streamlines



$Re = 491$

Fine mesh

$h = 50 \text{ mm}$

$s = 6 \text{ mm}$

$t = 2 \text{ mm}$