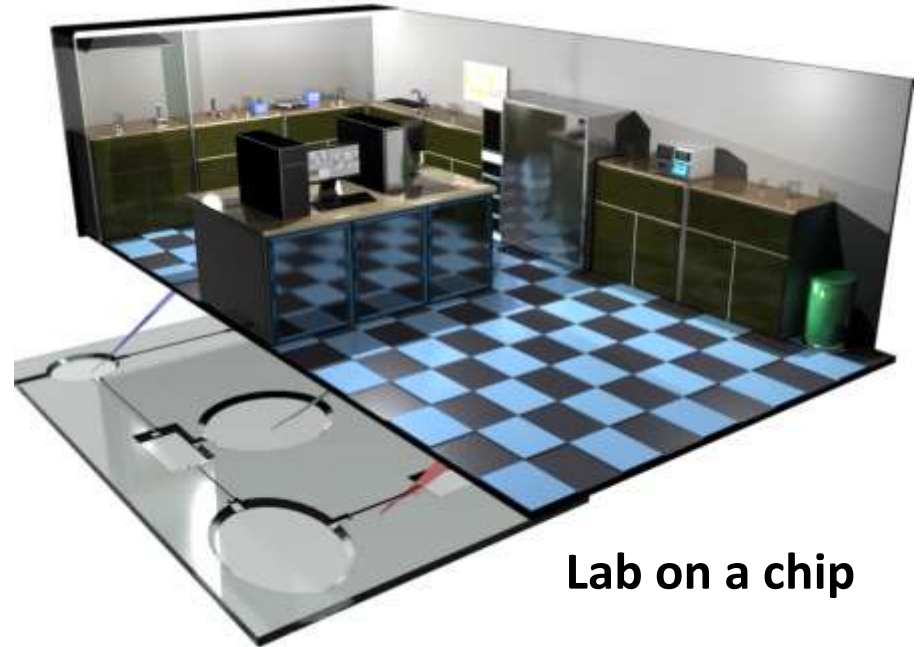


Mathematical Modeling of Electrokinetic Micropumps



INSTITUTE OF
CHEMICAL TECHNOLOGY
PRAGUE

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Department of Chemical Engineering, ICT Prague

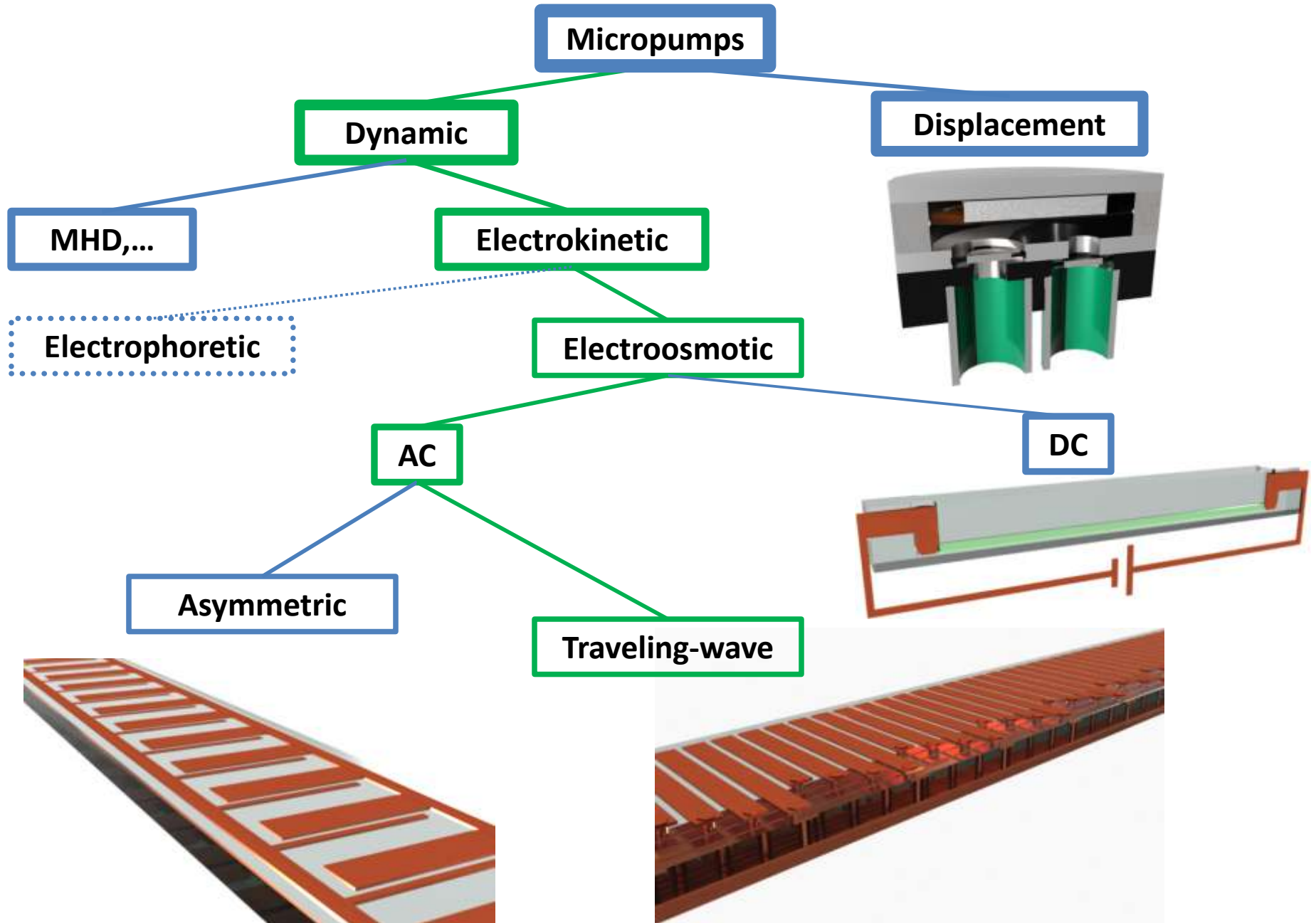


Lab on a chip

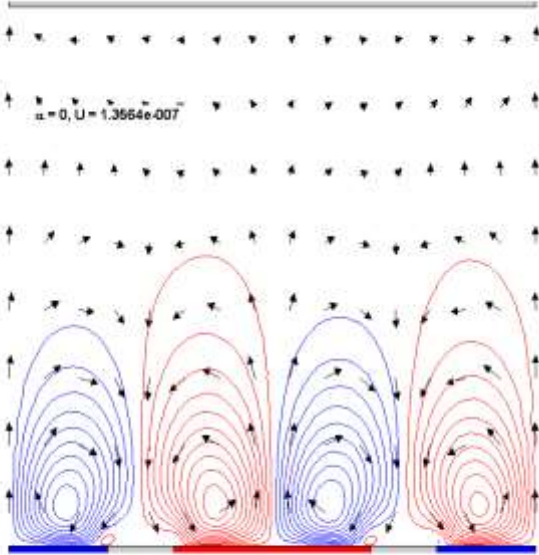
Outline

- ▣ **Pumping in micro- and nanoscale**
- ▣ **Interfacial phenomena and Electroosmotic flow**
- ▣ **Mathematical model equations**
- ▣ **Software implementation**
 - Model geometry and boundary conditions
 - Spatial discretisation and model solution
- ▣ **Results discussion**
 - Model quantities profiles
 - Velocity characteristics
- ▣ **Conclusions**

Pumping in micro- and nanoscale



Pumping in micro- and nanoscale

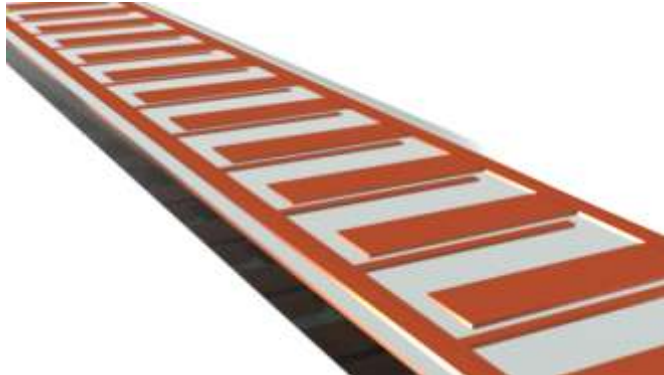


■ Symmetrical designs produce no net flow

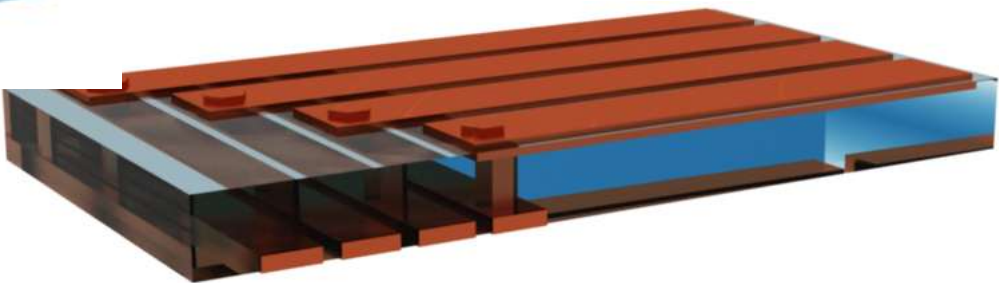
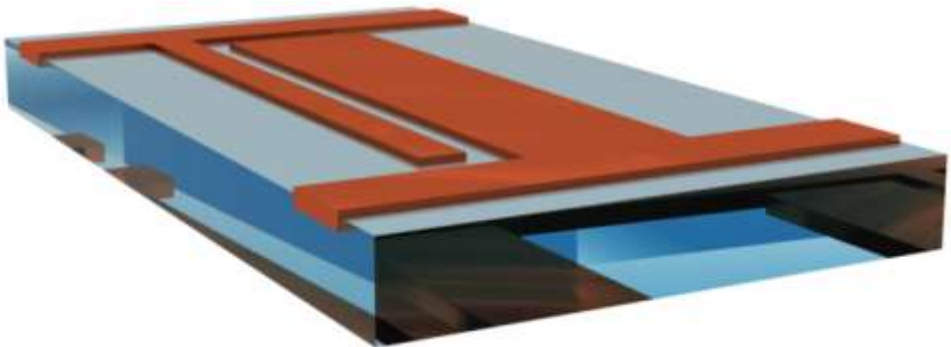
AC electro-osmotic

Asymmetric

Traveling-wave



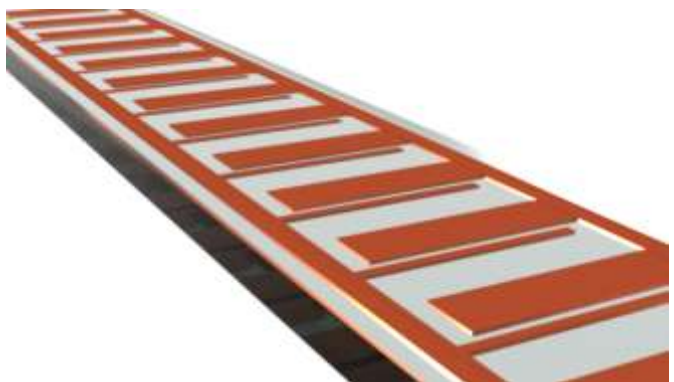
Pumping in micro- and nanoscale



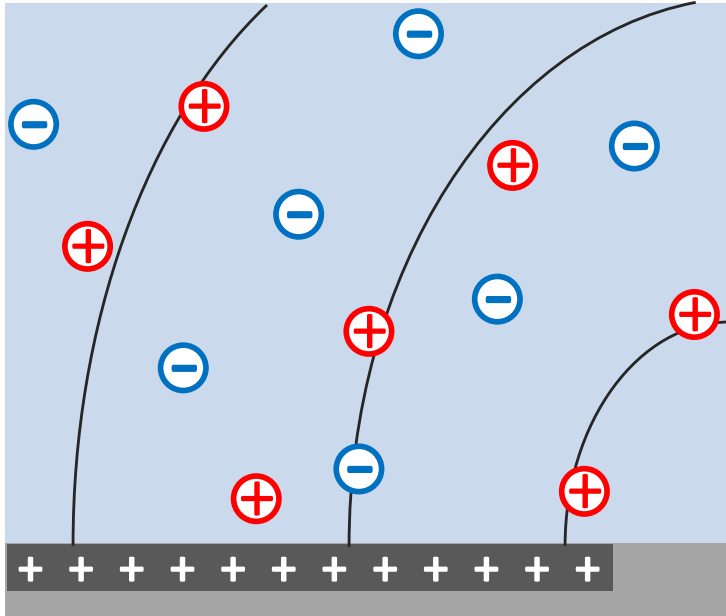
AC electro-osmotic

Asymmetric

Traveling-wave



Interfacial phenomena and Electroosmotic flow

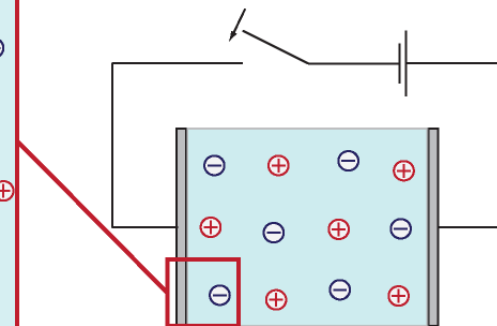
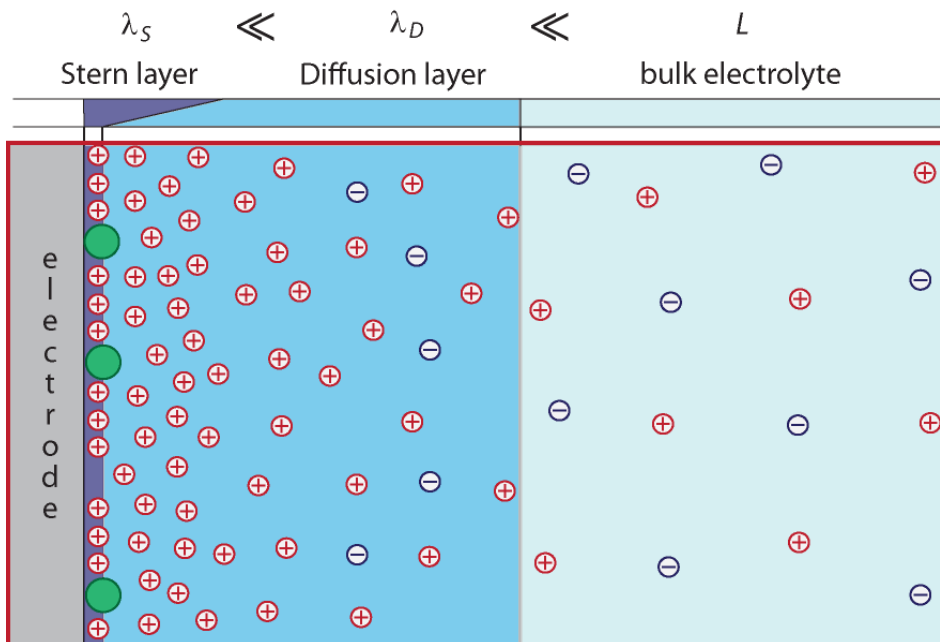


Normal component of the electric intensity vector

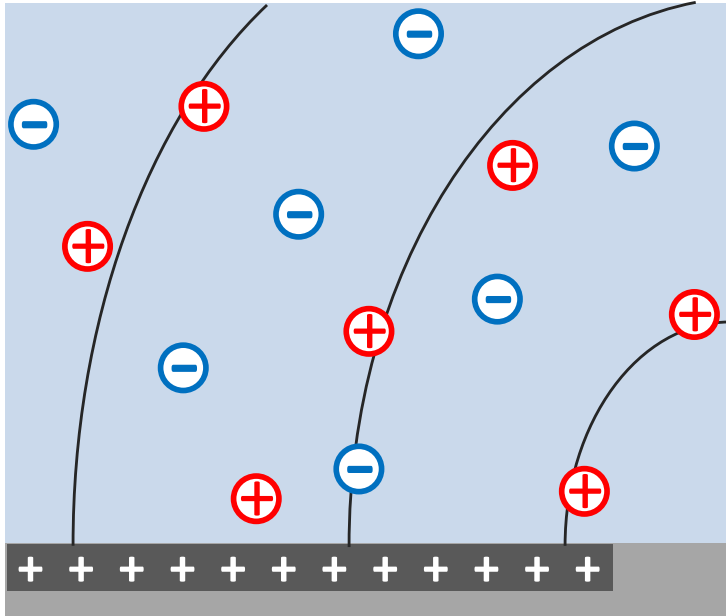
- ▣ Ions are attracted or repelled by the Coulombic force

$$f_e^\perp = qE^\perp = -q \frac{\partial \varphi}{\partial y}$$

- ▣ Ion concentrations change exponentially toward the charged wall.
- ▣ Coulombic force compete with diffusion
- ▣ There is non-zero charge density in electric double-layer, shielding



Interfacial phenomena and Electroosmotic flow

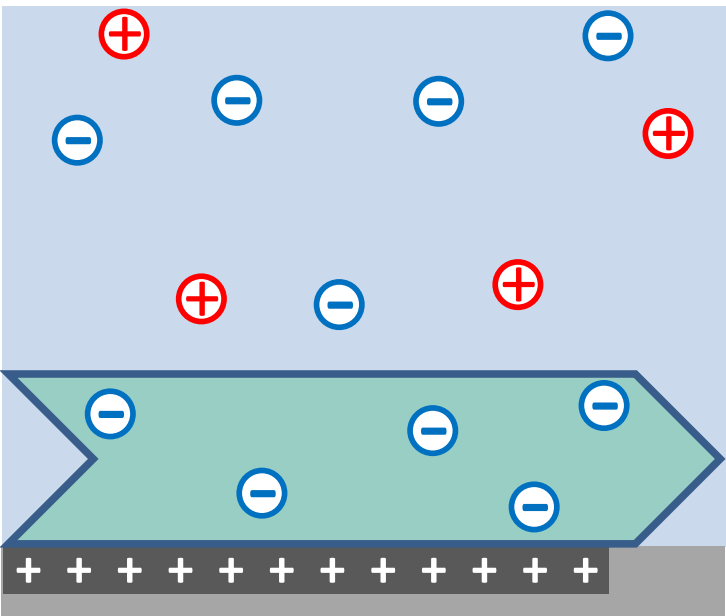


Normal component of the electric intensity vector

- Ions are attracted or repelled by the Coulombic force

$$f_e^\perp = qE^\perp = -q \frac{\partial \varphi}{\partial y}$$

- Ion concentrations change exponentially toward the charged wall.
- Coulombic force compete with diffusion
- There is non-zero charge density in electric double-layer, shielding



Tangential component of the electric intensity vector

- Accumulated ions are dragged by Coulombic force along the surface

$$f_e^\parallel = qE^\parallel = -q \frac{\partial \varphi}{\partial x}$$

- Momentum is transported into the electrolyte bulk via viscous forces

$$\mathbf{f}_\eta = -\nabla \cdot (-\eta \nabla \mathbf{v}) = \eta \nabla^2 \mathbf{v}$$

Mathematical model equations

Full model

Electrochemical problem

$$0 = -\tilde{\nabla} \cdot (\tilde{\nabla} \tilde{\varphi}) - \frac{\tilde{q}}{\tilde{\lambda}_D^2}$$

Poisson equation

$$\frac{1}{\tilde{\lambda}_D} \frac{\partial \tilde{c}}{\partial \tilde{t}} = -\tilde{\nabla} \cdot \left[\tilde{\mathbf{v}} \tilde{c} - \tilde{\nabla} \tilde{c} - \tilde{q} \tilde{\nabla} \tilde{\varphi} \right]$$

Local mass balances

$$\frac{1}{\tilde{\lambda}_D} \frac{\partial \tilde{q}}{\partial \tilde{t}} = -\tilde{\nabla} \cdot \left[\tilde{\mathbf{v}} \tilde{q} - \tilde{\nabla} \tilde{q} - \tilde{q} \tilde{\nabla} \tilde{\varphi} \right] - \frac{\tilde{q}}{\tilde{\lambda}_D^2}$$

Hydromechanical problem

$$\frac{1}{\tilde{\lambda}_D} \frac{1}{Sc} \frac{\partial \tilde{\mathbf{v}}}{\partial \tilde{t}} = -\tilde{\nabla} \tilde{p} - \tilde{\nabla} \cdot \left(\frac{\tilde{\mathbf{v}} \tilde{\mathbf{v}}}{Sc} - \tilde{\nabla} \tilde{\mathbf{v}} \right) - \frac{Ra}{\tilde{\lambda}_D^2} \tilde{q} \tilde{\nabla} \tilde{\varphi}$$

Navier-Stokes equation

$$0 = \tilde{\nabla} \cdot \tilde{\mathbf{v}}$$

Continuity equation

$$\tilde{\mathbf{x}} = (\tilde{x}, \tilde{y}) = (x/L, y/L), \quad \tilde{t} = \frac{t}{t_o}$$

$$\nabla_o = \frac{1}{L}, \quad \varphi_o = \frac{RT}{F}, \quad q_o = 2c_o F, \quad t_o = \frac{\lambda_D}{v_o}, \quad v_o = \frac{D}{L}, \quad p_o = \frac{v_o \eta_o}{L}$$

$$\tilde{\varphi} = \frac{\varphi}{\varphi_o}, \quad \tilde{c} = \frac{c^+ + c^-}{2c_o} - 1, \quad \tilde{q} = \frac{c^+ - c^-}{2c_o}, \quad \tilde{\mathbf{v}} = \frac{\mathbf{v}}{v_o}, \quad \tilde{p} = \frac{p}{p_o}$$

Mathematical model equations

Full model

Electrochemical problem

$$0 = -\tilde{\nabla} \cdot (\tilde{\nabla} \tilde{\varphi}) - \frac{\tilde{q}}{\tilde{\lambda}_D^2}$$

Poisson equation

$$\frac{1}{\tilde{\lambda}_D} \frac{\partial \tilde{c}}{\partial \tilde{t}} = -\tilde{\nabla} \cdot \left[\tilde{\mathbf{v}} \tilde{c} - \tilde{\nabla} \tilde{c} - \tilde{q} \tilde{\nabla} \tilde{\varphi} \right]$$

Local mass balances

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Hydromechanical problem

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Navier-Stokes equation

$$0 = \tilde{\nabla} \cdot \tilde{\mathbf{v}}$$

Continuity equation

Linearized model

$$\tilde{\nabla}^2 \tilde{\psi} = 0, \quad \tilde{\nabla}^2 \hat{\tilde{\mathbf{v}}} = \tilde{\nabla} \hat{\tilde{p}}, \quad \tilde{\nabla} \cdot \hat{\tilde{\mathbf{v}}} = 0$$

Laplace and Stokes equation

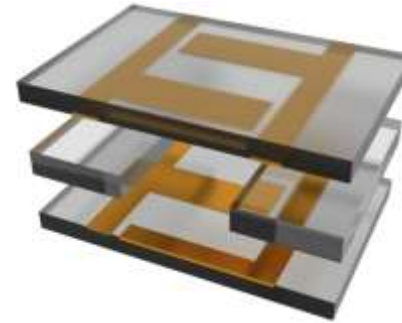
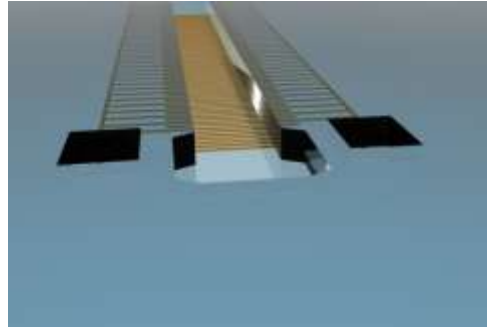
$$\frac{\partial \tilde{\psi}}{\partial \tilde{y}} = +i (\tilde{\psi} - \tilde{\psi}_m), \quad \frac{\partial \tilde{\psi}}{\partial \tilde{y}} = -i (\tilde{\psi} - \tilde{\psi}_m), \quad \frac{\partial \tilde{\psi}}{\partial \tilde{y}} = 0$$

RC boundary conditions

$$\frac{\hat{u}}{Ra} = \frac{1}{2} \Re \left[(\tilde{\psi} - \tilde{\psi}_m) \frac{\partial \tilde{\psi}^*}{\partial \tilde{x}} \right]$$

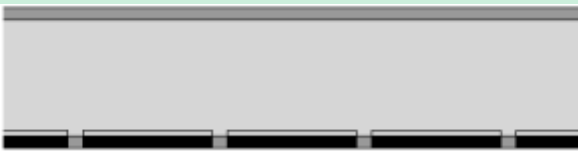
Helmholtz-Smoluchowski equation

Model geometry and boundary conditions



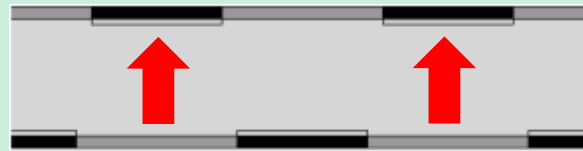
An assumption of the system-properties periodicity implies the periodicity in electrode array

variant 5-0



Bottom arrangement

variant 3-2



Shift of even electrodes

variant 3-2 with overlap



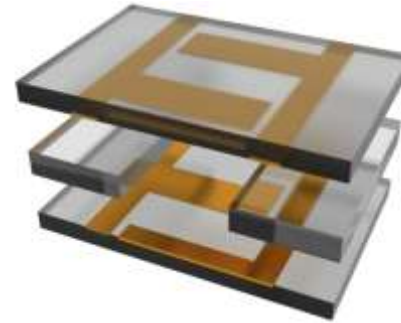
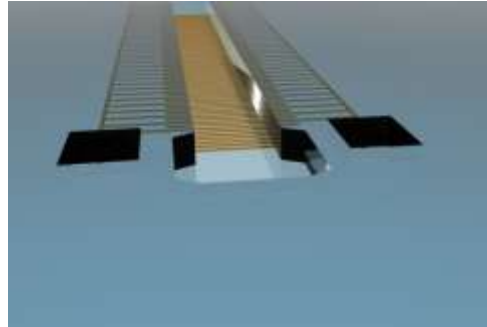
Extended electrodes

Electrode overlap brings new quality to model behavior

The boundary conditions and initial approximation

- ▣ Four-phase arrays require more than one construction layer (x spiral design)
- ▣ The more surface is covered by electrodes, the stronger is fluid flow
- ▣ Flow reversal seems to be generic feature of zig-zag arrangement

Model geometry and boundary conditions

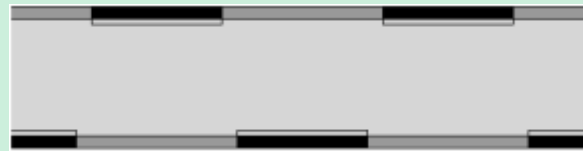
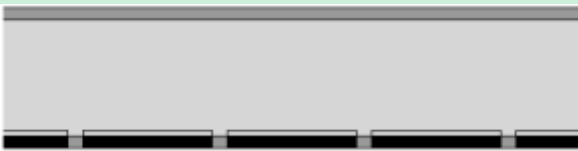


An assumption of the system-properties periodicity implies the periodicity in electrode array

variant 5-0

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variant 3-2 with overlap



Bottom arrangement

Shift of even electrodes

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The boundary conditions and initial approximation

Electrode surfaces

$$\varphi_i = A \sin \left(\omega t + i \frac{2\pi}{n} \right), \quad i = 0, 1, 2, 3$$

Left and right margin (periodicity)

$$\begin{aligned} \xi(x, y, t) &= \xi(x + L, y, t) \\ \xi &= \{ \varphi, c^\pm, \mathbf{v}, p \} \end{aligned}$$

Solid-electrolyte interface

$$\mathbf{n} \cdot \mathbf{J}^\pm = 0, \quad \mathbf{n} \cdot \nabla \varphi = 0, \quad \mathbf{v} = (0, 0)$$

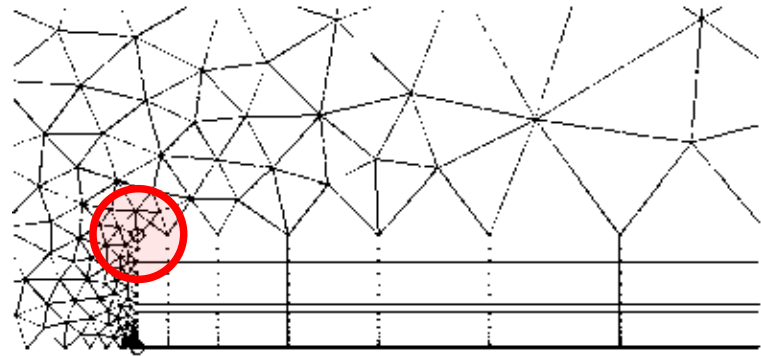
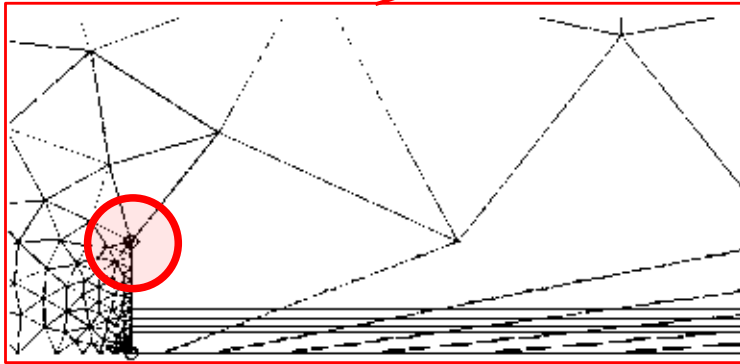
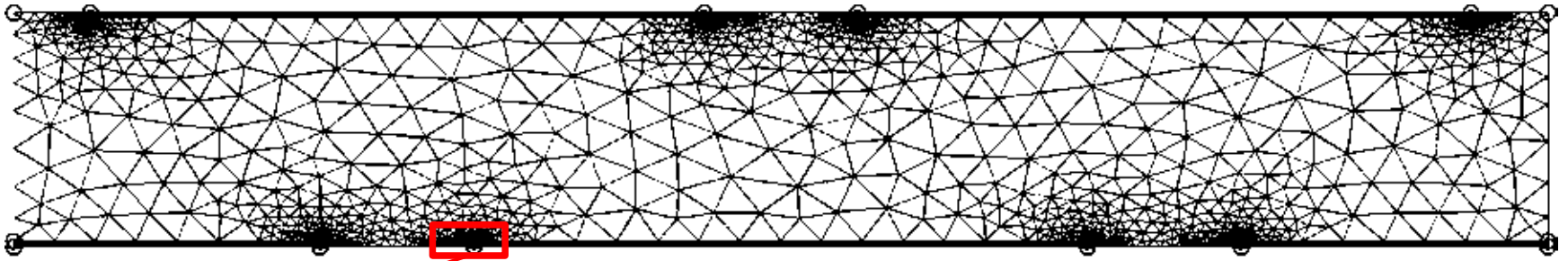
Initial approximation

$$\varphi(0, x, y) = 0, \quad c^+(0, x, y) = c^-(0, x, y) = c_0$$



Spatial discretization and model solution

Hybrid discretization mesh

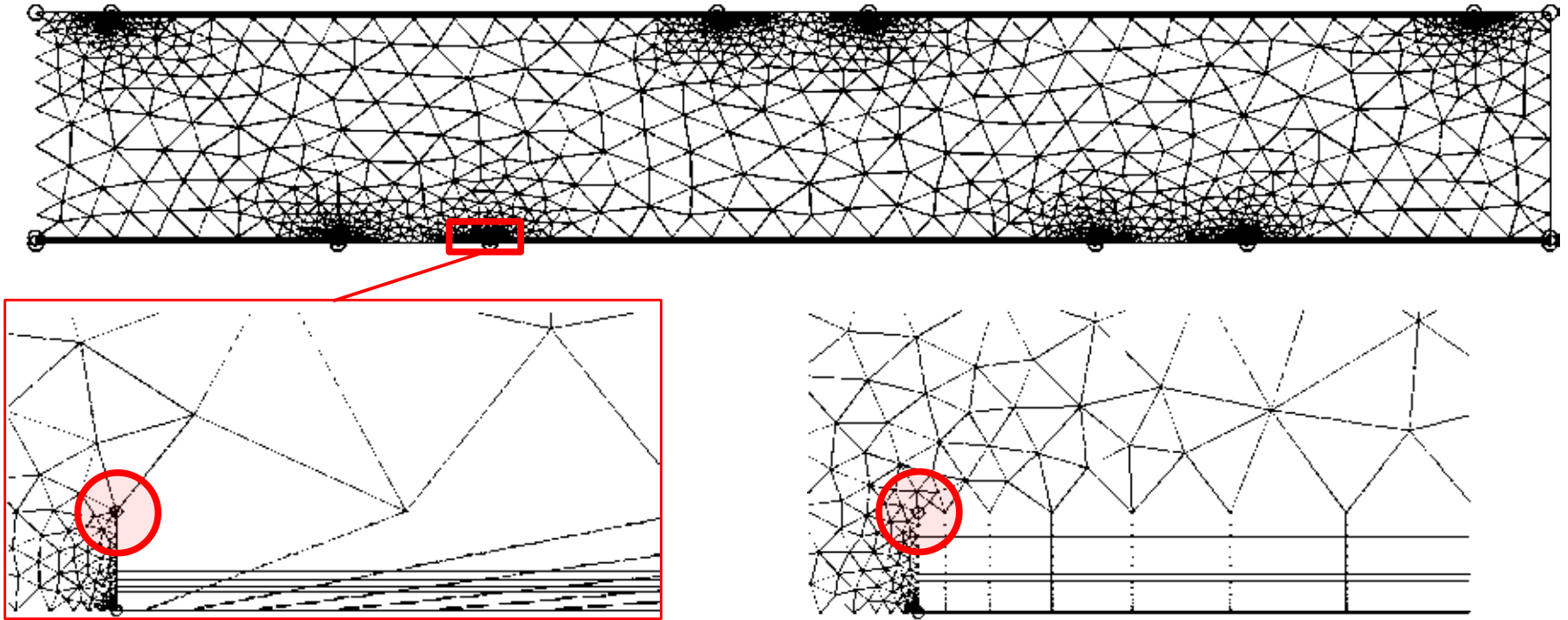


An advantage of skewed quadrilateral mesh

- Suppress element densification above the electrode corners

Spatial discretization and model solution

Hybrid discretization mesh

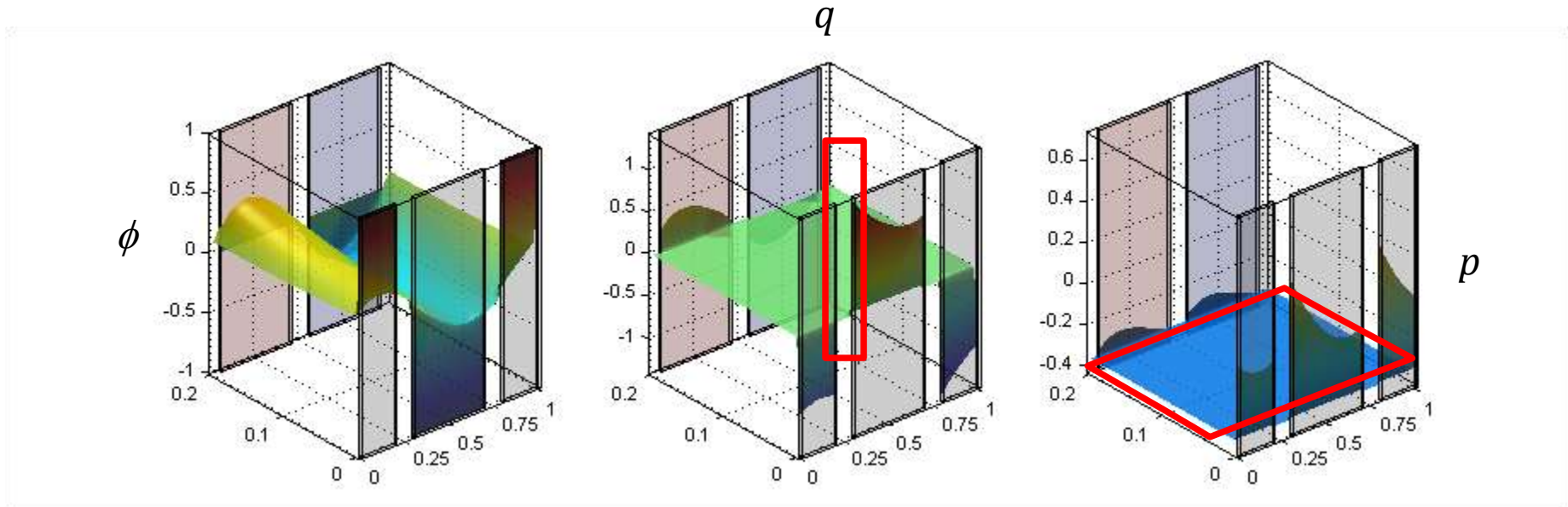


Used mathematical method and solver

- **Software:** Matlab 2007a & COMSOL Multiphysics 3.4a
- **Method:** FEM
- **FE type:** Lagrange, 2nd order, triangular and (skewed) quadrilateral
- **FE count range:** 2500-16000, **Typical FE count:** 4000-5000
- **Solver:** femtime (pardiso, UMFpack)

Profiles of model quantities

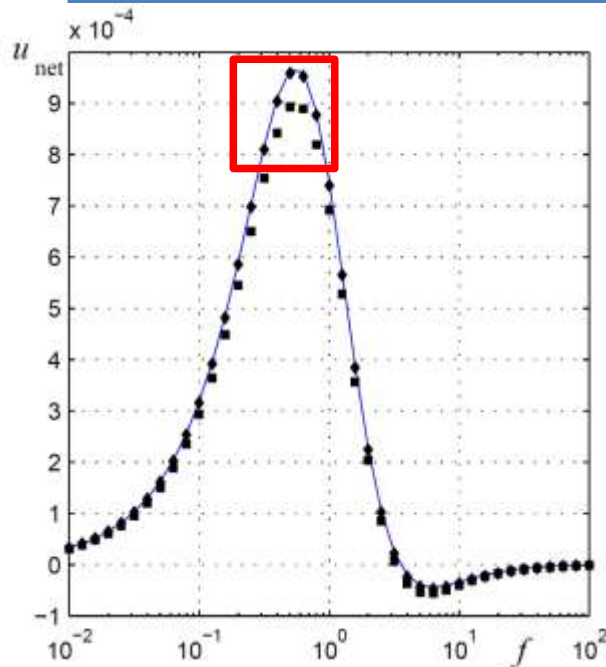
- ▣ The spatio-temporal profiles of the electric potential, the electric charge density and the pressure



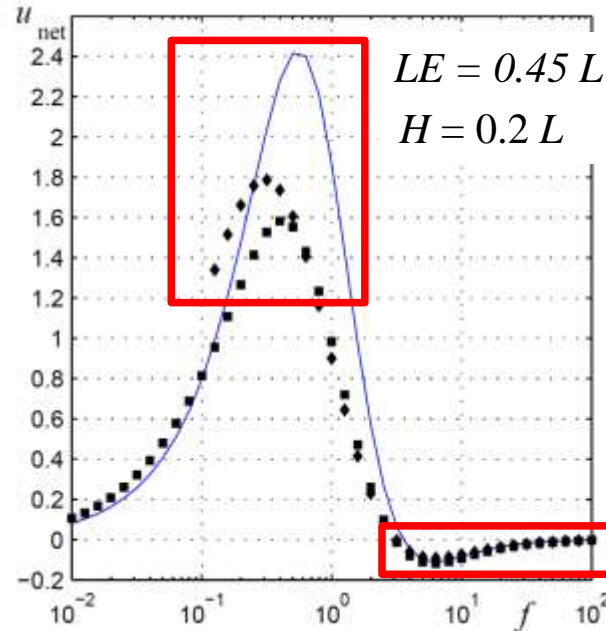
- ▣ The largest gradients of the physical fields occur near to the electrode corners
- ▣ The changes in physical quantities are restricted to the narrow zones close to the electrode surfaces

Net velocity characteristics

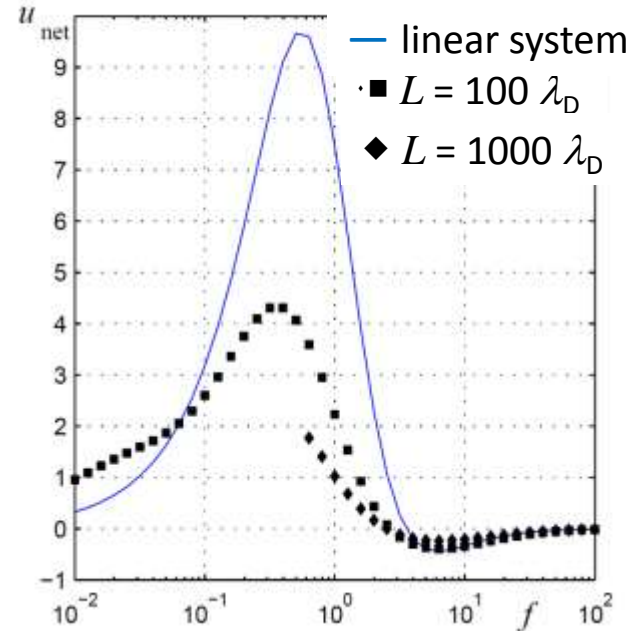
$$u_{\text{net}} = \frac{1}{T} \frac{1}{LH} \int_t^{t+T} \left(\iint_{\tilde{D}} \tilde{u}(\tilde{\mathbf{x}}, \tilde{t}) d\tilde{\mathbf{x}} \right) d\tilde{t}, \quad \tilde{D} = [0, 1) \times [0, \tilde{H}], \quad \tilde{t} \in [11, 12]T_o, \quad u_o = \frac{D}{L}, \quad t_o = \frac{\lambda_D L}{D}$$



A = 2,57 mV



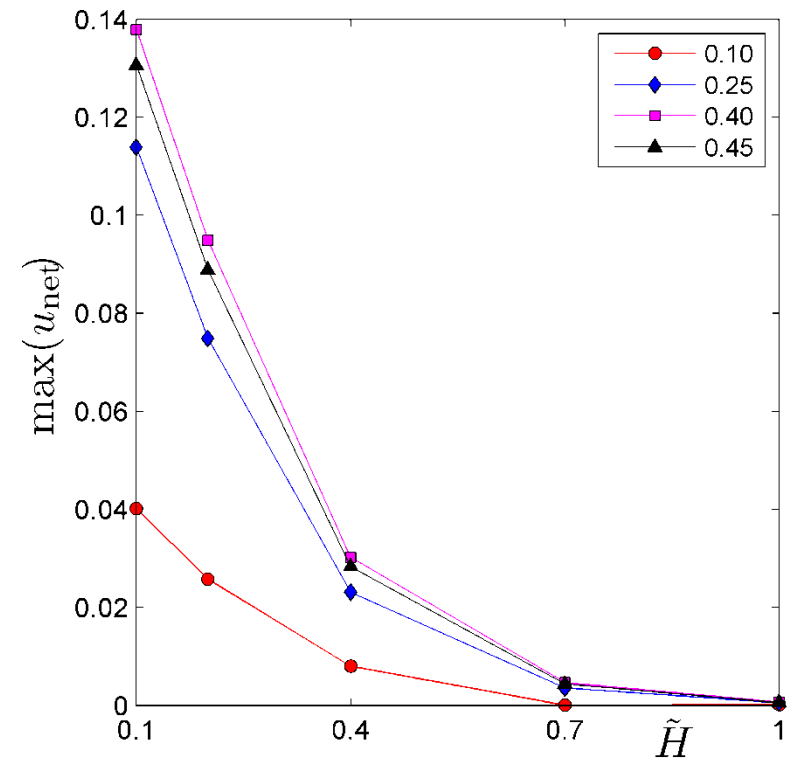
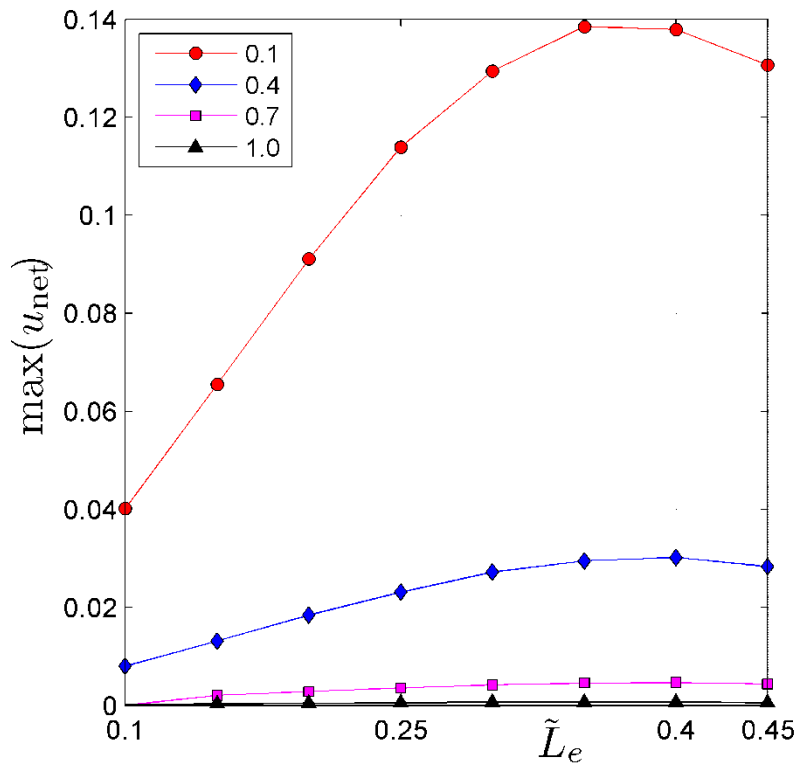
A = 128,5 mV



A = 257 mV

- There are discrepancies between data obtained by the linear and nonlinear models.
- With increased voltage, optimal frequencies drop to lower values.
- At higher frequencies, the direction of fluid flow changes, the flow reversal occurs.

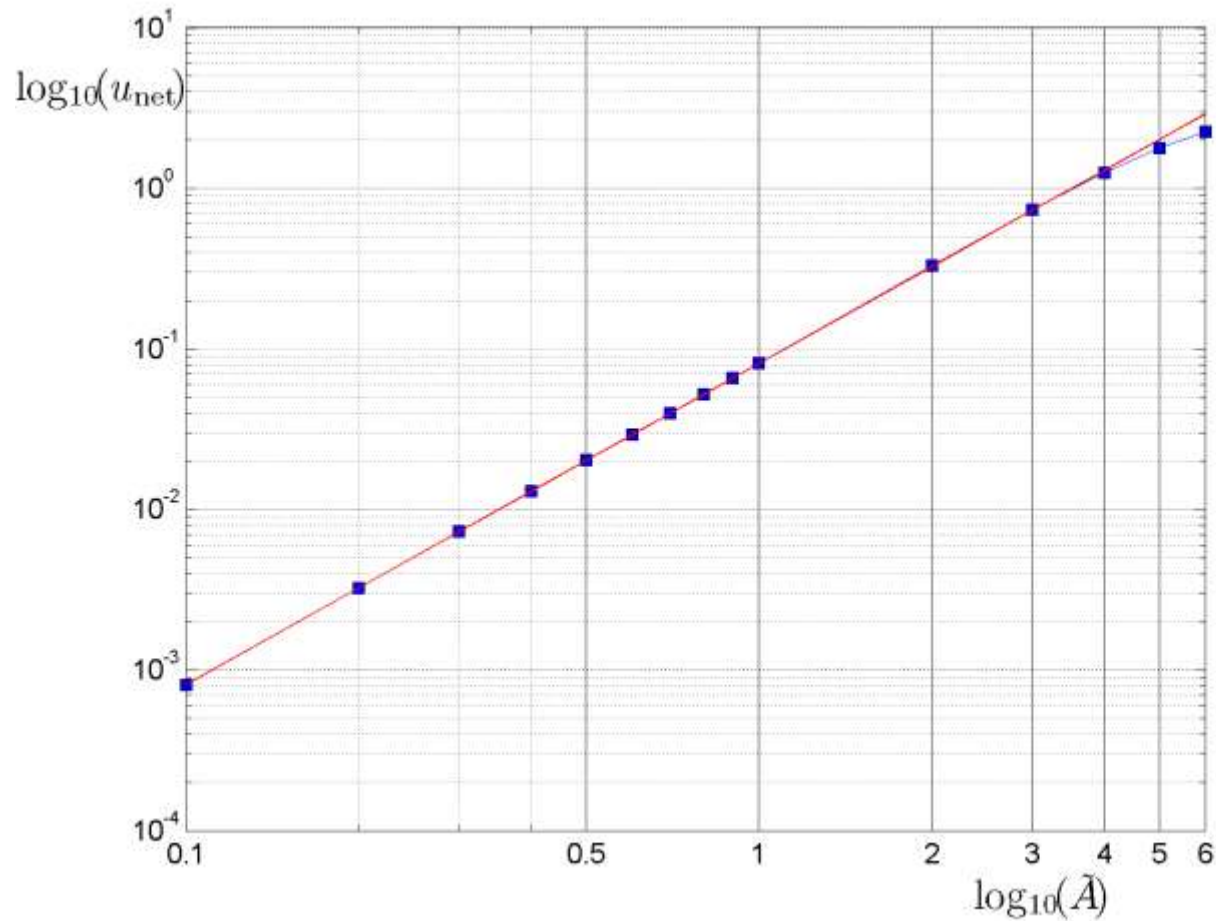
Net velocity characteristics – geometric parameters



■ There is an optimal electrode width, 30-40 % L

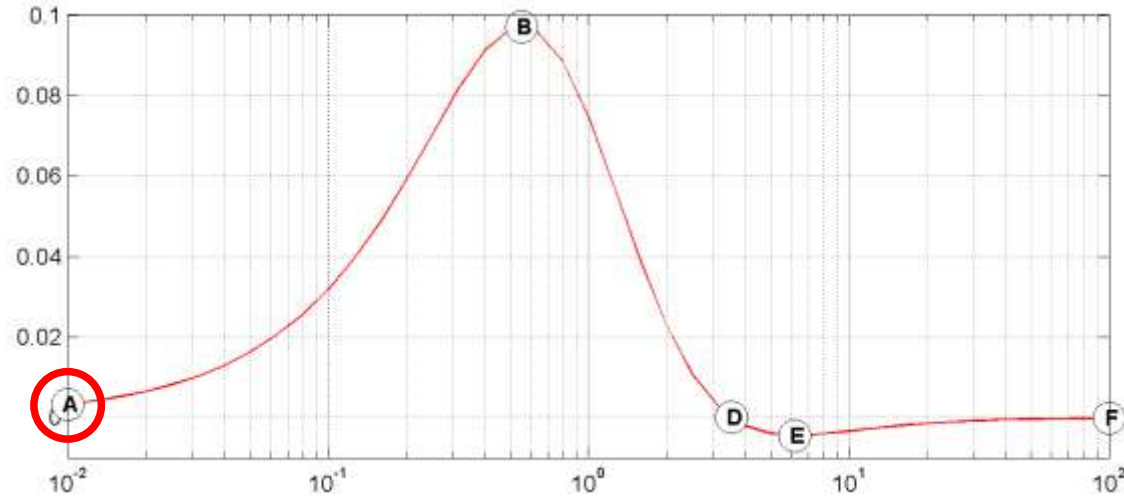
■ The net velocity decrease rapidly with the increasing channel height

Net velocity characteristics – voltage



- The net velocity is proportional to square of the voltage
- At higher voltages, the velocity increase slows down

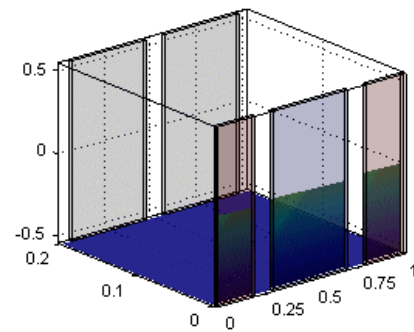
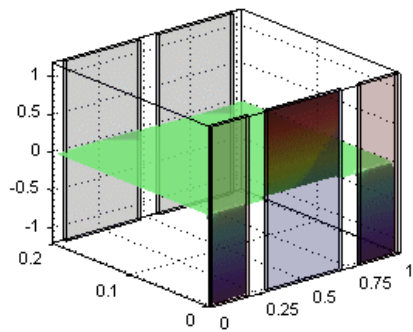
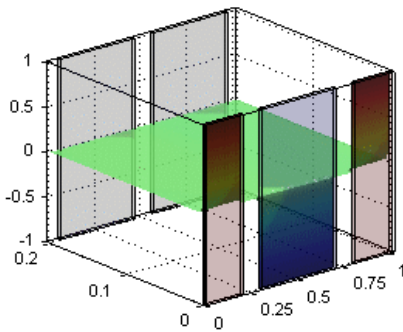
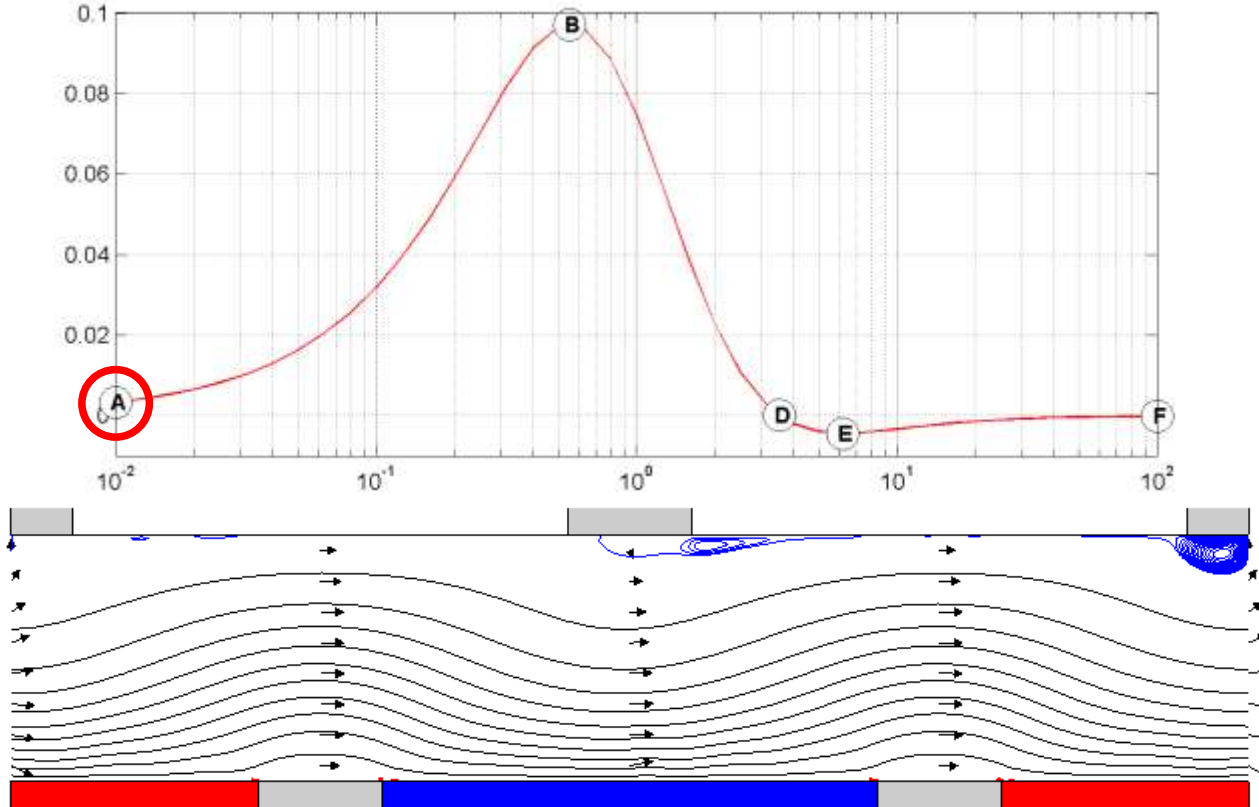
Net velocity characteristics – low frequencies



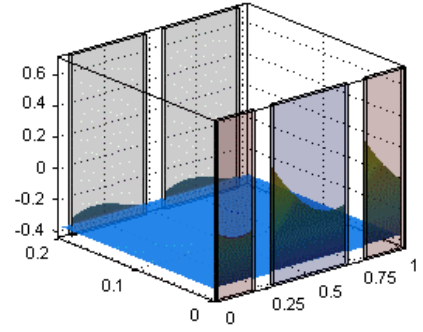
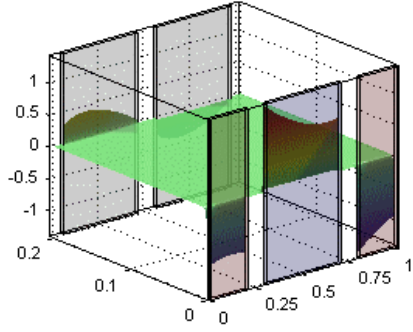
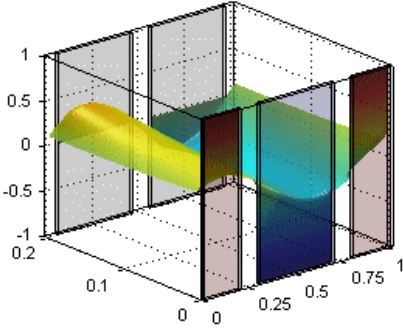
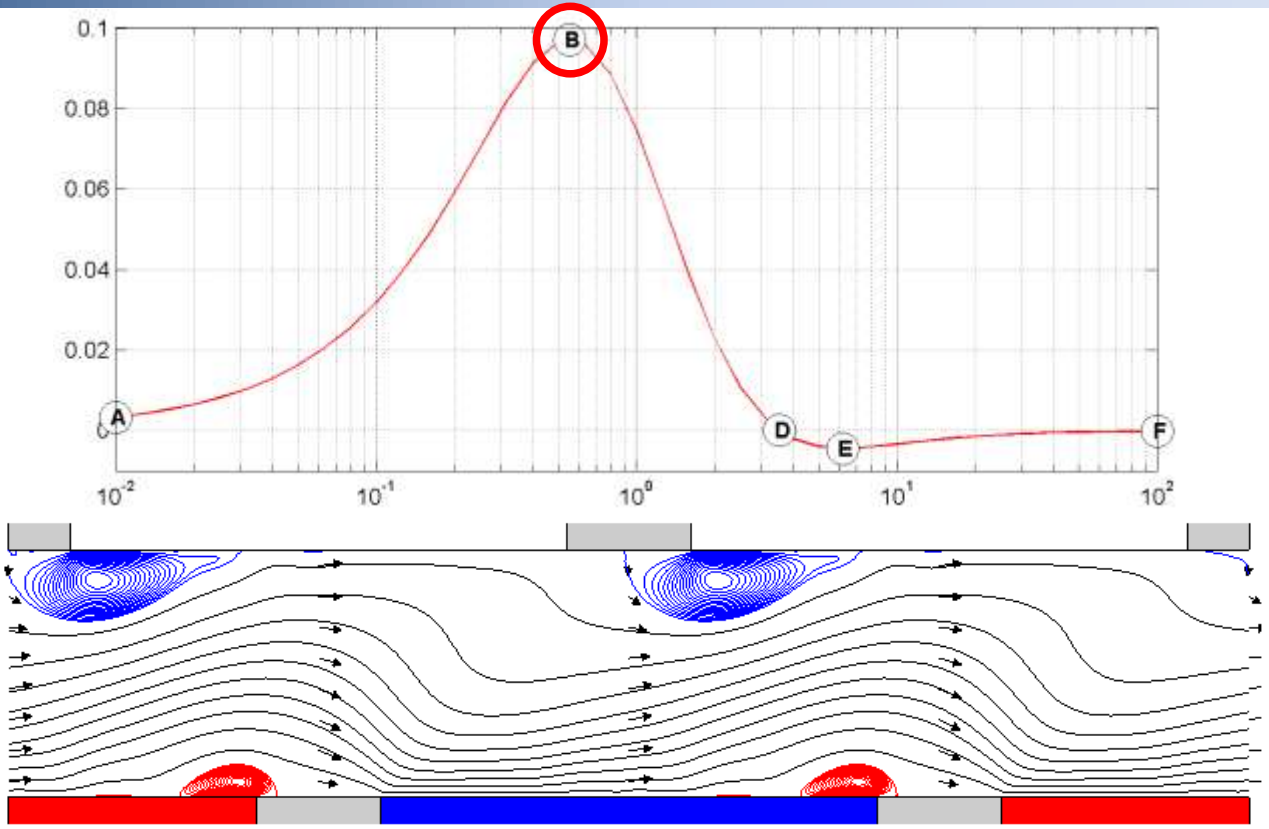
$$\tilde{A} = 1, \quad c_o = 92.54 \text{ mol/m}^3, \quad \tilde{\lambda}_D = 0.001 \quad \rightarrow \quad L = 1 \mu\text{m}, \quad f_o = 2 \text{ MHz}$$

$$\lambda_D = \sqrt{\frac{\varepsilon RT}{2c_o F^2}} \quad \& \quad c_o = \frac{\varepsilon RT}{2\lambda_D^2 F^2}$$

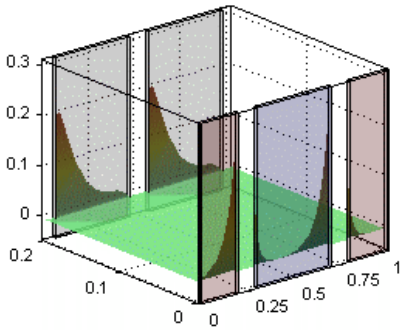
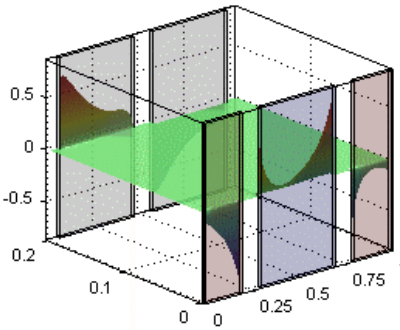
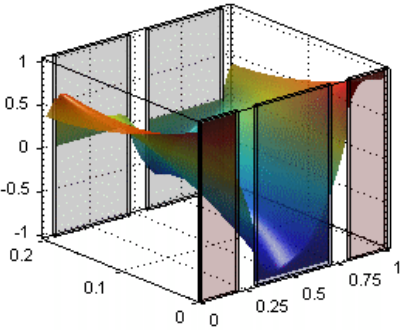
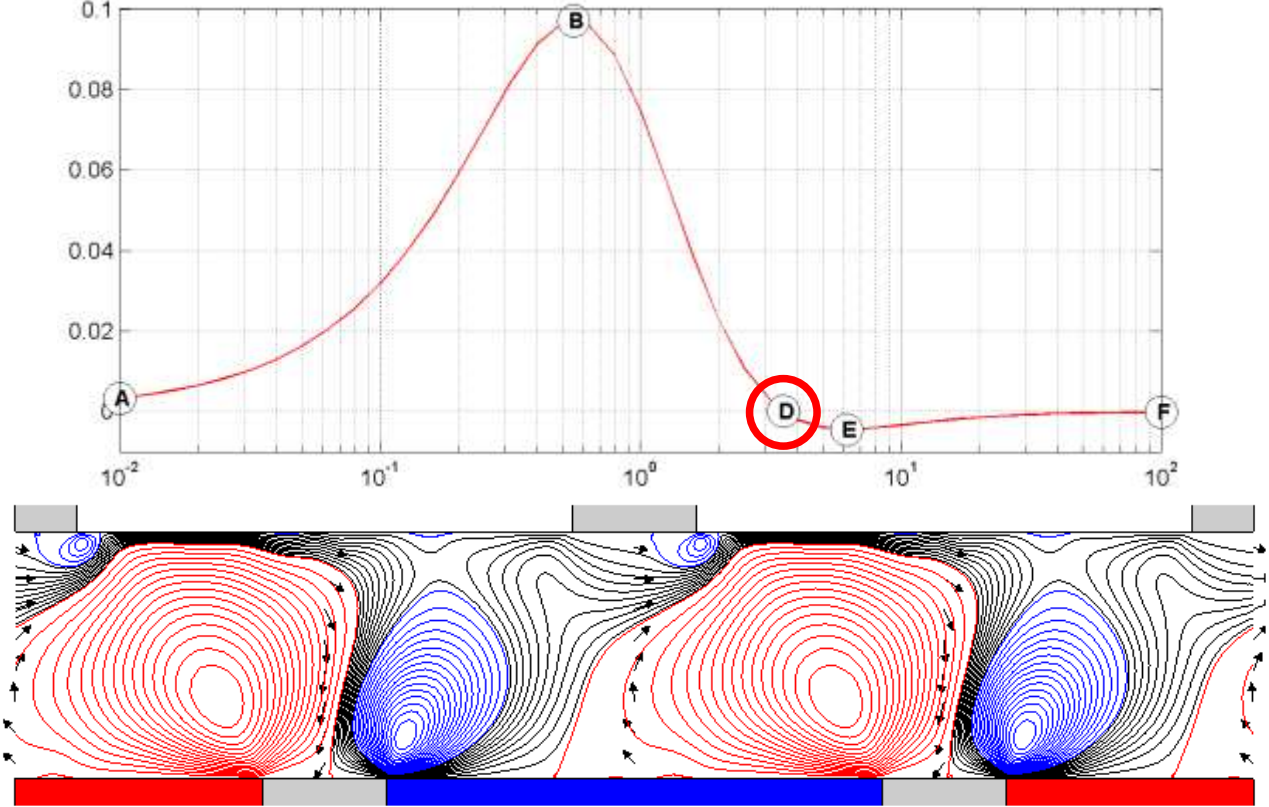
Net velocity characteristics – low frequencies



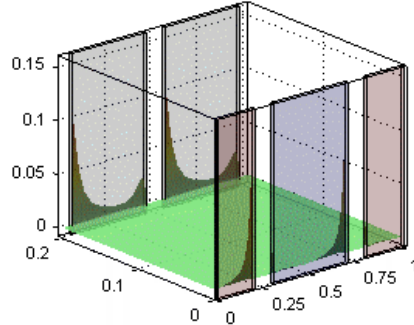
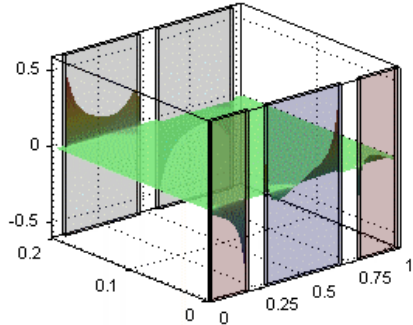
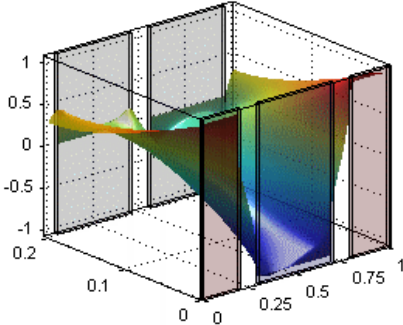
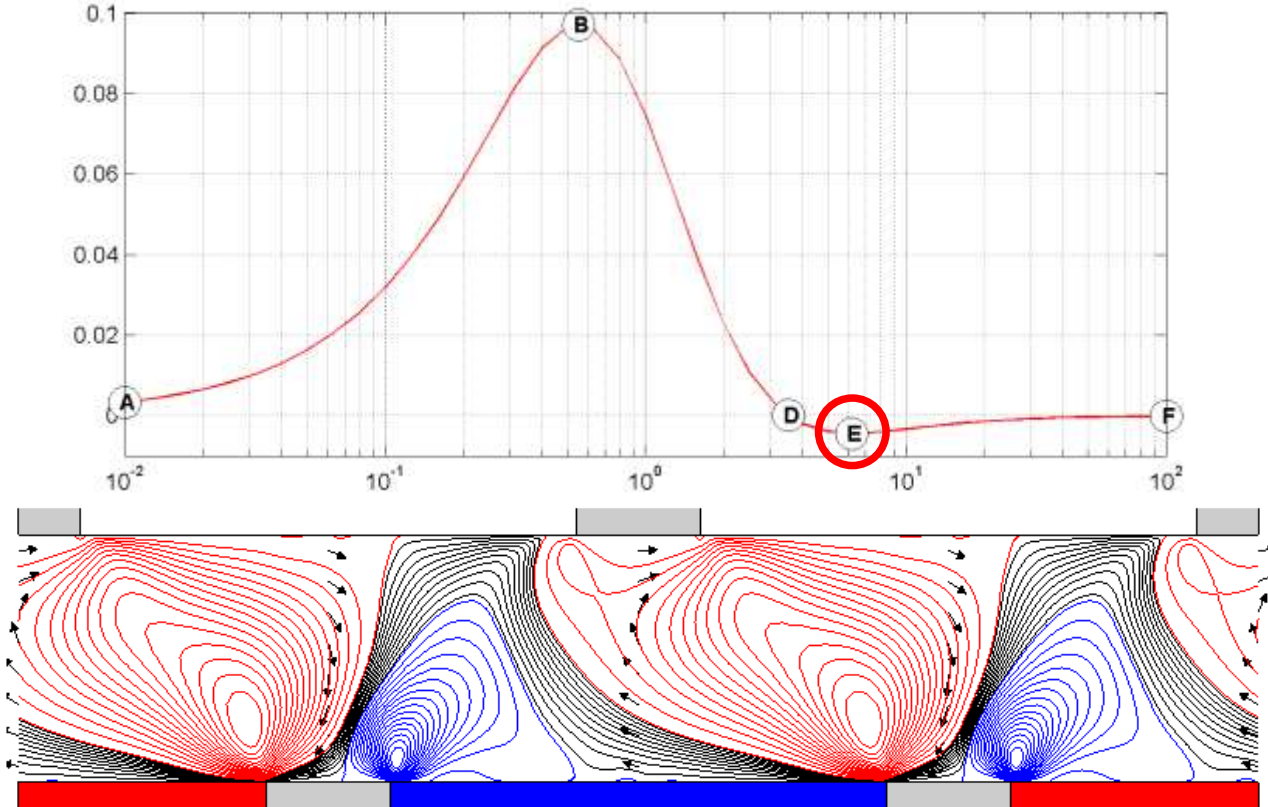
Net velocity characteristics – forward regime



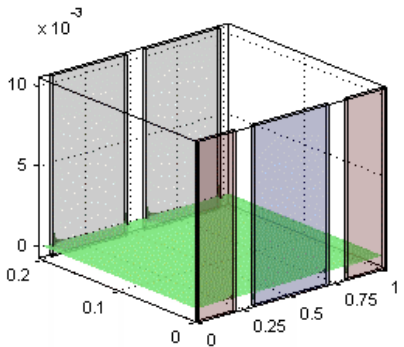
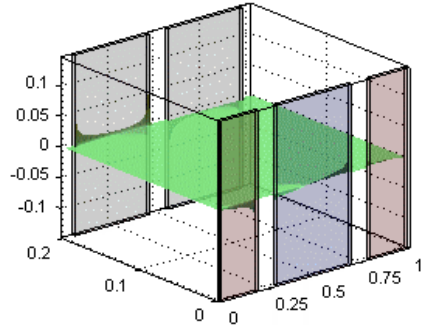
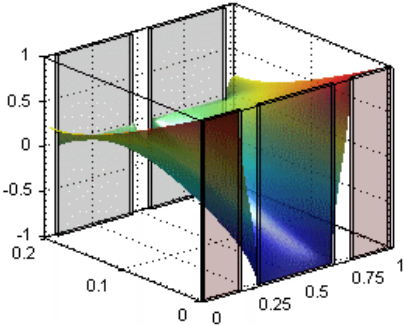
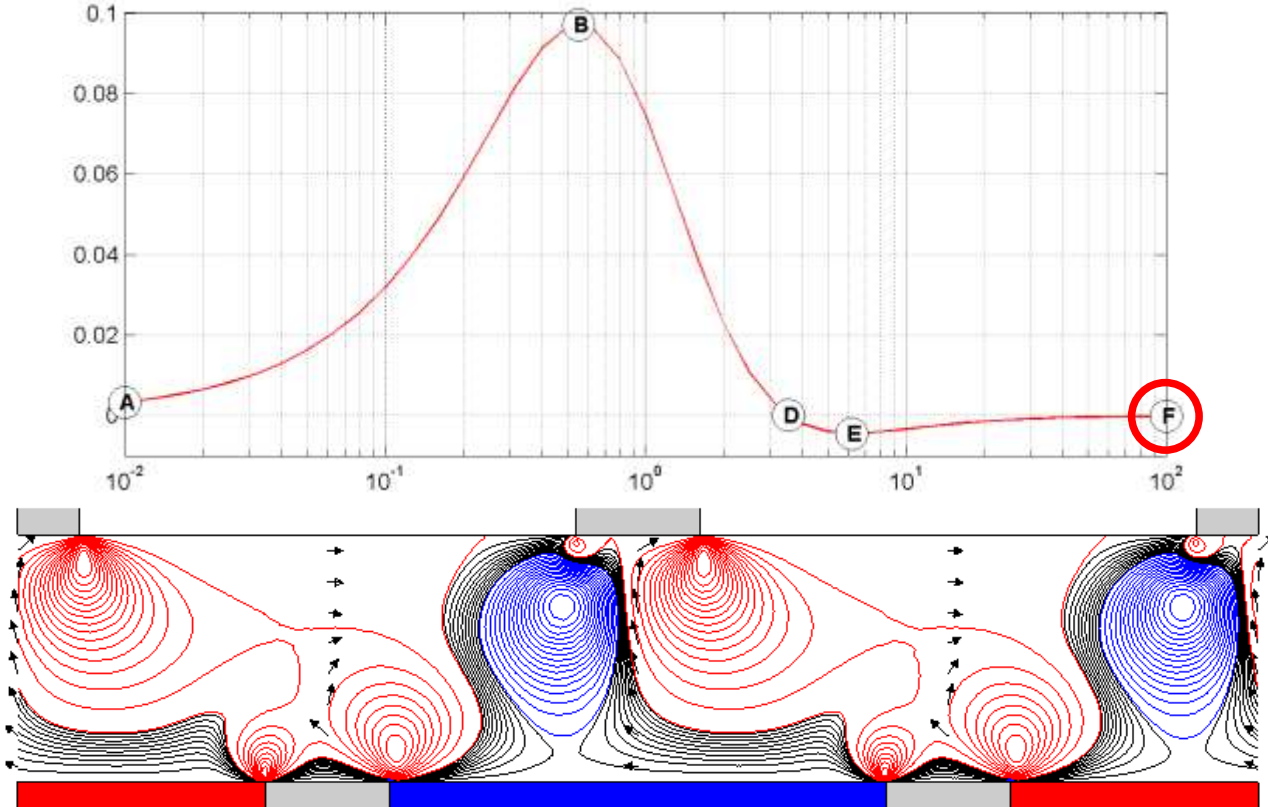
Net velocity characteristics – point of reversion



Net velocity characteristics – reversed regime



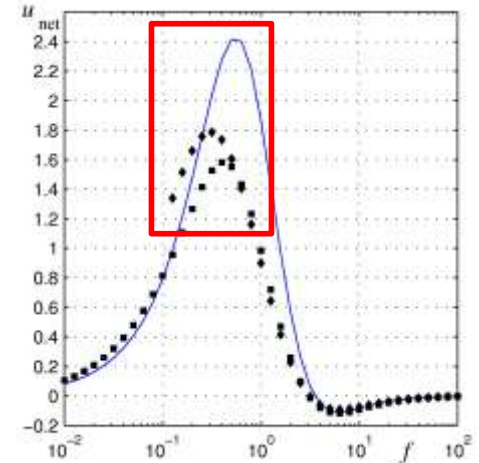
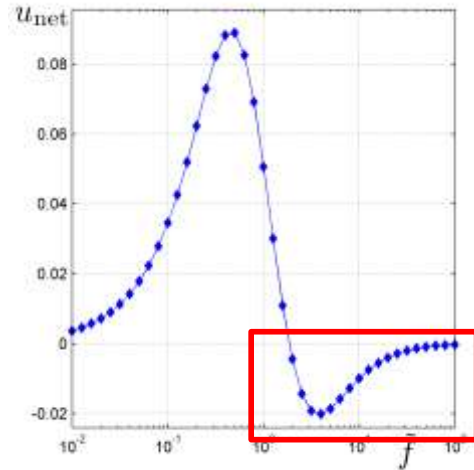
Net velocity characteristics – high frequencies



Conclusions

Zig-zag arrangement seems to have promising features

- ▣ Employs an interdigital technique for easier electrode arrays construction
- ▣ The electrode overlap makes possibility to control the flow direction



- ▣ The further miniaturization positively influences the net velocity

$$u_{\circ} = \frac{D}{L}$$

Future directions

- ▣ Experimental realization (first steps)
- ▣ More accurate model of EDL is needed (condensed layer), nonlinear description
- ▣ Incorporation of the energy balance to our mathematical model

Thank you for your attention!

Frequently Asked / Anticipated Questions:

- ▣ Continuum hypothesis vs. small elements
- ▣ Experimental realization
- ▣ Discretization mesh validation
- ▣ Cap height estimation
- ▣ Periodic regime determination