

Impact of Battery Operation and Manufacturing Process on Battery Performance over Lifetime

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Project Goals

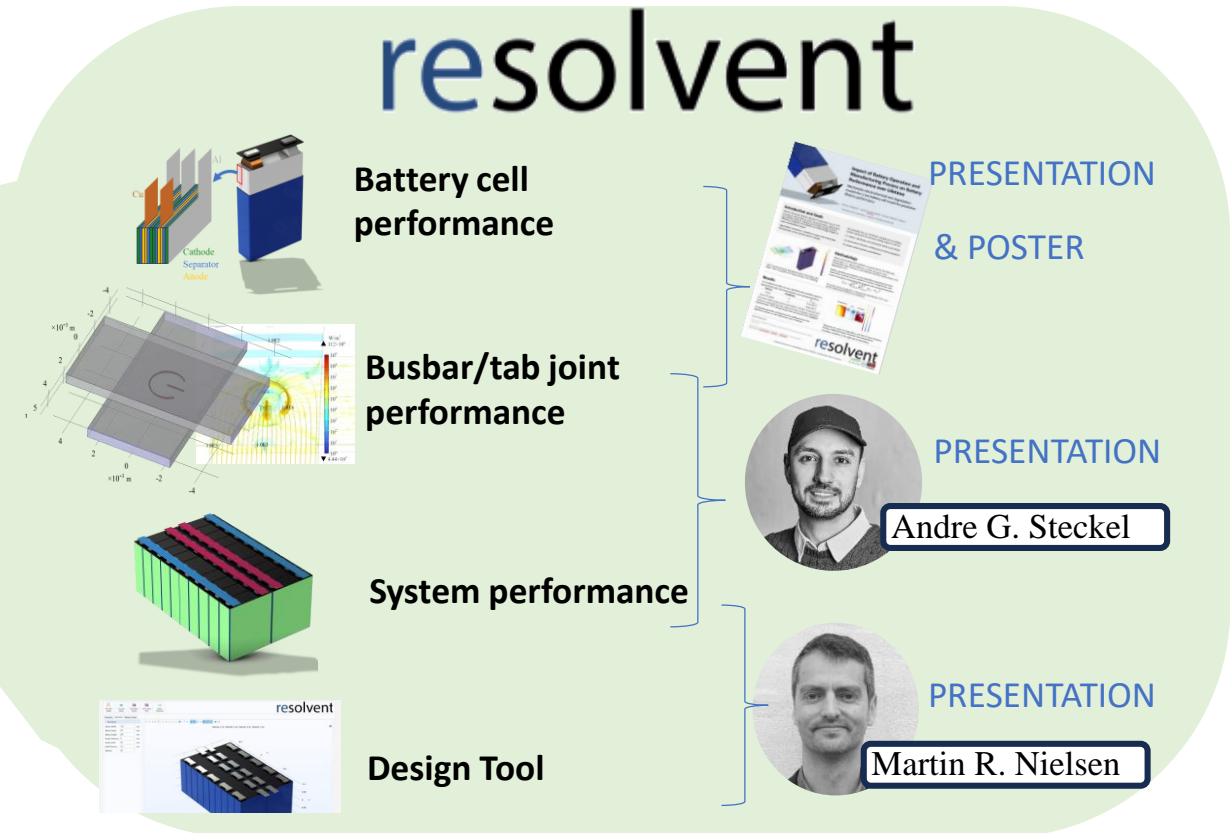
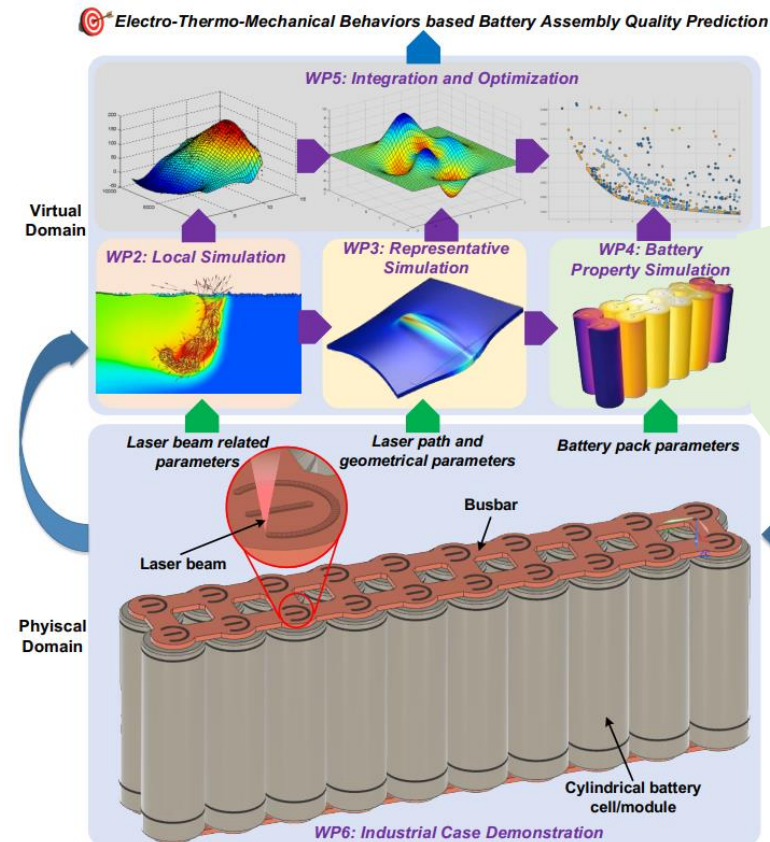
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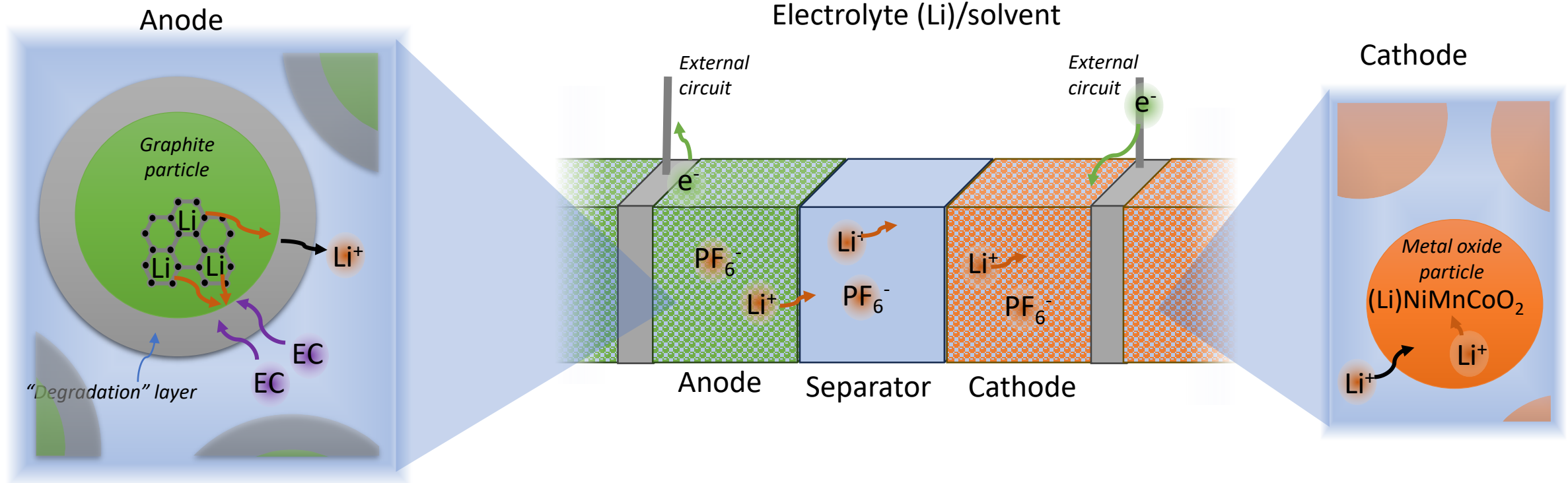
Project: Multi-scale simulation of laser welding for optimal battery pack manufacturing



Aurobay **resolvent**



Electrochemical Battery Model



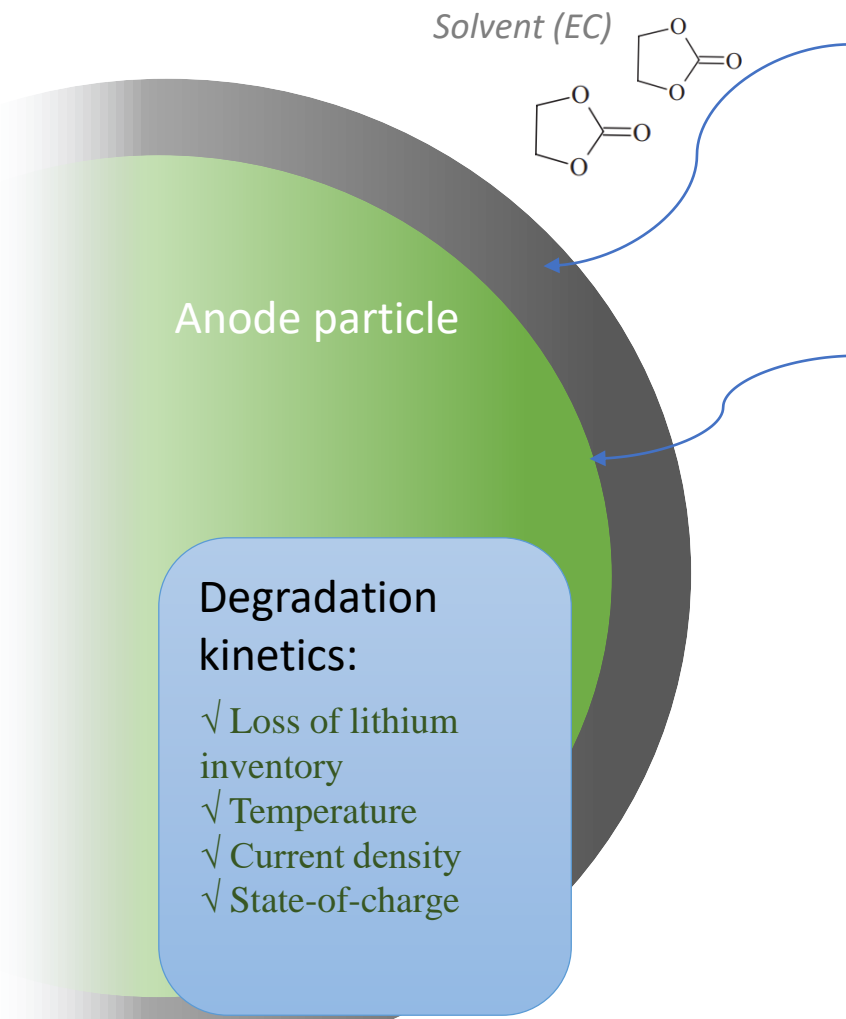
Lithium diffusion
 Ionic current distribution

Degradation

Intercalation

Electric current distribution

Electrochemical Battery Model

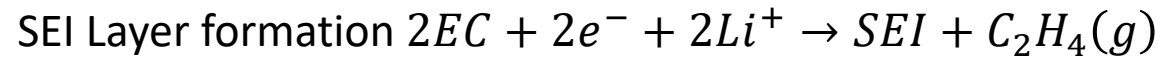


Solvent diffusion through SEI layer

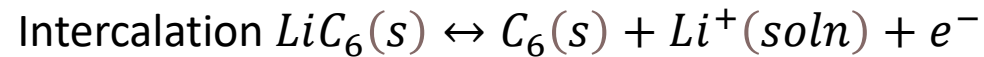
$$\frac{\partial c_{EC,P}}{\partial t} = \frac{\partial}{\partial r} \left(D_{EC,P} \frac{\partial c_{EC,P}}{\partial r} \right) - \frac{d\delta_{SEI}}{dt} \frac{\partial c_{EC,P}}{\partial r}$$

$$\frac{d\delta_{SEI}}{dt} = -\frac{i_s}{2F} \frac{M_{SEI}}{\rho_{SEI}}$$

Reaction on particle surface



$$i_s = -Fk_{f,s}c_{EC} \exp \left[-\frac{\beta F}{RT} \left(\phi_{S,n} - \frac{\delta}{\kappa_{SEI}} i_{tot} \right) \right]$$



$$i_{int} = i_{int,0} \cdot 2 \sinh \left[\frac{0.5F}{RT} \left(\phi_{S,n} - \phi_{E,n} - U_{0,n} - \frac{\delta}{\kappa_{SEI}} i_{tot} \right) \right]$$

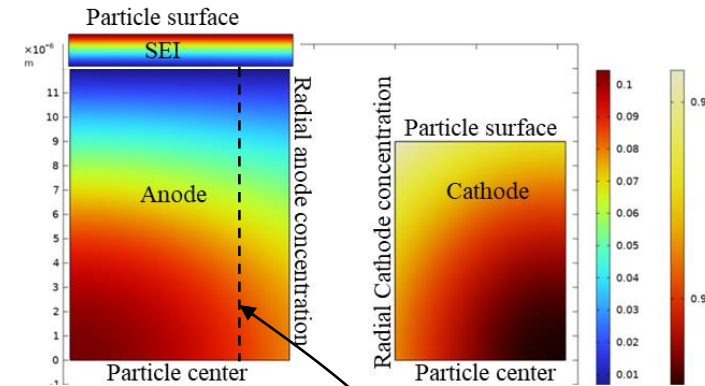
Total $i_{tot} = i_s + i_{int}$

Mass balance in particle surface:

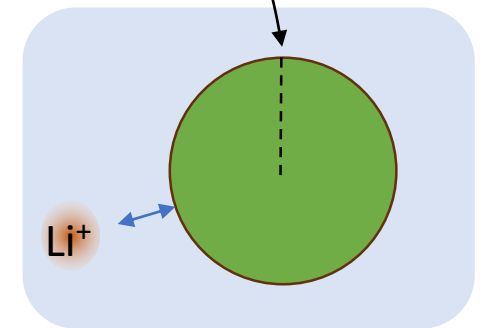
Lithium: $\left(-D_{eff,S} r^2 \frac{\partial c_P}{\partial r} \right) |_{r=\delta_{P,p}} = -\delta_{P,j}^2 \frac{i_{tot,j}}{F}$

Solvent: $\left(-D_{EC} \frac{\partial c_{EC}}{\partial r} + c_{EC} \right) |_{r=\delta_{P,p}} = i_s/F$

EC concentration at particle surface



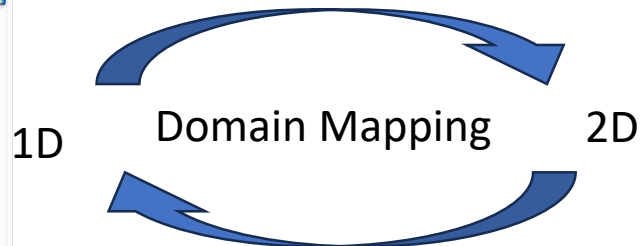
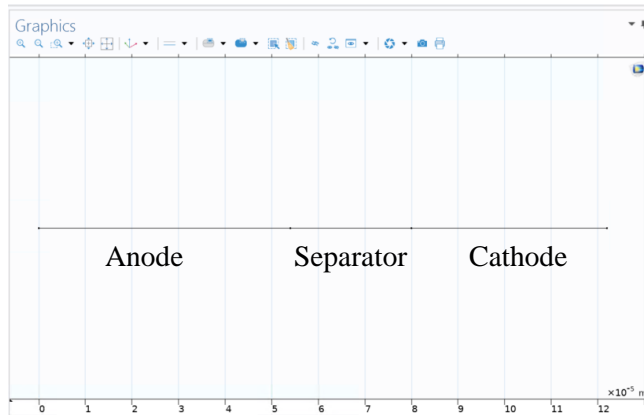
Spherical Electrode Particles



COMSOL Implementation

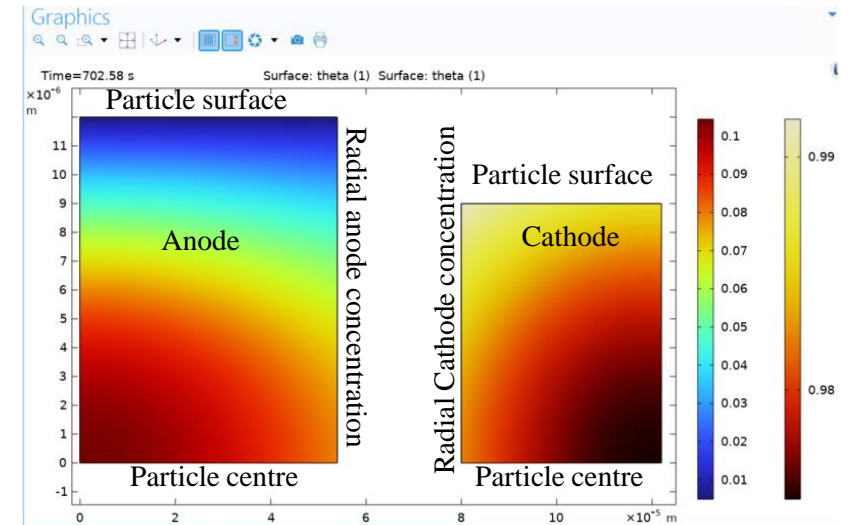
Electrochemistry & Degradation

- Component 1 | Cell (*comp1*)
 - Definitions
 - Geometry 1
 - Materials
 - Δu Coefficient Form PDE | Mass Balance Electrolyte Li ion (*c*) Lithium mass balance
 - Δu Coefficient Form PDE | Current Balance Electrolyte (*c3*) Current balance
 - Δu Coefficient Form PDE | Current Balance Electrode (*c4*) Heat balance
 - Δu Coefficient Form PDE | Energy Balance (*c5*) Heat balance
 - $\frac{d}{dt}$ Domain ODEs and DAEs | SEI Layer Formation (*dode*) Degradation
 - $\int du$ Weak Form PDE | Algebraic relations (*w*) Degradation
 - Mesh 1

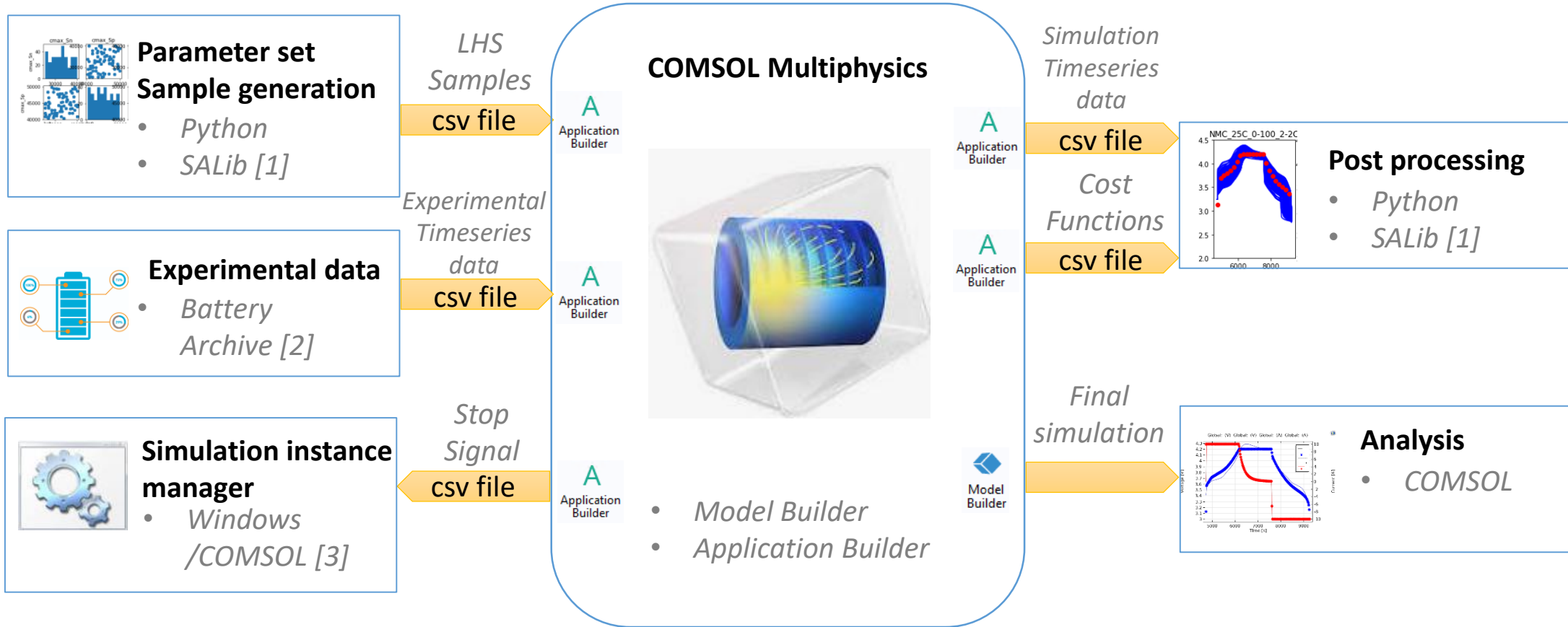


Particle and SEI Layer Diffusion

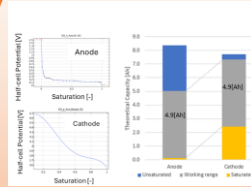
- Component 2 | Particle (*comp2*)
 - Definitions
 - Geometry 2
 - Materials
 - Δu Coefficient Form PDE | Mass Balance Li ion Particle (*c2*) Lithium mass balance
 - Δu Coefficient Form PDE | Mass Balance Solvent SEI (*c6*) Degradation
 - Mesh 2



COMSOL Implementation



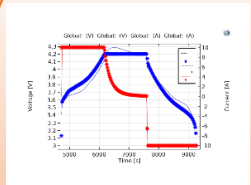
Parameter Fitting Method



Pre-Cycling

- Open cell voltage
- Half cell voltage
- SEM micrographs
- Design /Manufacturer data

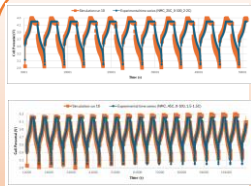
First-principles parameters



Single Cycle ("Fresh")

- Fresh battery
- Time-potential-current time series data
- Charge /Discharge /Rest
- Varying conditions (temperature, C-rates, SOC min /max)

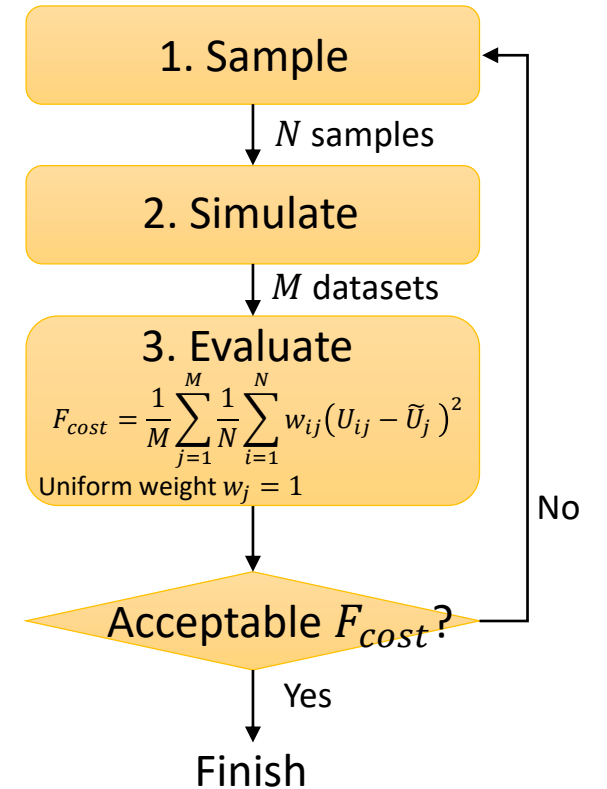
System parameters
Temperature dependent kinetics and diffusion
 $(k_n, E_{kn}), (k_p, E_{kp}), (D_n, E_{Dn}), (D_p, E_{Dp}), R_{cell}$



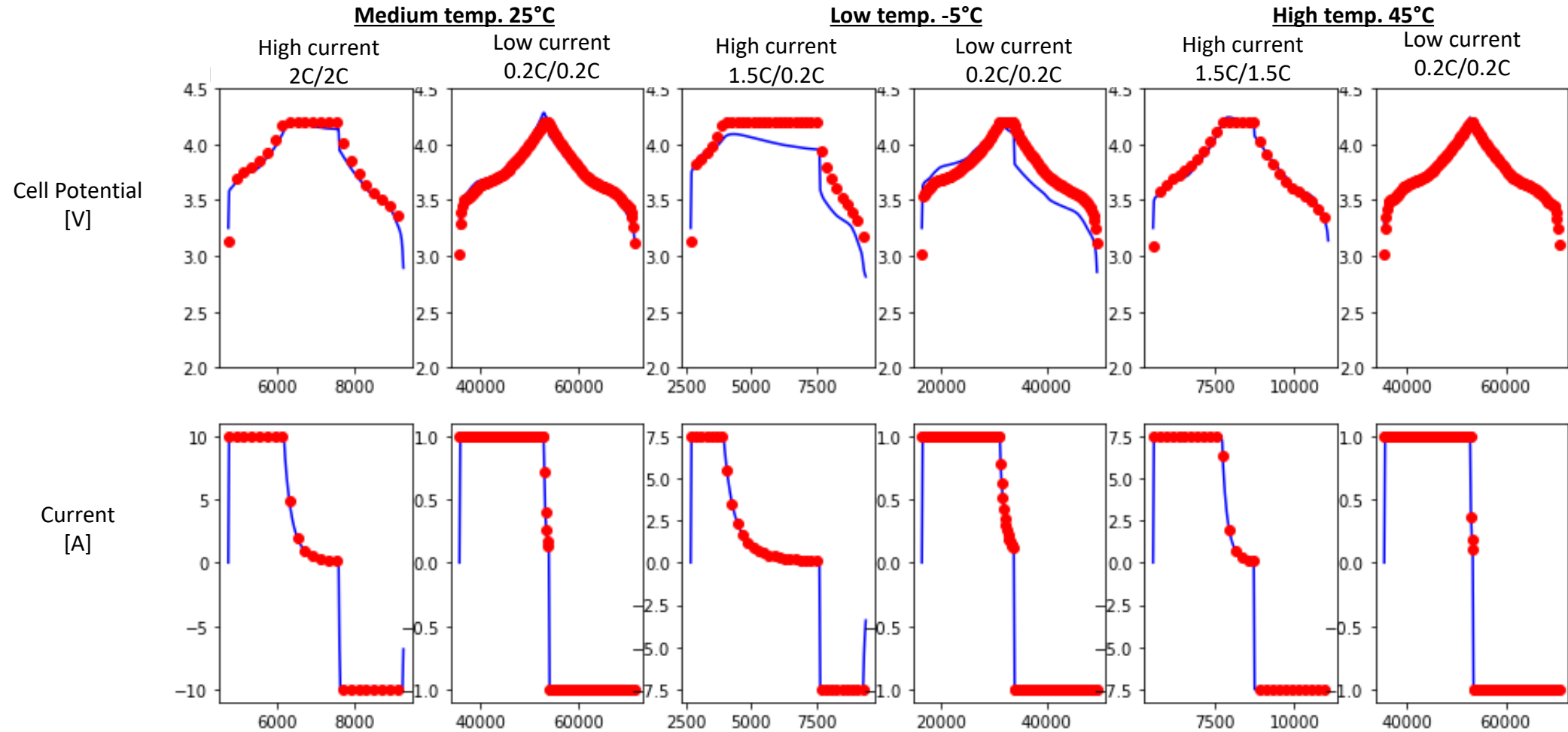
Multiple Cycles

- Multiple cycling data
- Time-potential-current time series data
- Charge /Discharge /Rest
- Varying conditions (temperature, C-rates, SOC min /max)

System Parameters
Degradation
 $D_{EC,SEI}, k_{SEI}$

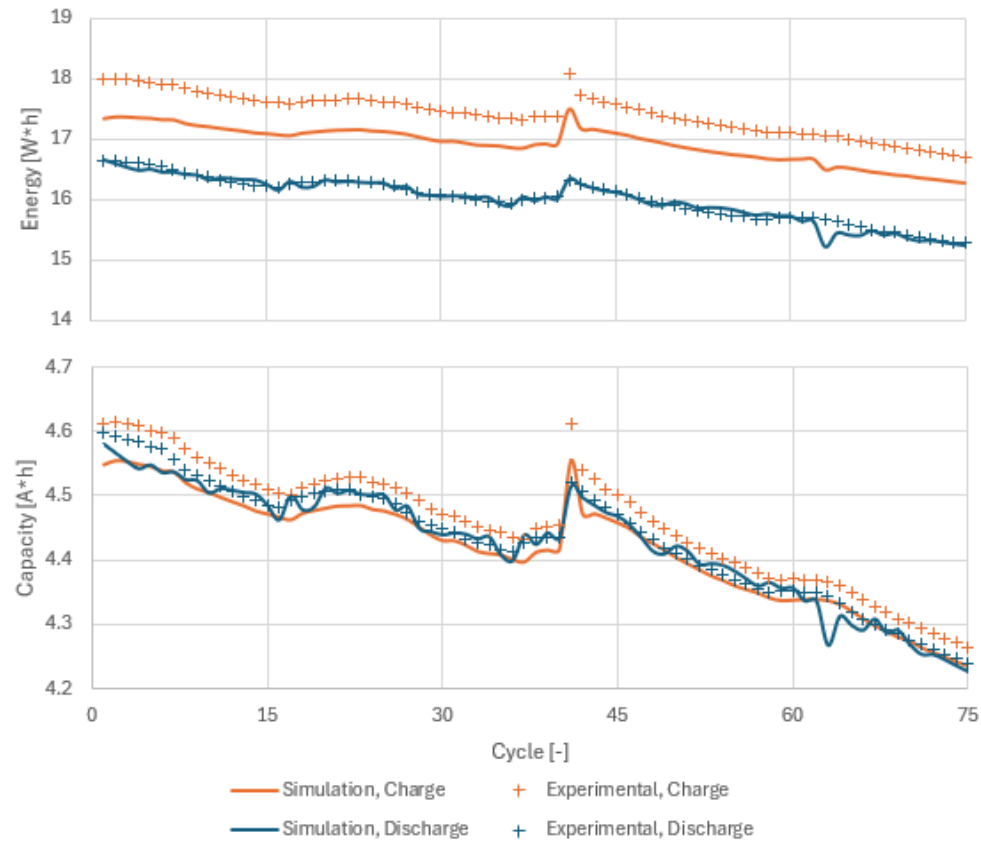


Expected vs Obtained Results

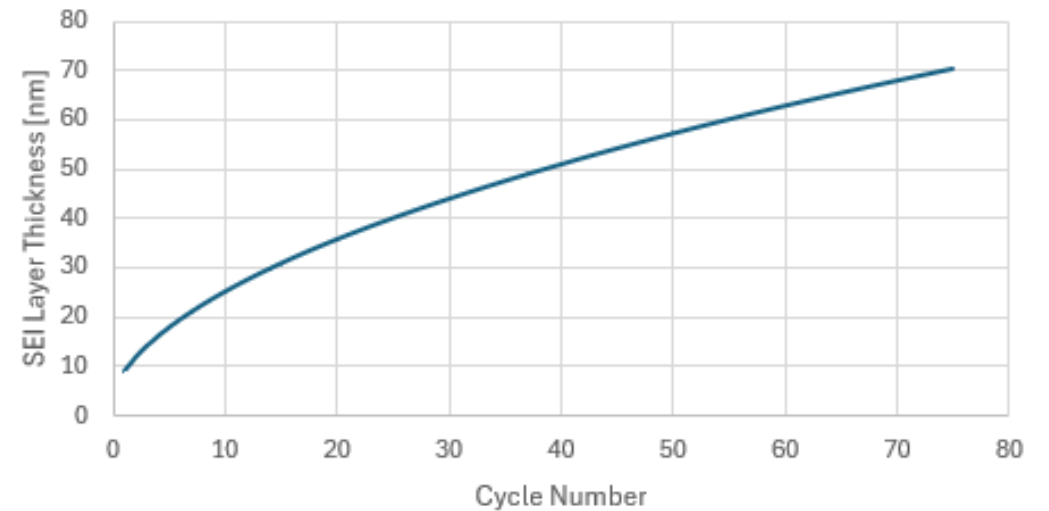


Expected vs Obtained Results

25°C, 2C Discharge, 2C Charge



25°C, 2C discharge, 2C charge current



Quality of Fit

Fresh Battery

$N = 600$ (samples)
 $M = 6$ (datasets)

$$\min F_{cost} = 0.012[V^2]$$

Degradation

$N = 25$ (samples)
 $M = 2$ (datasets)
 $CYC = 75$ (cycles)

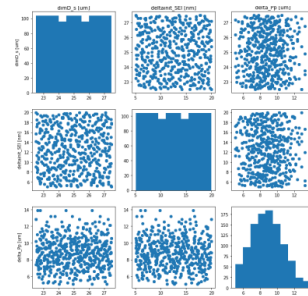
$$\min F_{cost} = 0.667[V^2]$$

Uncertainty and Sensitivity Analysis

Inputs – Manufacturing Parameters

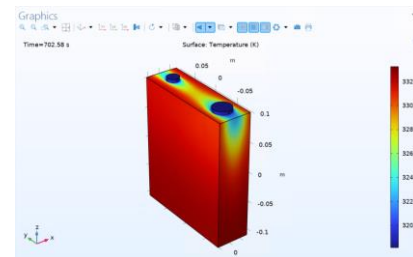
- Mechanical process tolerances**
Separator thickness variations
 $L_s \sim \mathcal{U}(22.5[\mu m]; 27.5[\mu m])$
- Cell Storage Conditioning variations**
Initial SEI layer thickness
 $\delta_{SEI,init} \sim \mathcal{U}(5[nm], 20[nm])$
- Electrode process parameter limits**
Positive electrode particle radius
 $\delta_{P,p} \sim \mathcal{N}(8.4[\mu m]; (2.5[\mu m])^2)$

Uncertain Parameter Sampling



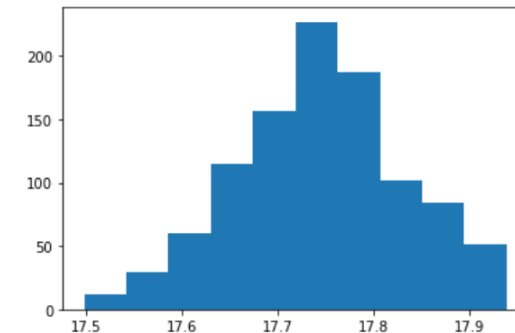
Sample size=1024

Battery Cell Electrochemical Model



Outputs – Cell Quality Control

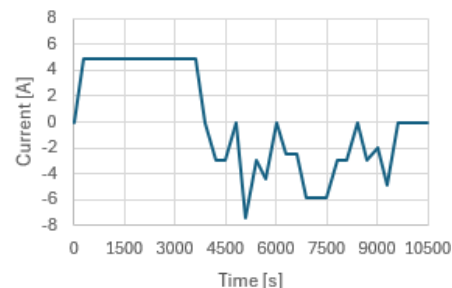
Uncertainty Analysis



Inputs – Operating Parameters

- Charge: 1C**
- Discharge conditions: Varying**
- Temperature: 25°C**

Load curve



Sensitivity Analysis

Sobol indices [1]:

S_{1i} = Contribution to output variance

S_{Ti} = Overall effect

Uncertainty and Sensitivity Analysis

Ranking of variables for importance on output variance:

- 1 cycle: $L_S > \delta_{SEI,init} > \delta_{P,p}$
- 25 cycles: $\delta_{P,p} > \delta_{SEI,init} > L_S$

Optimization

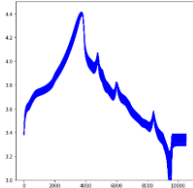
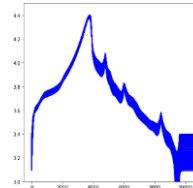
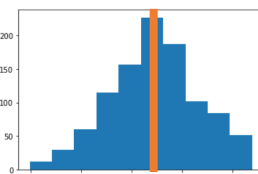
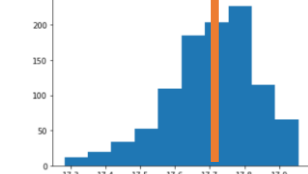
- Manufacturing cost example based on product specification:

$$Cost = Cost_{nomial} + Cost_{oversize}$$

$$Cost_{nomial} = f(\mu, \dots)$$

$$Cost_{oversize} = f(\sigma^2, \dots)$$

Reduce $Cost_{oversize}$ by reducing variance on cathode particle size distribution.

Variable	1 st cycle		25 th cycle	
Potential				
Histogram				
Discharge energy 95% confidence interval [W*h]	17.60 ≤ 17.75 ≤ 17.89		17.46 ≤ 17.71 ≤ 17.89	
Sensitivity [1]	$S_{1i}^{cycle=1}$	$S_{Ti}^{cycle=1}$	$S_{1i}^{cycle=25}$	$S_{Ti}^{cycle=25}$
L_S	0.36	0.97	0.03	0.36
$\delta_{SEI,init}$	0.38	0.86	0.30	0.78
$\delta_{P,p}$	0.33	0.69	0.39	0.90

Conclusions

- Successful implementation of an electrochemical model of a battery including degradation
- Robust framework for parameter fitting
- Parameters successfully tuned for data set (incl. temperature dependency)
- Uncertainty/Sensitivity Analysis to quantify performance parameter variance
- Uncertainty/Sensitivity Analysis to prioritize optimization efforts on e.g., manufacturing process

- COMSOL Application Builder offers excellent freedom and flexibility for handling large data sets and complex scenario simulations

Acknowledgement

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Project: Multi-scale simulation of laser welding for optimal battery pack manufacturing



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